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FINAL INSTALLATION RESTORATION STAGE 2 FEASIBILITY STUDY FOR THE EAST
AREA NAS FORT WORTH TX
10/1/1991
RADIAN CORPORATION

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A.F.



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FORT WORTH JRB
CARSWELL FIELD
TEXAS

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**ADMINISTRATIVE RECORD
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INSTALLATION RESTORATION PROGRAM (IRP)

STAGE 2

CARSWELL AFB, TEXAS

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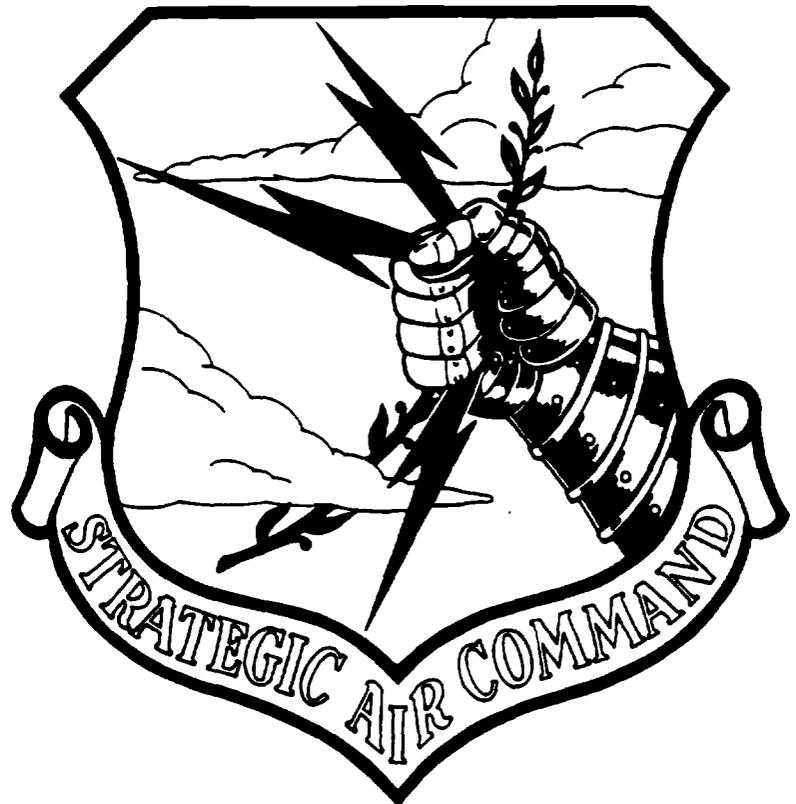
FINAL REPORT - OCTOBER 1991

FEASIBILITY STUDY
FOR THE EAST AREA

PREPARED FOR

HEADQUARTERS STRATEGIC AIR COMMAND
(HQ SAC/DE)
OFFUTT AIR FORCE BASE, NEBRASKA 68113-5001

UNITED STATES AIR FORCE
AIR FORCE CENTER FOR ENVIRONMENTAL EXCELLENCE
ENVIRONMENTAL SERVICES OFFICE
ENVIRONMENTAL RESTORATION DIVISION (AFCEE/ESR)
BROOKS AIR FORCE BASE, TEXAS 78235-5000





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HEADQUARTERS, STRATEGIC AIR COMMAND
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USAF CONTRACT NO. F33615-87-D-4023, DELIVERY ORDER NO. 0004, MODIFICATION 0005
CONTRACTOR CONTRACT NO. 227-005-04, DCN 91-227-005-04-22

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PREFACE

Radian Corporation is the contractor for the Installation Restoration Program (IRP) Phase II, Stage 2 investigation at Carswell AFB, Texas. The work was performed under USAF Contract No. F33615-87-D-4023, Delivery Order 0004, in two separate efforts; the first in 1987-88, and the second in 1990.

A hydrogeological investigation was conducted at several landfills, fire department training areas, and fuels handling areas to further assess and define the extent of contamination confirmed in the Stage 1 investigation at Carswell AFB. Soil gas surveys were conducted in 1988 at two locations to determine the extent of petroleum hydrocarbon vapors. Ground-water monitor wells were installed in alluvial materials to further define the limits of ground-water contamination. Soil samples were collected during drilling operations and with hand augers at selected sites and analyzed for a broad range of parameters in the initial Stage 2 effort. Water samples collected from the wells and several surface water bodies were analyzed for a wide spectrum of total metals, inorganic compounds, and organic compounds. Dissolved metals concentrations were analyzed only in the samples collected in 1990. A pumping test of the Upper Zone Aquifer was also performed in the Flightline Area in 1990. A baseline risk assessment, incorporating all analytical data, was performed, and remedial action alternatives were identified and evaluated for the Flightline Area and four sites in the East Area of the base (Sites LF01, SD13, ST14, and BSS) in the Feasibility Study.

Key Radian project personnel were:

| | |
|---------------------|--|
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Radian would like to acknowledge the cooperation of the Carswell AFB Civil Engineering Staff. In particular, Radian acknowledges the assistance of Mr. Frank Grey, Mr. Raj Sheth, and Sgt. Stanley Reinhartz.

The work reported herein was accomplished between December 1987 and July 1990. Mr. Karl W. Ratzlaff, IRP Technical Operations Branch, Human Services Division (AFSC) IRP Program Office (HSD/YAQ), was the Technical Project Manager.

Approved:


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TABLE OF CONTENTS

| <u>Section</u> | <u>Page</u> |
|---|-------------|
| 1.0 INTRODUCTION | 1-1 |
| 1.1 Purpose and Organization of Report | 1-2 |
| 1.2 Background Information | 1-3 |
| 1.2.1 East Area Description | 1-6 |
| 1.2.2 Site History | 1-9 |
| 1.2.3 Nature and Extent of Contamination | 1-12 |
| 1.2.3.1 Site LF01--Landfill 1 | 1-13 |
| 1.2.3.2 Site SD13--Unnamed Stream and Abandoned Gasoline Service Station | 1-15 |
| 1.2.3.3 Site ST14--POL Tank Farm | 1-17 |
| 1.2.3.4 Site BSS--Base Service Station | 1-17 |
| 1.2.4 Contaminant Fate and Transport | 1-20 |
| 1.2.4.1 Fate of Main Analytes Detected in the East Area | 1-20 |
| 1.2.4.2 Contaminant Transport Pathways | 1-21 |
| 1.2.5 Baseline Risk Assessment | 1-24 |
| 2.0 IDENTIFICATION AND SCREENING OF TECHNOLOGIES | 2-1 |
| 2.1 Remedial Action Objectives | 2-1 |
| 2.2 Screening of Technologies | 2-5 |
| 2.2.1 Wastes and Contaminated Soil | 2-5 |
| 2.2.2 Ground Water | 2-12 |
| 2.2.3 Surface Water | 2-21 |
| 2.3 Selection of Remedial Technologies | 2-25 |
| 2.3.1 Long-Term Monitoring | 2-25 |
| 2.3.2 Ground-Water Extraction Wells | 2-25 |
| 2.3.3 Interceptor Trenches | 2-27 |
| 2.3.4 Air Stripping Treatment System | 2-27 |
| 2.3.5 In-Situ Biological Treatment | 2-29 |
| 2.3.6 Soil Vapor Extraction | 2-31 |
| 2.3.7 Soil Piles | 2-33 |
| 2.3.8 Secondary Treatment Systems | 2-33 |
| 3.0 DEVELOPMENT AND SCREENING OF ALTERNATIVES | 3-1 |
| 3.1 Development of Alternatives | 3-1 |
| 3.1.1 Site LF01--Landfill 1 | 3-1 |
| 3.1.2 Site SD13--Abandoned Gasoline Station and Unnamed Stream | 3-3 |
| 3.1.3 Site ST14--POL Tank Farm | 3-5 |
| 3.1.3.1 Preliminary Ground-Water Alternatives | 3-5 |
| 3.1.3.2 Preliminary Soil Alternatives--Site ST14 | 3-17 |

03-000

TABLE OF CONTENTS (Continued)

| <u>Section</u> | <u>Page</u> |
|---|-------------|
| 3.1.4 Site BSS--Base Service Station | 3-20 |
| 3.1.4.1 Preliminary Ground-Water Alternatives | 3-21 |
| 3.1.4.2 Preliminary Soil Alternatives | 3-31 |
| 3.2 Screening of Preliminary Alternatives | 3-31 |
| 3.2.1 Site LF01--Landfill 1 | 3-31 |
| 3.2.2 Site SD13--Abandoned Gasoline Station and Unnamed Stream | 3-33 |
| 3.2.3 Site ST14--POL Tank Farm | 3-33 |
| 3.2.3.1 Preliminary Ground-Water Alternatives | 3-33 |
| 3.2.3.2 Preliminary Soil Alternatives | 3-37 |
| 3.2.4 Site BSS--Base Service Station | 3-37 |
| 3.2.4.1 Preliminary Ground-Water Alternatives | 3-37 |
| 3.2.4.2 Preliminary Soil Alternatives | 3-40 |
| 3.3 Summary of Preliminary Alternative Development and Screening | 3-41 |
| 4.0 DETAILED ANALYSIS OF ALTERNATIVES | 4-1 |
| 4.1 Description of Evaluation Criteria and Analysis Method | 4-2 |
| 4.2 Detailed Evaluation of the No-Action Alternative for Site LF01 | 4-4 |
| 4.2.1 Description of the Alternative | 4-4 |
| 4.2.2 Protection of Human Health and the Environment | 4-4 |
| 4.2.3 Compliance with ARARs | 4-5 |
| 4.2.4 Long-Term Effectiveness and Permanence | 4-5 |
| 4.2.5 Reduction in Toxicity, Mobility, or Volume | 4-5 |
| 4.2.6 Short-Term Effectiveness | 4-6 |
| 4.2.7 Implementability | 4-6 |
| 4.2.8 Cost | 4-6 |
| 4.3 Detailed Evaluation of the No-Action Alternative for Site SD13 | 4-6 |
| 4.3.1 Description of Alternative | 4-6 |
| 4.3.2 Protection of Human Health and the Environment | 4-7 |
| 4.3.3 Compliance with ARARs | 4-7 |
| 4.3.4 Long-Term Effectiveness and Permanence | 4-7 |
| 4.3.5 Reduction in Toxicity, Mobility, or Volume | 4-8 |
| 4.3.6 Short-Term Effectiveness | 4-8 |
| 4.3.7 Implementability | 4-8 |
| 4.3.8 Cost | 4-8 |
| 4.4 Detailed Evaluation of Alternatives for Site ST14 | 4-8 |
| 4.4.1 Alternative 1--No Action | 4-9 |
| 4.4.1.1 Description of the Alternative | 4-9 |
| 4.4.1.2 Protection of the Human Health and the Environment | 4-9 |
| 4.4.1.3 Compliance with ARARs | 4-10 |
| 4.4.1.4 Long-Term Effectiveness and Permanence | 4-10 |

TABLE OF CONTENTS (Continued)

| <u>Section</u> | <u>Page</u> |
|----------------|---|
| 4.4.1.5 | Reduction in Toxicity, Mobility, or Volume 4-10 |
| 4.4.1.6 | Short-Term Effectiveness 4-11 |
| 4.4.1.7 | Implementability 4-11 |
| 4.4.1.8 | Cost 4-11 |
| 4.4.2 | Alternative 4A--Air Stripping and Reinjection 4-11 |
| 4.4.2.1 | Description of the Alternative 4-12 |
| 4.4.2.2 | Protection of Human Health and the Environment 4-12 |
| 4.4.2.3 | Compliance with ARARs 4-14 |
| 4.4.2.4 | Long-Term Effectiveness and Permanence 4-14 |
| 4.4.2.5 | Reduction in Toxicity, Mobility, or Volume 4-15 |
| 4.4.2.6 | Short-Term Effectiveness 4-15 |
| 4.4.2.7 | Implementability 4-16 |
| 4.4.2.8 | Cost 4-16 |
| 4.4.3 | Alternative 4B--Air Stripping and Discharge to the Sanitary Sewer 4-16 |
| 4.4.3.1 | Description of the Alternative 4-16 |
| 4.4.3.2 | Protection of Human Health and the Environment 4-18 |
| 4.4.3.3 | Compliance with ARARs 4-18 |
| 4.4.3.4 | Long-Term Effectiveness and Permanence 4-18 |
| 4.4.3.5 | Reduction in Toxicity, Mobility, or Volume 4-19 |
| 4.4.3.6 | Short-Term Effectiveness 4-19 |
| 4.4.3.7 | Implementability 4-19 |
| 4.4.3.8 | Cost 4-19 |
| 4.4.4 | Alternative 5--In-Situ Biological Treatment 4-20 |
| 4.4.4.1 | Description of the Alternative 4-20 |
| 4.4.4.2 | Protection of Human Health and the Environment 4-20 |
| 4.4.4.3 | Compliance with ARARs 4-22 |
| 4.4.4.4 | Long-Term Effectiveness and Permanence 4-22 |
| 4.4.4.5 | Reduction in Toxicity, Mobility, or Volume 4-22 |
| 4.4.4.6 | Short-Term Effectiveness 4-23 |
| 4.4.4.7 | Implementability 4-23 |
| 4.4.4.8 | Cost 4-23 |
| 4.5 | Detailed Evaluation of Alternatives for Site BSS 4-24 |
| 4.5.1 | Alternative 1--No Action 4-24 |
| 4.5.1.1 | Description of the Alternative 4-24 |
| 4.5.1.2 | Protection of Human Health and the Environment 4-24 |
| 4.5.1.3 | Compliance with ARARs 4-25 |
| 4.5.1.4 | Long-Term Effectiveness and Permanence 4-25 |
| 4.5.1.5 | Reduction in Toxicity, Mobility, or Volume 4-25 |
| 4.5.1.6 | Short-Term Effectiveness 4-26 |
| 4.5.1.7 | Implementability 4-26 |
| 4.5.1.8 | Cost 4-26 |

000000

TABLE OF CONTENTS (Continued)

| <u>Section</u> | <u>Page</u> |
|--|-------------|
| 4.5.2 Alternative 2A--Air Stripping and Re-injection | 4-27 |
| 4.5.2.1 Description of the Alternative | 4-27 |
| 4.5.2.2 Protection of Human Health and the Environment | 4-29 |
| 4.5.2.3 Compliance with ARARs | 4-29 |
| 4.5.2.4 Long-Term Effectiveness and Permanence | 4-29 |
| 4.5.2.5 Reduction in Toxicity, Mobility, or Volume | 4-30 |
| 4.5.2.6 Short-Term Effectiveness | 4-30 |
| 4.5.2.7 Implementability | 4-31 |
| 4.5.2.8 Cost | 4-31 |
| 4.5.3 Alternative 2B--Air Stripping and Discharge to the Sanitary Sewer | 4-31 |
| 4.5.3.1 Description of the Alternative | 4-31 |
| 4.5.3.2 Protection of Human Health and the Environment | 4-33 |
| 4.5.3.3 Compliance with ARARs | 4-33 |
| 4.5.3.4 Long-Term Effectiveness and Permanence | 4-34 |
| 4.5.3.5 Reduction in Toxicity, Mobility, or Volume | 4-34 |
| 4.5.3.6 Short-Term Effectiveness | 4-34 |
| 4.5.3.7 Implementability | 4-34 |
| 4.5.3.8 Cost | 4-35 |
| 4.5.4 Alternative 3--In-Situ Biological Treatment | 4-35 |
| 4.5.4.1 Description of the Alternative | 4-35 |
| 4.5.4.2 Protection of Human Health and the Environment | 4-37 |
| 4.5.4.3 Compliance with ARARs | 4-37 |
| 4.5.4.4 Long-Term Effectiveness and Permanence | 4-37 |
| 4.5.4.5 Reduction in Toxicity, Mobility, or Volume | 4-38 |
| 4.5.4.6 Short-Term Effectiveness | 4-38 |
| 4.5.4.7 Implementability | 4-38 |
| 4.5.4.8 Cost | 4-39 |
| 4.6 Opportunities for Coordination of Remedial Activities | 4-39 |
| 4.6.1 Ground-Water Alternatives | 4-39 |
| 4.6.2 Soil Alternatives | 4-40 |
| 4.6.3 Combined Soil and Ground-Water Alternatives | 4-41 |
| 4.7 Comparative Evaluation of Remedial Alternatives | 4-42 |
| 4.7.1 Matrix Approach | 4-42 |
| APPENDIX A: COST ESTIMATES | A-1 |

LIST OF FIGURES

| <u>Figure</u> | <u>Page</u> |
|---|-------------|
| ES-1 Location of East Area IRP Sites, Carswell AFB, Texas | ES-2 |
| 1-1 Regional Setting of Carswell AFB, Texas | 1-4 |
| 1-2 Location of East Area IRP Sites, Carswell AFB, Texas | 1-5 |
| 1-3 Generalized Hydrogeologic Units, Carswell AFB, Texas | 1-7 |
| 1-4 Potentiometric Surface Map of the Upper Zone, East Area, Carswell AFB, Texas | 1-10 |
| 1-5 Location of Wells Sampled at Site LF01, East Area, Carswell AFB, Texas | 1-14 |
| 1-6 Location of Monitor Wells and Surface Water Samples, Site SD13, East Area, Carswell AFB, Texas | 1-16 |
| 1-7 Probable Extent of Benzene Contamination (Spring 1990), Site ST14, Carswell AFB, Texas | 1-18 |
| 1-8 Location of Monitor Wells, Site BSS, East Area, Carswell AFB, Texas | 1-19 |
| 1-9 Potential Pathways to Human Exposure from Landfill 1, the POL Tank Farm, and the Base Service Station, East Area, Carswell AFB, Texas | 1-28 |
| 1-10 Potential Pathways to Human Exposure from Site SD13, East Area, Carswell AFB, Texas | 1-29 |
| 2-1 Schematic of Air Stripping Treatment System | 2-28 |
| 2-2 Schematic of In-Situ Biological Treatment System | 2-30 |
| 2-3 Schematic of Soil Vapor Extraction System | 2-32 |
| 3-1 Basic Remedial Action Components of Alternative 2A, Site ST14, East Area, Carswell AFB, Texas | 3-8 |
| 3-2 Basic Remedial Action Components of Alternative 2B, Site ST14, East Area, Carswell AFB, Texas | 3-9 |
| 3-3 Basic Remedial Action Components of Alternative 2C, Site ST14, East Area, Carswell AFB, Texas | 3-10 |

044 400

LIST OF FIGURES (Continued)

| <u>Figure</u> | <u>Page</u> |
|--|-------------|
| 3-4 Basic Remedial Action Components of Alternative 3, Site ST14, East Area, Carswell AFB, Texas | 3-13 |
| 3-5 Basic Remedial Action Components for Alternative 4A, Site ST14, East Area, Carswell AFB, Texas | 3-14 |
| 3-6 Basic Remedial Action Components for Alternative 4B, Site ST14, East Area, Carswell AFB, Texas | 3-15 |
| 3-7 Basic Remedial Action Components for Alternative 4C, Site ST14, East Area, Carswell AFB, Texas | 3-16 |
| 3-8 Basic Remedial Action Components for Alternative 5, Site ST14, East Area, Carswell AFB, Texas | 3-18 |
| 3-9 Basic Remedial Action Components for Alternative 2A, Site BSS, East Area, Carswell AFB, Texas | 3-23 |
| 3-10 Basic Remedial Action Components for Alternative 2B, Site BSS, East Area, Carswell AFB, Texas | 3-24 |
| 3-11 Basic Remedial Action Components for Alternative 2C, Site BSS, East Area, Carswell AFB, Texas | 3-25 |
| 3-12 Basic Remedial Action Components for Alternative 3, Site BSS, East Area, Carswell AFB, Texas | 3-26 |
| 3-13 Basic Remedial Action Components for Alternative 4A, Site BSS, East Area, Carswell AFB, Texas | 3-27 |
| 3-14 Basic Remedial Action Components for Alternative 4B, Site BSS, East Area, Carswell AFB, Texas | 3-28 |
| 3-15 Basic Remedial Action Components for Alternative 4C, Site BSS, East Area, Carswell AFB, Texas | 3-29 |
| 3-16 Basic Remedial Action Components for Alternative 5, Site BSS, East Area, Carswell AFB, Texas | 3-30 |
| 4-1 Remedial Alternative 4A, Site ST14, East Area, Carswell AFB, Texas | 4-13 |
| 4-2 Alternative 4B, Site ST14, East Area, Carswell AFB, Texas | 4-17 |
| 4-3 Alternative 5, Site ST14, East Area, Carswell AFB, Texas | 4-21 |
| 4-4 Alternative 2A, Site BSS, East Area, Carswell AFB, Texas | 4-28 |

144-000

LIST OF FIGURES

| <u>Table</u> | | <u>Page</u> |
|--------------|--|-------------|
| 4-5 | Alternative 2B, Site BSS, East Area, Carswell AFB, Texas | 4-32 |
| 4-6 | Alternative 3, Site BSS, East Area, Carswell AFB, Texas | 4-36 |

2014-09-09

LIST OF TABLES

| <u>Table</u> | <u>Page</u> |
|--|-------------|
| ES-1 Summary of Remedial Action Options for the East Area IRP Sites . . | ES-4 |
| ES-2 Preliminary Ground-Water Remedial Alternatives for Site ST14-- POL Tank Farm | ES-5 |
| ES-3 Preliminary Ground-Water Remedial Alternatives for Site BSS-- Base Service Station | ES-6 |
| ES-4 Preliminary Soil Remedial Alternatives for Site ST14--POL Tank Farm and Site BSS--Base Service Station | ES-7 |
| 1-1 Indicator Chemicals for Site LF01--Landfill 1 | 1-25 |
| 1-2 Indicator Chemicals for Site SD13--Unnamed Stream and Abandoned Gasoline Station | 1-25 |
| 1-3 Indicator Chemicals for Site SD14--POL Tank Farm | 1-26 |
| 1-4 Indicator Chemicals for Site BSS--Base Service Station | 1-26 |
| 2-1 Remedial Action Objectives for East Area IRP Sites, Carswell AFB, Texas | 2-3 |
| 2-2 Identification and Screening of Technologies for Waste Material and Contaminated Soil | 2-7 |
| 2-3 Identification and Screening of Technologies for Ground Water | 2-13 |
| 2-4 Identification and Screening of Technologies for Surface Water | 2-22 |
| 2-5 Summary of Remedial Action Options for the East Area IRP Sites | 2-26 |
| 3-1 Preliminary Ground-Water Remedial Alternatives for Site ST14--POL Tank Farm | 3-6 |
| 3-2 Preliminary Soil Remedial Alternatives for Site ST14-- POL Tank Farm | 3-19 |

LIST OF TABLES (Continued)

| <u>Table</u> | <u>Page</u> |
|---|-------------|
| 3-3 Preliminary Ground-Water Remedial Alternatives for Site BSS--Base Service Station | 3-22 |
| 3-4 Preliminary Soil Remedial Alternatives for Site BSS--Base Service Station | 3-32 |
| 4-1 Criteria Scores for Detailed Analysis of Remedial Alternatives . . | 4-44 |
| 4-2 Remedial Alternatives Comparative Evaluation Matrix, Site ST14, East Area, Carswell AFB, Texas | 4-45 |
| 4-3 Remedial Alternatives Comparative Evaluation Matrix, Site BSS, East Area, Carswell AFB, Texas | 4-46 |
| 4-4 Remedial Alternatives Comparative Evaluation Matrix, Site ST14, East Area, Carswell AFB, Texas | 4-47 |
| 4-5 Remedial Alternatives Comparative Evaluation Matrix, Site BSS, East Area, Carswell AFB, Texas | 4-48 |

100-400

EXECUTIVE SUMMARY

Four sites at Carswell Air Force Base, Texas, are the subject of a feasibility study (FS) performed by Radian Corporation for the Human Systems Division at Brooks Air Force Base, Texas.

Those four sites, which were identified in the East Area of Carswell AFB under USAF Installation Restoration Program (IRP), are the following (refer to Figure ES-1):

- Site LF01--Landfill 1;
- Site SD13--Unnamed Stream and Abandoned Gasoline Station;
- Site ST14--POL Tank Farm; and
- Site BSS--Base Service Station.

The FS relied on data obtained during the IRP remedial investigation (RI), various stages of which were performed by Radian between 1988 and 1991; and from the earlier IRP Phase I (CH2M Hill, 1984) and Phase II Stage 1 (Radian, 1986) efforts. Guidance published by the U.S. Environmental Protection Agency in response to the Comprehensive Environmental Response, Compensation, and Liability Act of 1980 (CERCLA) was used to perform the FS.

Benzene, lead, and arsenic were the principal contaminants detected in ground water and surface water samples collected from the East Area sites in 1990. Low concentrations of some additional metals and volatile organic compounds were also detected. Soil sampling and analysis was not required by the scope of work for the 1990 effort, but limited data generated in previous IRP efforts provided inconclusive evidence of soil contamination potentially requiring remediation at Sites ST14 and BSS.

Three remedial action objectives were identified for the FS:

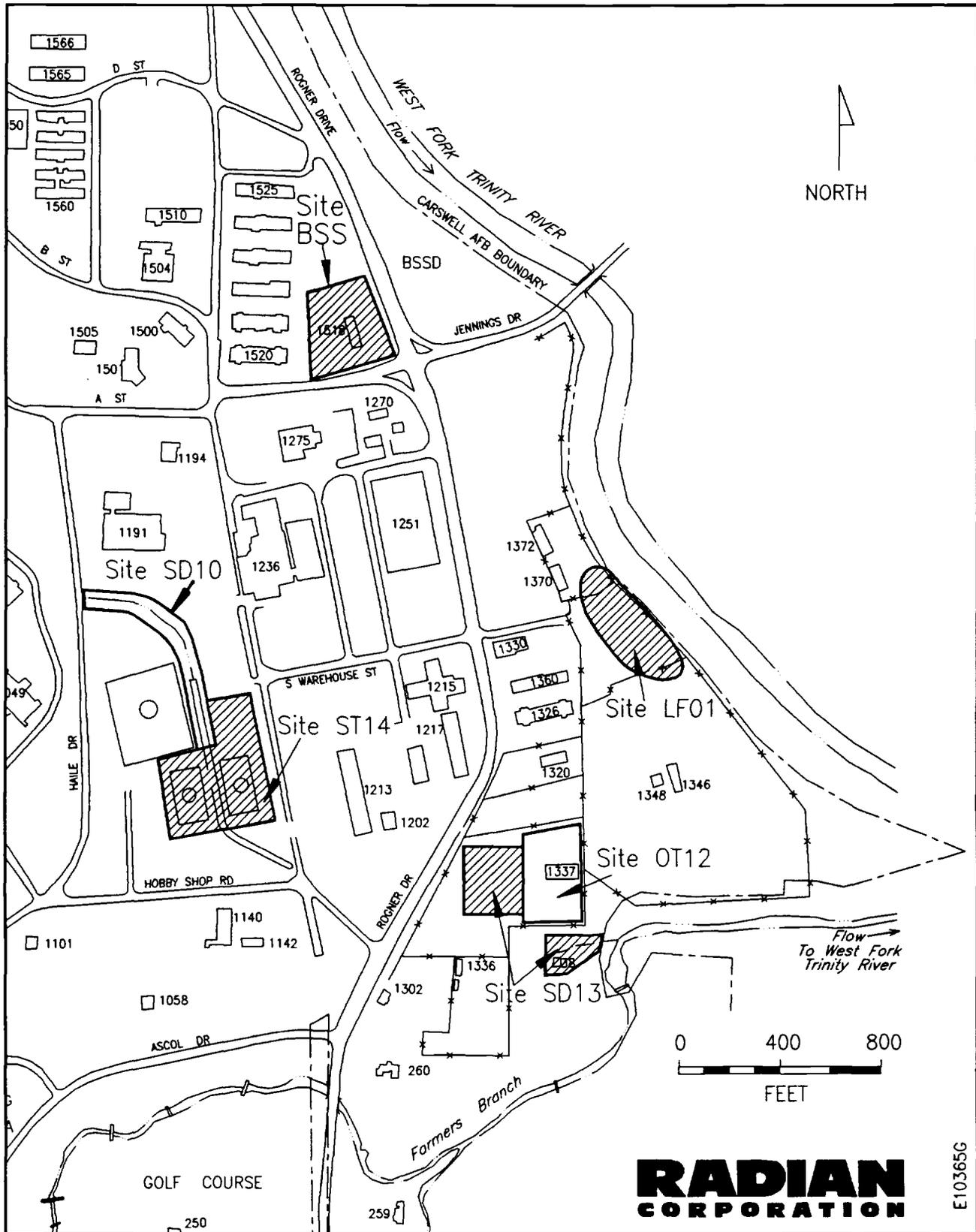


Figure ES-1. Location of East Area IRP Sites, Carswell AFB, Texas
 Note: Only cross-hatched sites are included in the FS

- 1) To reduce or eliminate potential future impacts to human health and the environment;
- 2) To reduce or eliminate the potential for future contaminant migration in the ground water; and
- 3) To reduce or eliminate the potential for continuing mobilization of metals and/or organic contaminants in near-surface soil (Upper Zone deposits) or in residual wastes (as leachate).

These general objectives were developed in detail during the FS.

Potential media-specific response actions, technologies, and process options available for remedying the contamination in the East Area first were identified and then were screened. The screening process eliminated technologies that were inappropriate or that did not meet the criteria of (1) demonstrated performance and effectiveness, (2) constructability and implementability, and (3) cost. Refer to Table ES-1 for a summary of technologies that remained after the screening process. For each site, the potentially applicable technologies were combined into preliminary media-specific remedial alternatives that were developed and screened against the broad criteria of effectiveness, implementability and cost. For Sites LF01 and SD13, the no-action alternative was identified as the only appropriate action. Nine ground-water remedial alternatives (including the no-action alternative) were developed for each of Sites ST14 and BSS. The components of these alternatives are shown in Tables ES-2 and ES-3, respectively. Five preliminary alternatives, potentially applicable to contaminated soil remediation, if required, at Sites ST14 and BSS were also developed (see Table ES-4 for components of each alternative).

TABLE ES-1. SUMMARY OF REMEDIAL ACTION OPTIONS FOR THE EAST AREA
IRP SITES

| | Site | | | |
|---|------|------|------|-----|
| | LF01 | SD13 | ST14 | BSS |
| No Action | ■ | ■ | ■ | ■ |
| <u>Institutional</u> | | | | |
| Long-Term Monitoring | ■ | ■ | ■ | ■ |
| <u>Containment</u> | | | | |
| Hydraulic Barrier (see ground-water extraction) | | | ■ | ■ |
| <u>Ground-Water Extraction</u> | | | | |
| Extraction Well Fields | | | ■ | ■ |
| Interceptor Trenches | | | ■ | ■ |
| <u>Ground-Water Pretreatment</u> | | | | |
| Oil/Water Separator | | | ■ | |
| <u>Primary Ground-Water Treatment</u> | | | | |
| Air Stripping | | | ■ | ■ |
| In-Situ Biological Treatment | | | ■ | ■ |
| <u>Treated Ground-Water Discharge</u> | | | | |
| Discharge to POTW | | | ■ | ■ |
| Discharge to Stream | | | ■ | ■ |
| Aquifer Recharge | | | ■ | ■ |
| <u>Soil Treatment</u> | | | | |
| Soil Vapor Extraction | | | ■ | ■ |
| In-Situ Biological Treatment | | | ■ | ■ |
| Excavation/Soil Piles | | ■ | ■ | ■ |
| <u>Secondary Treatment</u> | | | | |
| Carbon Adsorption | | | ■ | ■ |
| Fume Incineration | | | ■ | ■ |
| <u>Treated Soil Disposal</u> | | | | |
| On Site | | ■ | | ■ |

TABLE ES-2. PRELIMINARY GROUND-WATER REMEDIAL ALTERNATIVES^a FOR
SITE ST14--POL TANK FARM

| Technology | Alternatives | | | | | | | | | |
|----------------------------------|--------------|----|----|----|---|----|----|----|---|---|
| | 1 | 2A | 2B | 2C | 3 | 4A | 4B | 4C | 5 | |
| Monitoring | • | • | • | • | • | • | • | • | • | • |
| Interceptor Trenches | NA | • | • | • | • | | | | | |
| Extraction Wells | NA | | | | | • | • | • | • | |
| Oil/Water Separator | NA | • | • | • | • | • | • | • | • | |
| Air Stripping | NA | • | • | • | | • | • | • | | |
| In-Situ Bio-Treatment | NA | | | | • | | | | | • |
| Treated Ground-Water ReInjection | NA | • | | | • | • | | | | • |
| Ground-Water Disposal to POTW | NA | | • | | | | • | | | |
| Ground-Water Discharge to Stream | NA | | | • | | | | | • | |

NA - No Action

^a Preliminary remedial alternatives do not include secondary ground-water treatment (i.e., fume incineration or carbon adsorption for stripped contaminants).

TABLE ES-3. PRELIMINARY GROUND-WATER REMEDIAL ALTERNATIVES^a FOR
SITE BSS--BASE SERVICE STATION

| Technology | Alternatives | | | | | | | | |
|----------------------------------|--------------|----|----|----|---|----|----|----|---|
| | 1 | 2A | 2B | 2C | 3 | 4A | 4B | 4C | 5 |
| Monitoring | • | • | • | • | • | • | • | • | • |
| Interceptor Trenches | NA | • | • | • | • | | | | |
| Extraction Wells | | | | | | • | • | • | • |
| Air Stripping | NA | • | • | • | | • | • | • | |
| In-Situ Bio-Treatment | NA | | | | • | | | | • |
| Treated Ground-Water ReInjection | NA | • | | | • | • | | | • |
| Ground-Water Disposal to POTW | NA | | • | | | | • | | |
| Ground-Water Discharge to Stream | NA | | | • | | | | • | |

NA = No Action

^a Preliminary remedial alternatives do not include secondary ground-water treatment.

TABLE ES-4. PRELIMINARY SOIL REMEDIAL ALTERNATIVES^a
 FOR SITE ST14--POL TANK FARM AND SITE BSS--
 BASE SERVICE STATION

| Technology | Alternatives | | | | |
|-------------------------------|--------------|----|----|---|---|
| | 1 | 2A | 2B | 3 | 4 |
| Confirmation Sampling | • | • | • | • | • |
| Excavation | NA | | | • | |
| In-Situ Bio-Treatment | NA | | | | • |
| Soil Vapor Extraction | NA | • | • | | |
| Extraction Trenches | NA | • | | | |
| Extraction Wells | NA | | • | | |
| Soil Piles | NA | | | • | |
| On-Site Treated Soil Disposal | NA | | | • | |

NA - No Action

^a If required, pending results of additional soil sampling and analysis--
 preliminary remedial alternatives do not include secondary treatment.

As a result of the alternatives screening, for Sites LF01 and SD13 only the no-action alternative was retained for detailed evaluation. For Site ST14, the no-action alternative (Alternative 1), two air stripping alternatives (Alternatives 4A and 4B) and one in-situ biological treatment alternative (Alternative 5) were retained for detailed evaluation. For Site BSS, the no-action alternative (Alternative 1), two air stripping alternatives (Alternatives 2A and 2B) and one in-situ biological treatment alternative (Alternative 3) were retained for detailed evaluation. Because of data limitations, the preliminary soil remedial alternatives cannot undergo detailed analysis until additional data become available.

The detailed analysis of ground-water alternatives was then performed for the four East Area sites, using the evaluation criteria established by CERCLA:

- Overall protection of human health and the environment;
- Compliance with applicable or relevant and appropriate requirements (ARARs);
- Long-term effectiveness and permanence;
- The reduction of toxicity, mobility, or volume through treatment;
- Short-term effectiveness;
- Implementability; and
- Cost.

(The two remaining CERCLA criteria, state and community acceptance, will be evaluated in the Record of Decision.)

The FS concluded with a comparative (matrix) evaluation of alternatives for Sites ST14 and BSS. The most cost-effective alternative for Site ST14 was determined to be Alternative 5. The most cost-effective alternative for Site BSS was determined to be Alternative 3. The no-action alternative is the appropriate action for Sites LF01 and SD13.

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1.0 INTRODUCTION

In partial fulfillment of the requirements of the Scope of Work (SOW) for Delivery Order 04, Modification 05 of Contract No. F33615-87-D-4023 with the U.S. Air Force, Radian Corporation (Radian) performed a Feasibility Study (FS) for remediation of environmental contamination present in the East Area of Carswell AFB, Texas. Six former waste disposal/release sites within the East Area have been studied and characterized with respect to the nature and extent of contamination, if any, associated with each under the Air Force Installation Restoration Program (IRP). The East Area IRP sites are:

- Site LF01--Landfill 1;
- Site SD10--Flightline Drainage Ditch;
- Site OT12--Entomology Dry Well;
- Site SD13--Unnamed Stream and Abandoned Gasoline Station;
- Site ST14--POL Tank Farm; and
- Site BSS--Base Service Station.

Data obtained in the earlier IRP investigations were sufficient to prepare a decision document (Radian, 1990a) identifying the recommended remedial alternative and a detailed remedial design and specifications for Site SD10; and for Carswell AFB personnel to complete final site characterization activities (soil sampling and analysis) to confirm the absence of contamination prior to planned construction at Site OT12. These sites are therefore not included in this FS. A second decision document (Radian, 1990b), outlining the preliminary basis for recommendation of an appropriate remedial alternative for Site BSS, was also prepared. An additional round of groundwater samples was collected from existing Site BSS monitor wells and analyzed in the 1990 effort. The results generally support the remedial alternative presented in the decision document (Radian, 1990b), but because no additional soil sampling was included in the SOW received by Radian for the additional effort, the need for and potential magnitude of a soils remedial action remains unresolved. Sites LF01, SD13, and ST14 are the remaining East Area sites addressed by this FS. Because the contaminants detected at Sites SD13 and ST14 are similar in nature, and because they are probably at least

partially related to a common source in the POL Tank Farm (Site ST14), the remedial technologies and alternatives identified for the POL Tank Farm will also affect Site SD13. As in the case of Site BSS, no additional soil sampling at Site ST14 was authorized in the 1990 effort. Therefore, the need for and potential magnitude of any soils remedial action in the POL Tank Farm requires resolution prior to detailed design of a remedial alternative.

1.1 Purpose and Organization of Report

The purpose of this report is to document the procedures and findings of the FS, which was performed in accordance with the U.S. EPA Guidance for Conducting Remedial Investigations and Feasibility Studies Under CERCLA (Interim Final) (EPA, 1988). Activities performed in the FS and documented in this report include:

- Identification and screening of remedial technologies;
- Development and screening of remedial alternatives; and
- Detailed evaluation of alternatives for remediation of Upper Zone ground-water contamination in the East Area.

Background information pertaining to the general hydrogeologic setting of Carswell AFB and to site-specific conditions in the East Area, summarized from the RI report (Radian, 1991), is provided in Section 1.2. Section 2 presents the results of the identification and screening of technologies applicable to contamination in the East Area. Remedial action objectives (RAOs) and remedial technologies are presented in Sections 2.1 and 2.2, respectively. Section 2.3 provides a list of the technologies remaining after screening and provides more detailed descriptions of these technologies as they could be implemented at one or more of the East Area sites.

Section 3 describes the basis for developing media-specific alternatives (Section 3-1) and the results of the alternatives screening evaluation (Section 3.2). Because insufficient data are available to perform a detailed

evaluation of soils remedial alternatives, preliminary soils alternatives are developed and screened on a qualitative basis only. This approach is consistent with CERCLA guidance. Section 4 presents the detailed evaluation of ground-water remedial alternatives for Sites LF01, SD13, ST14, and BSS. The CERCLA evaluation criteria and methodology are described in Section 4.1. Feasible alternatives for remediation of ground water remaining after the initial screening are developed by site and are evaluated individually against the CERCLA evaluation criteria (Sections 4.2 through 4.5). Section 4.6 discusses possibilities for and benefits of coordinating remedial actions at multiple sites. The alternatives are evaluated on a comparative basis in Section 4.7.

1.2 Background Information

Most of the background information contained in this section is based on the most recent data from the East Area (Radian, 1991), combined with information summarized from earlier IRP reports (CH2M Hill, 1984; Radian, 1986, 1989).

Carswell AFB is located six miles west of Fort Worth in Tarrant County, Texas (Figure 1-1). The base is bordered by Lake Worth to the north, the West Fork of the Trinity River and the community of Westworth to the east and southeast, and Air Force Plant 4 (AF Plant 4) to the west. Figure 1-2 shows the location of the East Area IRP sites.

Five major hydrogeologic units exist beneath Carswell AFB. From shallowest to deepest they are: 1) an Upper Zone of unconfined ground water occurring within the alluvial terrace deposits associated with the Trinity River; 2) an aquitard of predominantly dry limestone of the Goodland and Walnut Formations; 3) an aquifer in the Paluxy Sand; 4) an aquitard of relatively impermeable limestone in the Glen Rose Formation; and 5) a major aquifer in the sandstone of the Twin Mountains Formation. The Upper Zone was the only unit studied in this most recent Stage 2 site characterization (1990) effort. During a previous IRP effort, two monitor wells installed in the

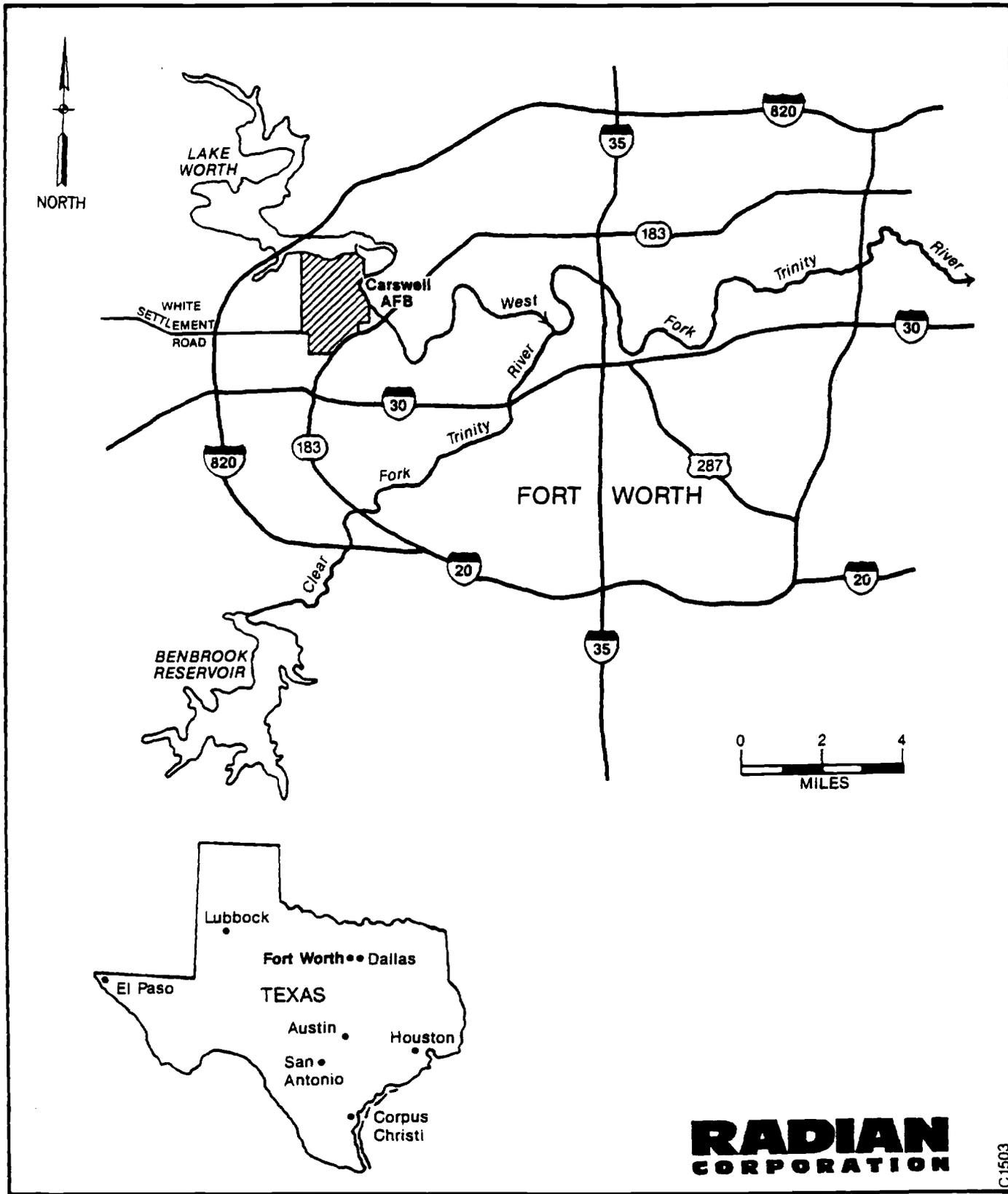


Figure 1-1. Regional Setting of Carswell AFB, Texas

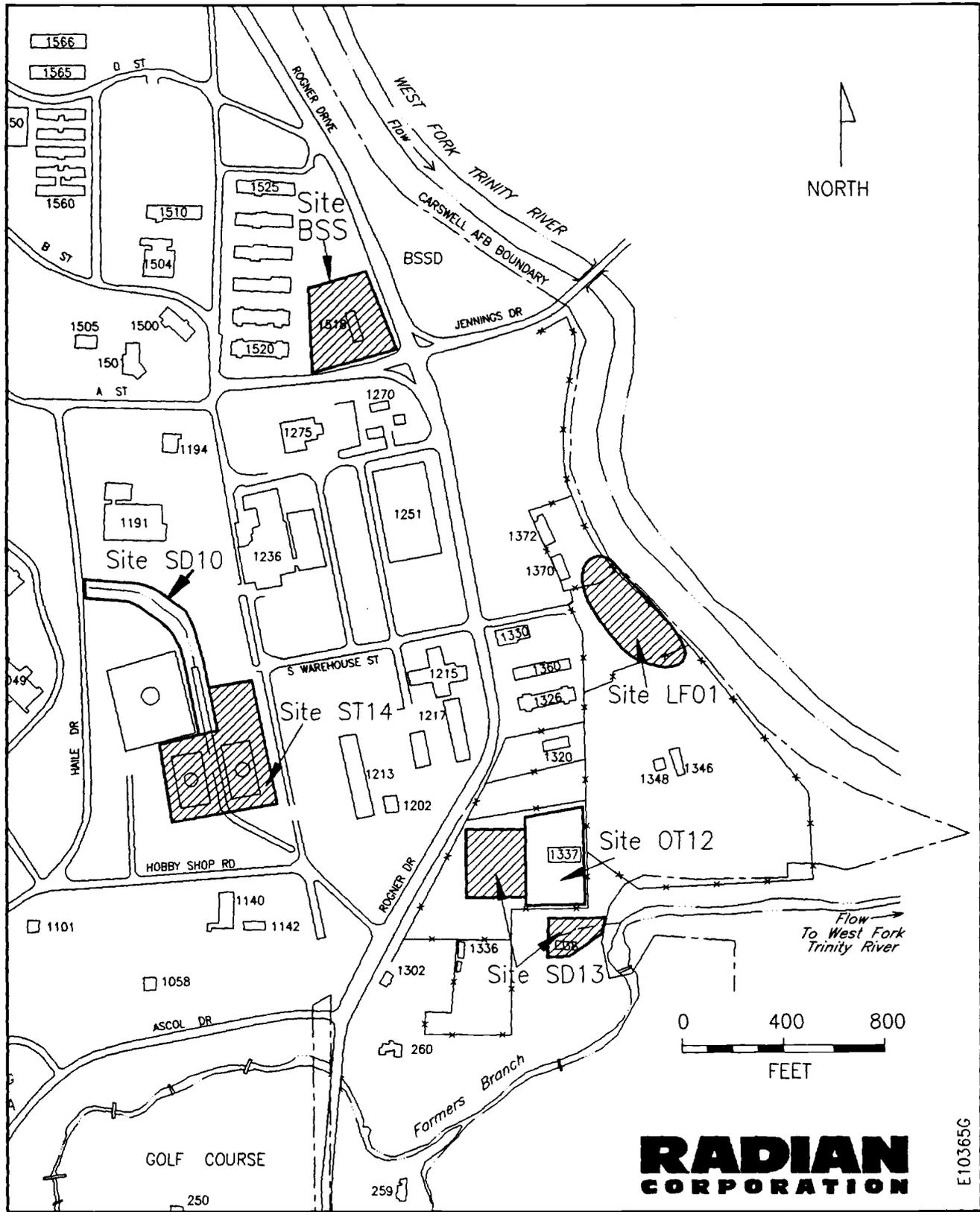


Figure 1-2. Location of East Area IRP Sites, Carswell AFB, Texas
 (Note: Only cross-hatched sites are included in the FS)

Paluxy Aquifer in the Flightline Area of the base and sampled in 1988 provided no evidence of deeper ground-water contamination (Radian, 1989). Figure 1-3 shows the general depth of occurrence and thickness of each of the major hydrogeologic units expected in the East Area. The following subsections present the hydrogeologic characteristics of the Upper Zone formation and the Goodland/Walnut Aquitard that lies beneath it.

The Upper Zone ground water occurs within the alluvial deposits at Carswell AFB. Low permeability is typical of this alluvium; however, there are zones of greater permeability corresponding to sands and gravels of former channel deposits. Recharge to the water-bearing deposits is local, from rainfall and infiltration from stream channels and drainage ditches. The direction of ground-water flow is generally controlled by the bedrock topography of the Walnut Formation, and to a lesser extent by land surface topography.

The Upper Zone ground water is separated from deeper aquifers by the low-permeability limestones and shales of the Goodland Limestone and Walnut Formation. The aquitard is composed of moist clay and shale layers interbedded with dry limestone beds. The thickness of the Goodland/Walnut aquitard is approximately 30-40 feet beneath the Flightline Area at Carswell AFB. This thickness range is based on two monitor wells drilled through the aquitard and completed in the Paluxy Aquifer during the initial Stage 2 study (Radian, 1989). No corresponding information is available for the East Area, where all subsurface borings were terminated at or above the top of bedrock.

1.2.1 East Area Description

The East Area is located on land that gently slopes eastward to the West Fork of the Trinity River and southward to Farmers Branch. Elevations range from 595 feet MSL west of the POL Tank Farm (Site ST14) to 560 feet MSL on the flood plain above the West Fork of the Trinity River and Farmers Branch.

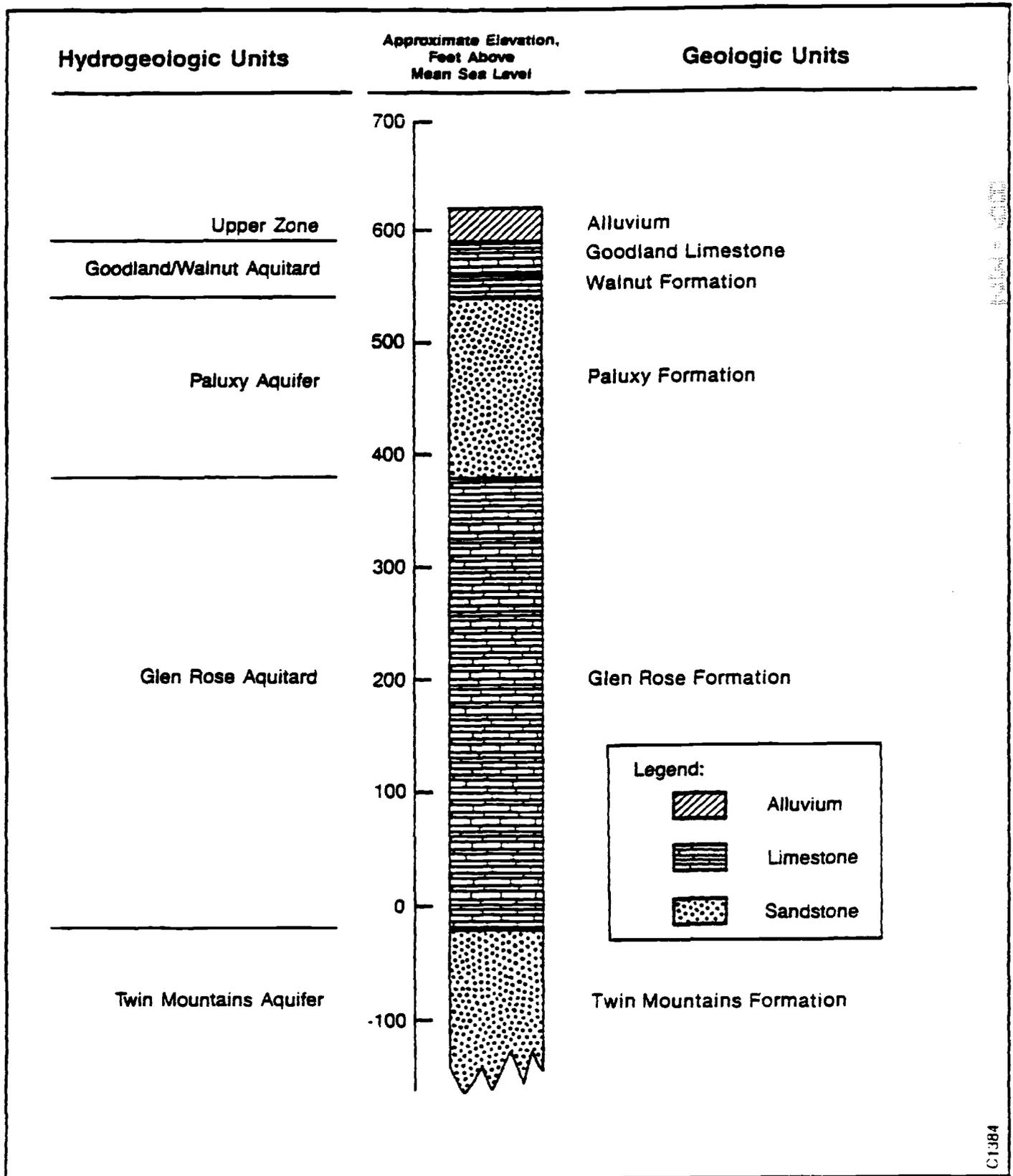


Figure 1-3. Generalized Hydrogeologic Units, Carswell AFB, Texas (Radian, 1989)

The Soil Conservation Service (SCS) has identified three soil associations in the East Area of Carswell AFB (USDA, 1981). The clayey soils of the Sanger-Purves-Slidell association occur in the western portion of the East Area at Site ST14. Approaching the Trinity River, the Bastsil-Silawa loamy soils are prevalent in the nearly level to sloping stream terrace sections found at Sites SD13 and Site BSS, while the Frio-Trinity association of clayey soil occurs in the nearly level flood plain environment in the easternmost portion of Site LF01. The reported permeabilities of the surficial soils range from $<4.2 \times 10^{-5}$ to 3×10^{-3} cm/sec (USDA, 1981).

The main surface water bodies in the East Area are the West Fork of the Trinity River, Farmers Branch, and Unnamed Stream at Site SD13 (Figure 1-2). Surface drainage at Sites LF01 and BSS is toward the Trinity River, with drainage at Sites ST14 and SD13 being mainly toward Farmers Branch.

Water in Unnamed Stream emerges from an oil/water separator. Water enters the separator from a french drain which was installed to intercept fuel spills and/or leaks from the POL Tank Farm (Site ST14). Unnamed Stream is a perennial stream feeding into Farmers Branch.

The Upper Zone alluvial deposits in the East Area generally consists of 5 to 15 feet of gray to black clay and clayey silt overlying, 2 to 10 feet of fine-grained sand, and up to 5 feet of gravel. The underlying Goodland Formation is usually encountered between 7 and 20 feet below ground level (bgl), although it occurred deeper in some wells. In general, across the East Area the depth to the Goodland decreases as the West Fork of the Trinity River is approached. However, within 400 feet of the river, the trend reverses and the depth to bedrock may exceed 20 feet. The Goodland in the East Area is dry and occurs as gray, hard limestone and as blue-gray, mottled shale. No monitor wells were drilled in the East Area that penetrated through the Goodland and Walnut Formations into the Paluxy Aquifer.

The depth to Upper Zone ground water in the East Area ranges from about 6 to 13.5 feet bgl. A potentiometric surface map for the Upper Zone of the East Area, based on a synoptic water level survey performed on 18 June

1990, is presented in Figure 1-4. The ground-water surface generally slopes from west to east, indicating ground-water flow toward the West Fork of the Trinity River or Farmers Branch. The direction of ground-water flow in the Upper Zone is apparently controlled principally by the elevation of the upper surface of the Goodland Limestone. Hydraulic conductivities of the Upper Zone materials, based on slug tests in six East Area monitor wells, range from about 1.2×10^{-2} cm/sec to 1×10^{-5} cm/sec (Radian, 1989).

1.2.2 Site History

The physical features and historical uses of each of the four East Area IRP sites included in this FS are summarized below. The descriptions of these sites and the wastes reportedly disposed of or released from each are taken mainly from the Phase I Records Search (CH2M Hill, 1984).

Site LF01--Landfill 1

Landfill 1 is reportedly the original base landfill and was operated during the 1940s. The site is located adjacent to the West Fork of the Trinity River levee at the current location of the Defense Reutilization and Marketing Office (DRMO) storage yard. Due to its age, no records were found concerning past waste disposal practices. However, analytical data obtained in the IRP studies performed to date suggest solvent- and metal-bearing wastes may have been disposed of in this landfill.

Site SD13--Unnamed Stream and Abandoned Gasoline Station

Site SD13 consists of two areas: a paved lot near an abandoned gasoline station located west of the former Entomology Dry Well (Site OT12) and Unnamed Stream itself. Unnamed Stream is a small tributary of Farmers Branch that emerges from an underground oil/water separator (Facility 38). The stream and the separator are located south of the communications building (No. 1337) and immediately south of the fenced civil engineering storage yard. The oil/water separator is connected to a french drain system which was

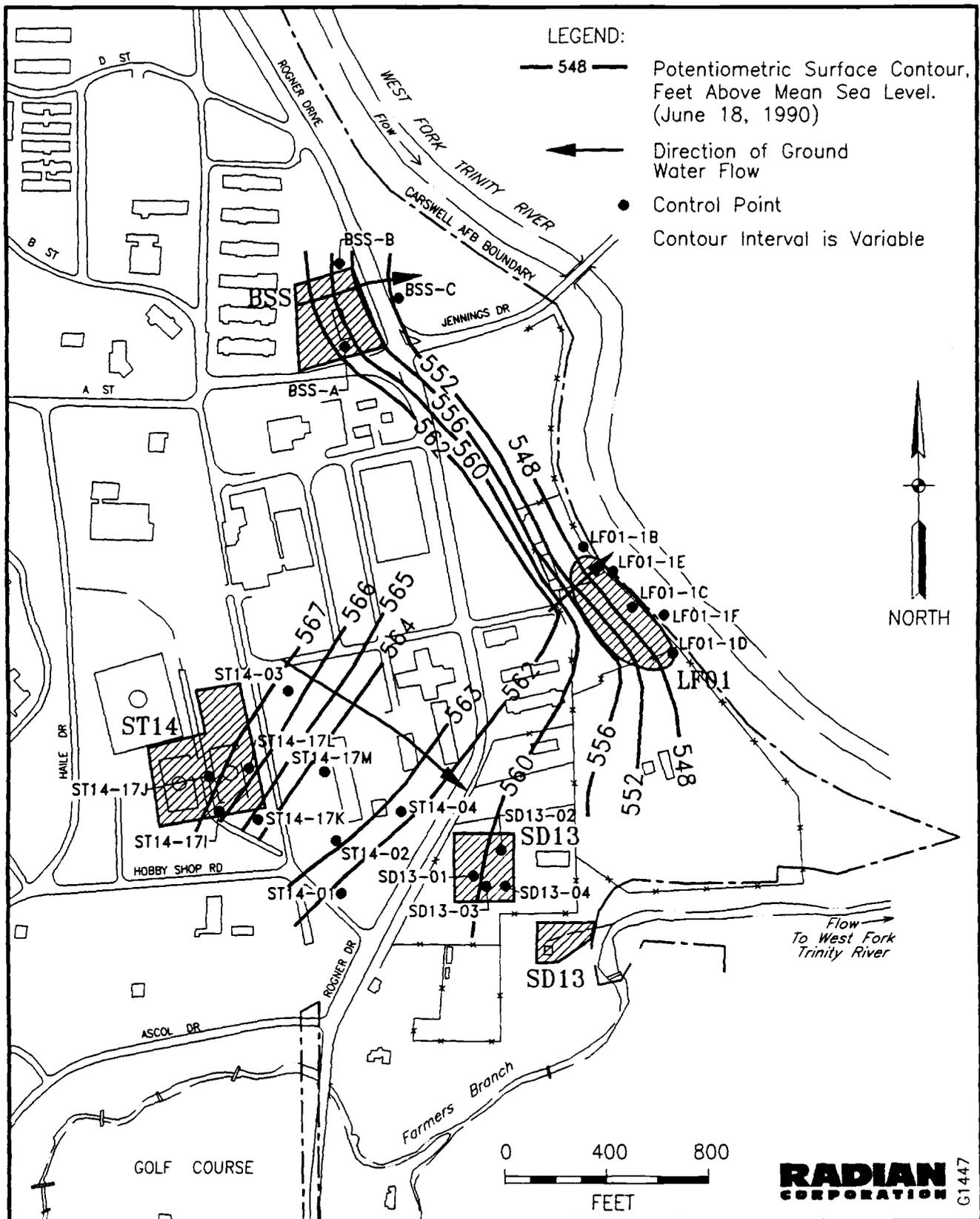


Figure 1-4. Potentiometric Surface Map of the Upper Zone, East Area, Carswell AFB, Texas

reportedly built in 1965 to intercept hydrocarbon products leaking from the POL Tank Farm into sewer pipes. The location of the french drain has been approximated, but is not documented in available base records. Unnamed Stream is perennial, receiving flow from ground water entering the french drain and discharging from the separator.

Site ST14--POL Tank Farm

The POL Tank Farm is located along Knights Lake Road, near the Carswell AFB main gate. The site is occupied by two above-ground fuel storage tanks. Three additional tanks were formerly located at this site, but have been dismantled. During the early 1960s, fuel was discovered in the ground at this area and downgradient of the site. A french drain system was installed in the downgradient area to collect the released fuel. The french drain discharged through the oil/water separator at Site SD13 (Section 1.2.2). At that time, the leaking underground pipes were reportedly located and replaced. No other fuel releases were reported after 1965, but the french drain system continues to collect residual hydrocarbon constituents which are discharged through the oil/water separator. As previously noted, the exact location of the french drain is unknown.

Site BSS--Base Service Station

The Base Service Station is located on the northwest corner of Rogner Drive and Jennings Drive. Gasoline is stored in four 10,000-gallon, fiberglass reinforced plastic underground tanks located north of the pump islands. Surface drainage from Site BSS flows to culverts adjacent to Rogner Drive. The Base Service Station has been in operation for less than 20 years. It was constructed to replace the abandoned service station located at Site SD13. The main contaminants identified at Site BSS are petroleum fuel and fuel derivatives.

1.2.3 Nature and Extent of Contamination

The Carswell AFB IRP Phase II Stage 1 report (Radian, 1986) identified volatile organic compounds and metals at several sites in the East Area. Additional work was performed during Stage 2 (1987-88) to define the concentration distribution and extent of detected contaminants and to investigate other sites (e.g., Site BSS) with the potential for subsurface contamination. The four sites included in this report had additional work performed in 1990.

Ground-water and surface water samples collected during the 1990 field program were analyzed for various volatile organic compounds and metals species. Metals analyses were performed on both unfiltered and filtered samples to evaluate concentrations of total and dissolved metals, respectively. In previous IRP investigations conducted by Radian, only total metals analyses were required. Total metals analyses yield results that are not representative of the dissolved concentrations of metals in water and therefore, can lead to erroneous conclusions regarding water quality.

Concentrations of both volatile organic compounds and inorganic constituents in ground-water and surface water samples collected in 1990 were generally lower than concentrations of the same analytes determined in previous IRP studies. This trend may be the result of natural attenuation of these constituents in the ground-water or surface water systems. However, it should be noted that the weeks immediately preceding the spring 1990 sampling event were characterized by abnormally high precipitation (and flooding). It is possible that temporarily increased infiltration and recharge may have resulted in some dilution of contaminant concentrations.

Since the wastes and historically detected contaminants vary from site to site, not all samples were analyzed for the same suite of chemical constituents. Therefore, the nature (and extent) of contaminants is most conveniently discussed on a site-specific basis. The Informal Technical Information Report (ITIR) for the current effort includes complete analytical summary tables, QA/QC data, sample cross-reference tables, and chain-of-

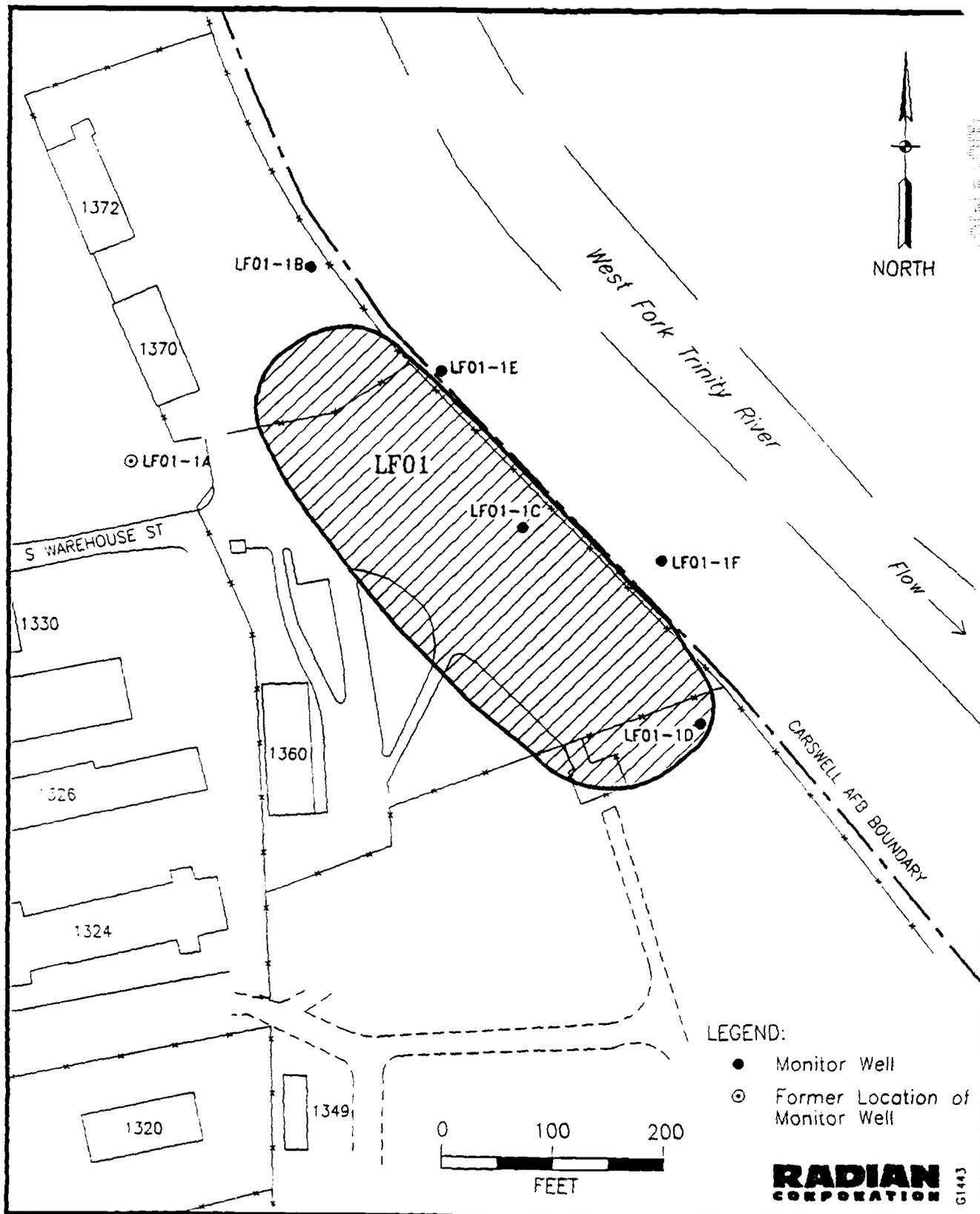


Figure 1-5. Location of Wells Sampled at Site LF01, East Area, Carswell AFB, Texas

04-08

Volatile organic compounds were detected in both rounds of ground-water samples collected during Stage 2. Trichloroethene (TCE) and vinyl chloride were detected in several wells at levels below their MCLs. No definable volatile organic contaminant plume was identified beneath Site LF01, because the distribution of detected compounds was sporadic, and the detected concentrations were very low. Similar results were obtained in 1990. Vinyl chloride; cis-1,2-DCE; and chlorobenzene were detected, but only vinyl chloride was detected in more than one well. All concentrations were below MCLs and were at or less than five times their respective detection limits. Such low concentrations have a high degree of uncertainty associated with them.

1.2.3.2 Site SD13--Unnamed Stream and Abandoned Gasoline Station

IRP activities conducted at Site SD13 in 1985 revealed high levels of organic compounds in grab samples of ground water collected from three soil borings. These constituents were suspected to be from petroleum releases associated with the abandoned gasoline station at the site. However, in 1990, when monitor wells were installed at the site and sampled, the volatile organic compound results did not confirm this hypothesis. No volatile organic compounds or metals were detected above MCLs in ground-water samples from Site SD13.

No volatile organic compounds were detected above MCLs in the surface water samples from Site SD13. The analytical results for inorganic constituents and field observations suggest that metals in Unnamed Stream are preferentially adsorbed to sediments rather than remaining dissolved in the surface water (Radian, 1989; 1991). Total concentrations of arsenic, lead, and selenium were detected above MCLs in at least one surface water sample, but only selenium was reported above the MCL in any dissolved metals analysis. This result was subsequently determined to be a reporting error; the actual concentration was below detection. Locations of monitor wells and surface water sampling points at Site SD13 are shown in Figure 1-6.

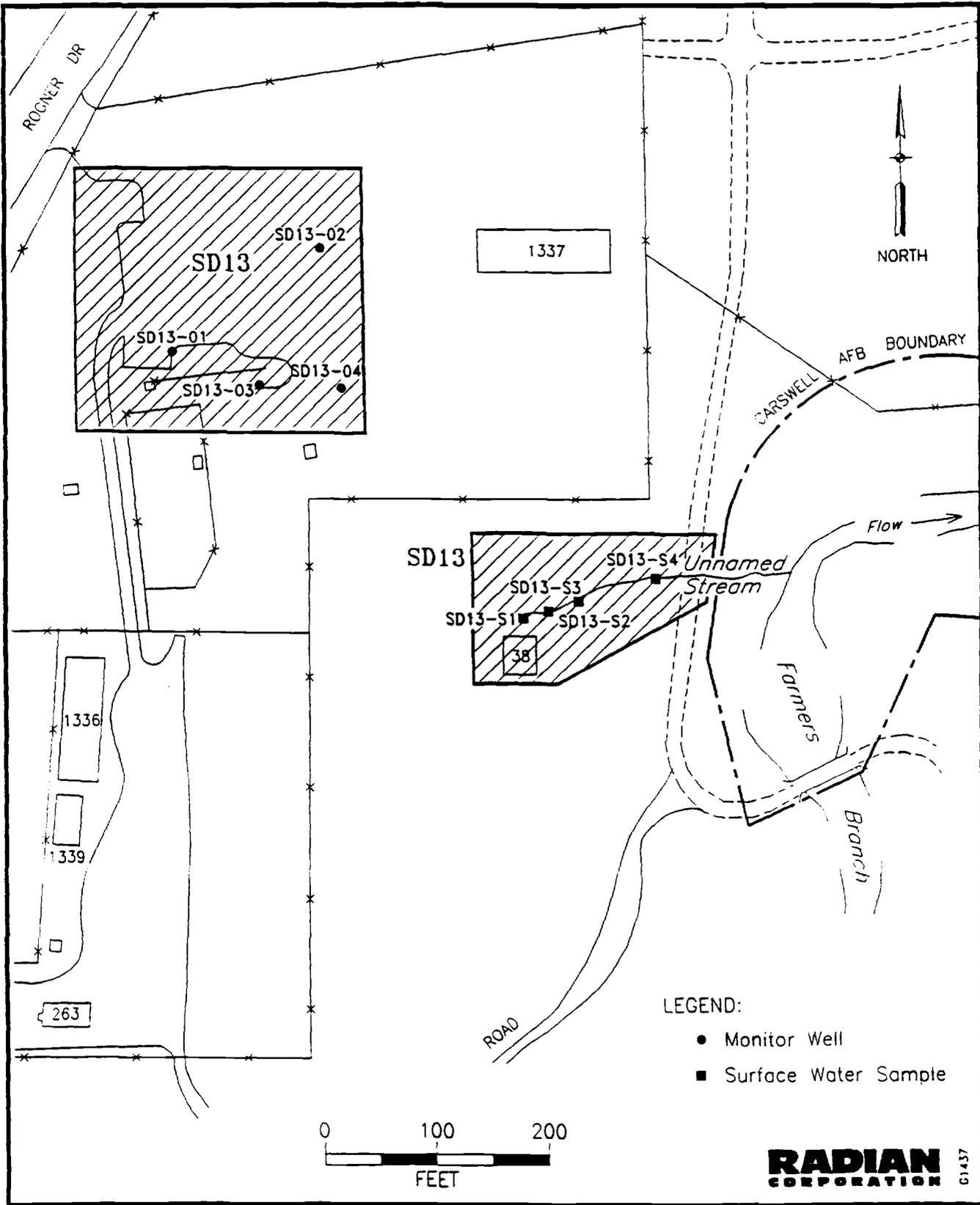


Figure 1-6. Location of Monitor Wells and Surface Water Samples, Site SD13, East Area, Carswell AFB, Texas

1.2.3.3 Site ST14--POL Tank Farm

Benzene, ethylbenzene, chlorobenzene, toluene, and total xylenes were detected in the ground water at Site ST14. Of these, ethylbenzene was the most common. However, benzene was the only volatile organic compound detected at a concentration which exceeded its MCL. Figure 1-7 depicts the probable extent of benzene contamination at Site ST14, interpreted from the 1990 analytical data and the distribution of soil gas determined in an earlier survey (Radian, 1989). Two separate plumes of benzene are suggested. These plumes are roughly coincident with the two plumes interpreted earlier (Radian, 1989). The ground-water sample from monitor well ST14-17M, located at the center of the benzene plume beneath the fuel loading facility, had the highest concentration of benzene, and the only concentration in excess of the MCL. More than 2 feet of free-phase hydrocarbon was floating on the water in monitor well ST14-17M at the time of the 1990 sampling. The highest concentrations of chlorobenzene, toluene, and total xylenes were also detected in this well.

Chromium was detected above its MCL in only one well at Site ST14, and this concentration was measured in the total metals analysis. Lead was detected above MCLs in three monitor well samples at Site ST14, but only one analysis was for dissolved metals. The single dissolved lead concentration above the MCL was analyzed by atomic absorption (AA) and is considered suspect because it was higher than the corresponding total lead concentration. Lead was not detected in either the filtered or unfiltered samples from the same well that were analyzed by inductively coupled plasma emission spectroscopy (ICPES).

1.2.3.4 Site BSS--Base Service Station

Figure 1-8 shows the locations of the three monitor wells at site BSS sampled most recently in 1990. Both volatile organic compounds and metals were identified at Site BSS. In the previous Stage 2 investigation (Radian, 1989), volatile organic compounds were detected primarily in ground-water samples from monitor well BSS-B. In samples collected during the spring 1990

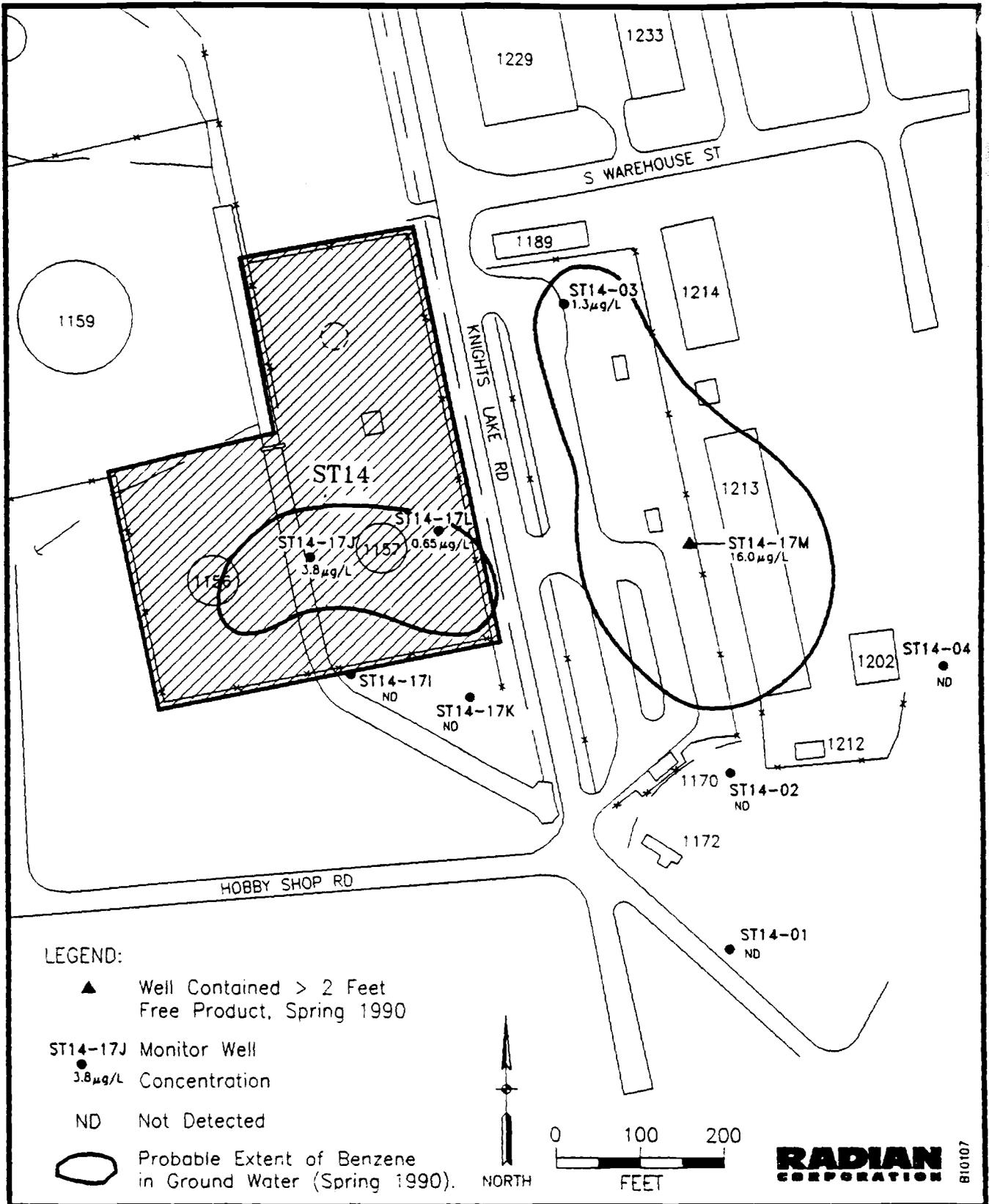


Figure 1-7. Probable Extent of Benzene Contamination (Spring 1990), Site ST14, East Area, Carswell AFB, Texas

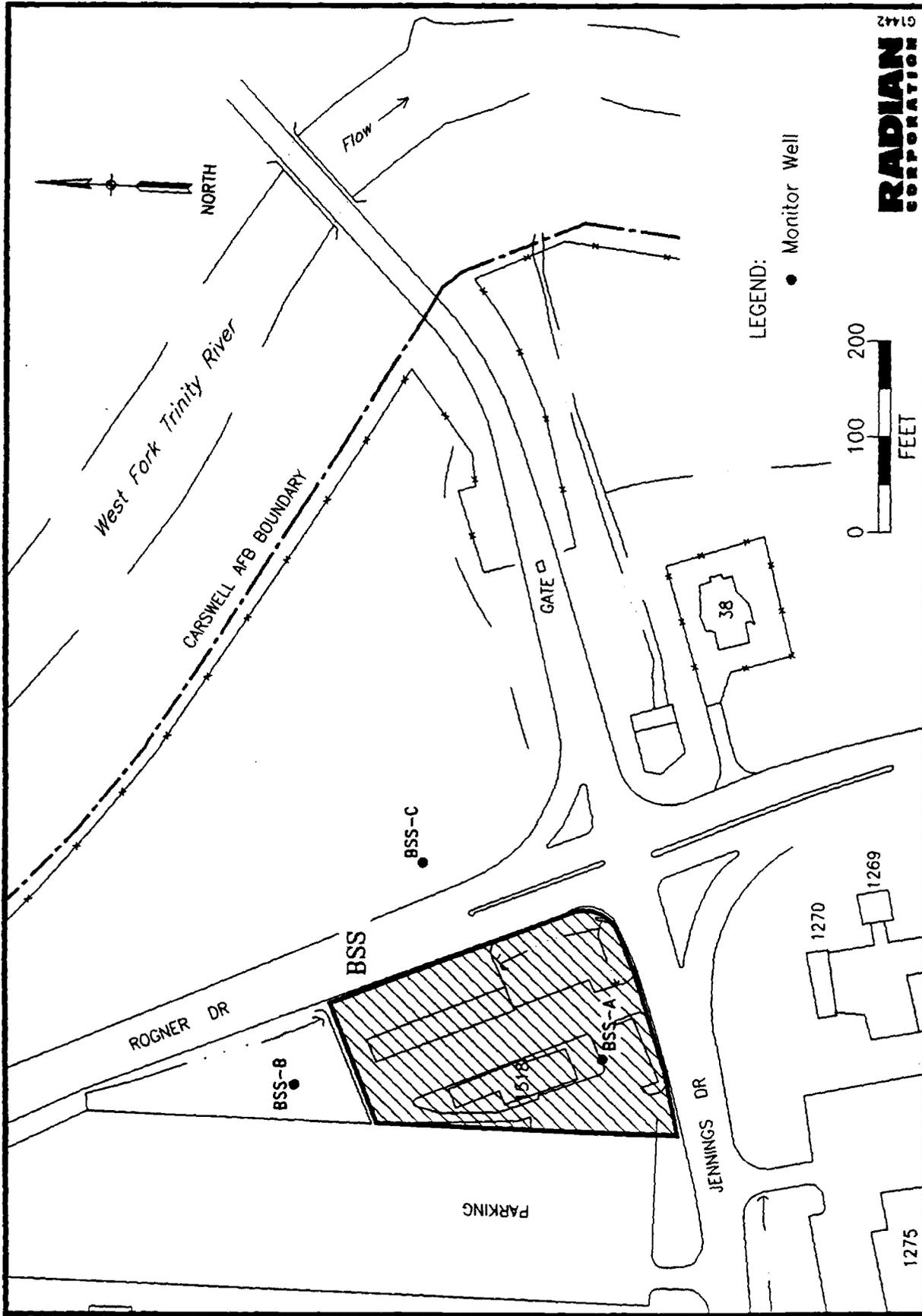


Figure 1-8. Location of Monitor Wells, Site BSS, East Area, Carswell AFB, Texas

sampling event, volatile organic compounds were detected only in this well. The 1990 analytical results confirm the localized nature of the volatile organic contamination and support the interpretation that past leakage from the underground storage tank(s) adjacent to monitor well BSS-B is the main source of the observed contamination.

In the 1990 sampling event, cadmium was detected above the MCL in monitor well BSS-C in the total metals analysis. Cadmium was not detected in any other well, or in the filtered sample (dissolved metals fraction) from the same well. Therefore, there is insufficient evidence to conclude there is ground-water contamination by cadmium (or by any other metals) at the site.

1.2.4 Contaminant Fate and Transport

Ground-water and surface water sampling and analysis conducted in the East Area in 1990 revealed volatile organic contamination at levels above MCLs in Upper Zone ground water at two sites (Site ST14 and Site BSS). No confirmed contaminants were detected above MCLs in the surface water in Unnamed Stream (Site SD13). The fate and transport mechanisms for the main detected analytes are discussed in the following sections.

1.2.4.1 Fate of Main Analytes Detected in the East Area

Benzene and lead were the principal ground-water constituents occurring in excess of MCLs in the East Area sites. Total concentrations of arsenic and lead were identified above MCLs in the surface water at Site SD13. In general these constituents exhibit the following characteristics relative to fate in ground-water and/or surface water systems:

- Benzene is relatively soluble in water, and is relatively inactive chemically. Volatilization is the principal means of removal of benzene from ground water. It also biodegrades slowly in ground water.

- Lead may be removed from the ground water up to 100 percent by the formation of organic complexes and other compounds with high affinities to adsorb onto soil grains and/or low solubility coefficients. As such, lead will tend to accumulate in soils near sources. Lead in surface water may also be removed through bioaccumulation.
- Arsenic has a high chemical activity, and cycles through the surface water system by sorption and desorption from soil grains and the formation of various compounds and complexes. Due to this high activity, little arsenic is removed from the surface water by these processes. However, arsenic may be removed from surface water by bioaccumulation.

1.2.4.2 Contaminant Transport Pathways

Following is a site-by-site discussion of the various contaminants found in the East Area and the transport mechanisms through the ground-water and surface water systems.

Site LF01--Landfill 1

Recent ground-water sampling results show very low levels of vinyl chloride and cis-1,2-dichloroethene (1,2-DCE) in wells LF01-1C and LF01-1F. Ground-water samples collected in 1988 contained very low levels of trichloroethene (TCE) and vinyl chloride.

Since there is no historical record indicating the use of cis-1,2-dichloroethene or vinyl chloride at Carswell AFB, the small quantities of these compounds in ground water are likely to be the result of the chemical and biological breakdown of TCE, which was detected in the 1988 study. Although several metals were detected in the ground water at total concentrations exceeding MCLs during the 1988 investigation (Radian, 1989), there were no metals (dissolved or total) detected above MCLs in the 1990 sampling.

The low levels of volatile organic contaminants in the Upper Zone ground water would be expected to move downgradient to the east, toward the West Fork of the Trinity River. Shallow ground-water flow near the river probably will be discharged at the surface as broadly diffuse seepage, much of which will be consumed by evapotranspiration. There is no visual evidence of seepage at the land surface between Site LF01 and the river. Shallow ground-water flow is not expected to be downward, to deeper aquifers (because of the Goodland/Walnut aquitard beneath the Upper Zone), or laterally beyond the river. Any contaminants which reach the river by ground-water migration would move downstream with the surface water flow. Any VOCs present in the surface water will be subject to volatilization to the air. Since the detected concentrations of volatile organic compounds in ground water are already low (in most cases at levels less than five times their detection limits), it is unlikely that these compounds would be detectable following their introduction into the West Fork of the Trinity River.

Site SD13--Unnamed Stream and Abandoned Gasoline Station

Any contaminants in the ground water would be expected to move hydraulically downgradient, eventually entering either Unnamed Stream or Farmers Branch, and finally discharging into the West Fork of the Trinity River. Any VOCs discharged into the surface water would be subject to volatilization to the air. No metals were detected above MCLs in the shallow ground water at Site SD13.

No volatile organic compounds were detected above MCLs in Unnamed Stream. The results of the laboratory analysis for inorganic constituents and field observations suggest that some metals in Unnamed Stream are preferentially adsorbed to sediments rather than dissolved in the surface water. This mode of transport (i.e., adsorbed to sediment) would result in slower migration of contaminants downstream than for the dissolved phase, and would be slower than the actual surface water flow rate. As evidenced by the lower dissolved and total concentrations of arsenic and lead in the downstream water samples, the metals apparently tend to adsorb to the stream bed sediments near their source. Both metals also have a tendency to bioaccumulate. The

presence of iron oxides, identified as coating on sediments in Unnamed Stream in the Phase II Stage 1 investigation, suggests that precipitation of metals is active in the stream sediments. The removal of metals such as lead and arsenic is enhanced by this process, as these metals commonly co-precipitate with or are adsorbed onto hydrous iron oxide compounds. Both lead and arsenic are, relatively speaking, nonvolatile and will tend to remain adsorbed to the sediments in Unnamed Stream. As long as there is a source of these metals, the sediments in the upper reaches of the stream will continue to act as a "sink" for them.

Site ST14--POL Tank Farm

The average Upper Zone ground-water flow velocity at the POL Tank Farm is approximately 0.3 feet per day, and Upper Zone ground-water flow is toward the southeast, or Farmers Branch. Therefore, the hydrocarbon contamination observed in the shallow ground water at Site ST14 is expected to migrate with the shallow ground water toward Farmers Branch. Volatilization and degradation of the hydrocarbon constituents from the ground water will tend to decrease the concentration of hydrocarbon constituents as they move downgradient, assuming there are no additional sources. Increased volatilization of the hydrocarbon constituents in Farmers Branch surface water would be expected due to increased surface area and turbulence in the stream.

Alternatively, hydrocarbon constituents from the POL Tank Farm could be intercepted by the existing french drain system and flow through the oil/water separator, ultimately entering Farmers Branch by Unnamed Stream. Volatilization of the constituents would be expected throughout this pathway.

The low dissolved lead concentrations in the shallow ground water, the nonvolatile nature of the metal, and the affinity of the metal to adsorb onto sediments suggest the overall distribution of lead at the site will not change significantly in the future.

Site BSS--Base Service Station

Migration of volatile organic compounds in the Upper Zone ground water will generally be toward the West Fork of the Trinity River, in the direction of ground-water flow. However, the permeable water-bearing sands observed at monitor well BSS-B are not present in the lithologic log for borehole BSS-D, located downgradient, or east, of Site BSS. Therefore, ground-water flow velocities are probably lower east of monitor well BSS-B, but contaminants could still potentially migrate toward the river in the lower permeability materials.

The principal fate of the volatile organic compounds detected in the ground water at well BSS-B would be volatilization to the atmosphere. This could occur as the ground water moves toward the West Fork of the Trinity River or upon entering the river. Insufficient downgradient well control precludes determination of the maximum contaminant extent. Metals contamination is not a concern at Site BSS.

1.2.5 Baseline Risk Assessment

The results of the baseline risk assessments for the four East Area IRP sites included in the 1990 study are summarized below. More complete descriptions of the risk assessment process are provided in the IRP Stage 2 RI/FS report (Radian, 1989) and in the East Area RI report (Radian, 1991).

Using both the 1988 and 1990 sampling results for soil, ground water, and surface water in the East Area, lists of indicator chemicals were developed for each site. The indicator chemicals were selected according to the method described in the U.S. EPA Health Evaluation Manual (EPA, 1986a) and are shown in Tables 1-1 through 1-4.

Although some of the indicator chemicals, particularly the metals and the semivolatile compounds, probably are not representative of site conditions (because of leaching from suspended sediment as a result of sample acidification and/or laboratory contamination, respectively), they were

TABLE 1-1. INDICATOR CHEMICALS FOR SITE LF01--LANDFILL 1

| Metals | Semivolatile Organic Compounds | Volatile Organic Compounds (VOCs) |
|-----------|---------------------------------|-----------------------------------|
| Antimony | Bis(2-ethylhexyl)- phthalate | Methylene chloride |
| Arsenic | | Toluene |
| Barium | | Trichloroethene |
| Beryllium | | Vinyl chloride |
| Cadmium | | |
| Chromium | | |
| Lead | | |
| Nickel | | |
| Selenium | | |
| Silver | | |

TABLE 1-2. INDICATOR CHEMICALS FOR SITE SD13--UNNAMED STREAM AND ABANDONED GASOLINE STATION

| Metals | Semivolatile Organic Compounds | Volatile Organic Compounds (VOCs) |
|-----------|--------------------------------|-----------------------------------|
| Antimony | None | Benzene |
| Arsenic | | Tetrachloroethene |
| Barium | | Toluene |
| Beryllium | | |
| Cadmium | | |
| Chromium | | |
| Lead | | |
| Nickel | | |
| Selenium | | |
| Silver | | |

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TABLE 1-3. INDICATOR CHEMICALS FOR SITE SD14--POL TANK FARM

| Metals | Semivolatile Organic Compounds | Volatile Organic Compounds (VOCs) |
|-----------|---------------------------------|-----------------------------------|
| Antimony | Bis(2-ethylhexyl)- phthalate | Benzene |
| Arsenic | | Methylene chloride |
| Barium | | Toluene |
| Beryllium | | Trichloroethene |
| Cadmium | | Vinyl chloride |
| Chromium | | |
| Lead | | |
| Nickel | | |
| Selenium | | |
| Silver | | |

TABLE 1-4. INDICATOR CHEMICALS FOR SITE BSS--BASE SERVICE STATION

| Metals | Semivolatile Organic Compounds | Volatile Organic Compounds (VOCs) |
|-----------|---------------------------------|-----------------------------------|
| Antimony | Bis(2-ethylhexyl)- phthalate | Benzene |
| Arsenic | | 1,2-Dichloroethane |
| Barium | | Tetrachloroethene |
| Beryllium | | Toluene |
| Cadmium | | Trichloroethene |
| Chromium | | |
| Lead | | |
| Nickel | | |
| Selenium | | |
| Silver | | |

included in the risk assessment process to ensure a conservative evaluation of possible health risks.

Possible mechanisms of contaminant release from the East Area sites include: 1) volatilization to the air, 2) leachate to ground water, 3) direct release to surface water, and 4) contaminated ground-water discharge to surface water. Figures 1-9 and 1-10 illustrate the potential pathways for human exposure for each of the East Area sites. Based on the potential pathways identified, potential human and wildlife receptors for exposure to contaminants migrating from the East Area sites were identified.

Potentially significant contaminant transport and fate mechanisms were identified and include: 1) air dispersion, 2) ground-water migration, 3) discharge to the surface, 4) transport in surface water, and 5) subsequent uptake by plants and animals.

Three types of exposures--inhalation, ingestion, and dermal contact--were quantified in the risk assessment. The maximum predicted annual average concentrations resulting from estimated East Area site VOC indicator chemical emissions are all lower than the conservative Texas Air Control Board (TACB) Effects Screening Levels (ESLs). For Sites LF01, SD13, ST14, and BSS respectively, the estimated emissions of the individual VOC indicator chemicals are lower by: 7 to 9, 3 to 6, 3 to 9, and 4 to 10 orders of magnitude. Potential ingestion exposures included consuming meat and dairy products or fish exposed to contaminants; however, neither of these potential pathways was found to represent a significant threat of human exposure. The likelihood of dermal exposure to contaminants in Farmers Branch and the West Fork of the Trinity River was so remote that it did not merit quantification.

The threat to human health posed by each site was evaluated in terms of noncarcinogenic and carcinogenic risks. The noncarcinogenic evaluation involved comparing maximum predicted annual average concentrations at various locations, both on site and off site, with inhalation Reference Doses (RFDs) for chronic (long-term) exposure. The results of this comparison indicate that the threat of noncarcinogenic health effects of inhalation

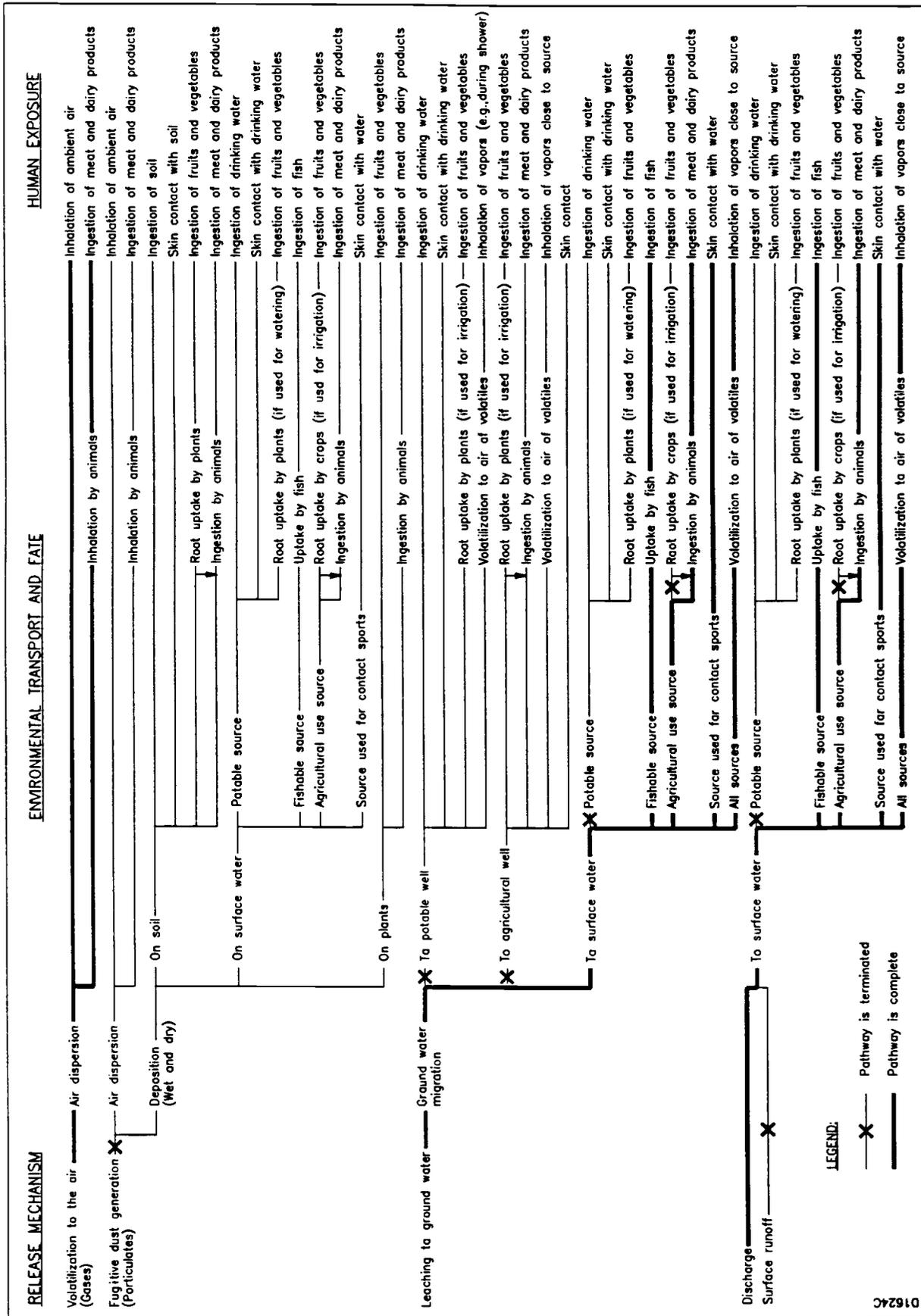


Figure 1-10. Potential Pathways to Human Exposure from Site SD13

exposure to contaminants from all East Area sites is not significant. For Sites LF01 and SD13, the expected maximum concentrations of all contaminants was at least six orders of magnitude below their RFDs. Similarly, for Sites ST14 and BSS, the concentrations were at least five orders of magnitude lower. For each site, incremental individual cancer risks were estimated for maximum exposed individuals at locations both on site and off site. The highest calculated risks were all dismissed as inconsequential, ranging from 5.7 in 100 million (Site ST14) to 9 in 10 billion (Site LF01). Ingestion and dermal risks were considered minimal and were not quantified.

Some risk exists for terrestrial wildlife that use Farmers Branch, Unnamed Stream, or the West Fork of the Trinity River as a source of drinking water and for aquatic organisms in these surface water bodies. However, all such risks were concluded to be minimal.

2.0 IDENTIFICATION AND SCREENING OF TECHNOLOGIES

Radian conducted a literature search to identify potential response actions, technologies, and process options available for remedying the contaminated environmental media at Carswell AFB. A variety of publications were reviewed both to identify and to screen remedial action technologies potentially appropriate to Carswell AFB IRP sites. General publications that are particularly appropriate to Carswell AFB are Evaluating Cost-Effectiveness of Remedial Actions at Uncontrolled Hazardous Waste Sites (Radian, 1983), Handbook: Remedial Action at Waste Disposal Sites (Revised) (EPA, 1986c), and Treatment Technology Briefs, Alternatives to Hazardous Waste Landfills (EPA, 1986d).

Section 2.1 defines the remedial action objectives (RAOs) of this FS. The screening of technologies is presented in Section 2.2. Technologies that remained after the screening are discussed in Section 2.3 as they relate to actual site conditions.

2.1 Remedial Action Objectives

The FS was performed to develop feasible remedial alternatives to mitigate environmental contamination associated with East Area IRP Sites LF01, SD13, ST14, and BSS. Volatile organic compounds, primarily benzene, associated with fuel spills and/or leaks are the main contaminants detected in the Upper Zone ground water, surface water, and soils in the East Area.

The remedial action objectives for this FS are:

- 1) To reduce or eliminate potential future impacts to human health and the environment;
- 2) To reduce or eliminate the potential for future contaminant migration in the ground water; and

- 3) To reduce or eliminate the potential for continuing mobilization of metals and/or organic contaminants in near-surface soil (Upper Zone deposits) or in residual wastes (as leachate).

To identify and evaluate remedial alternatives, contaminated environmental media were identified based on the IRP RI results (Radian, 1989; 1991). These media are wastes and contaminated soil, Upper Zone ground water, and surface water. Specific remedial action objectives identified for each of the media are presented in Table 2-1. Remedial action objectives were developed for each medium based upon the following standards or criteria:

- 70-year cancer risk;
- Maximum contaminant levels (MCLs) for organics (40 CFR 141.12 and 141.61) and inorganics (40 CFR 141.11 and 141.62) established by the national interim primary drinking water standards;
- Final MCLs for organics and inorganics (Federal Register, Vol. 56, No. 20, 30 January 1991); and
- Maximum BTEX (benzene, toluene, ethylbenzene, and xylene) and TPH (total petroleum hydrocarbon) levels for soil and ground water (TWC, 1990).

Table 2-1 does not list all contaminants that have regulatory criteria or standards. Instead, the table lists those contaminants that were identified as indicator chemicals in the baseline risk assessment for the Carswell AFB East Area sites. As discussed in the RI report (Radian, 1991), metals are included as indicator chemicals on the basis of total detected concentrations in water samples. However, the dissolved metals concentrations detected in the 1990 sampling event do not suggest a metals contamination problem.

TABLE 2-1. REMEDIAL ACTION OBJECTIVES FOR EAST AREA IRP SITES, CARSWELL AFB, TEXAS

| Environmental Medium | Remedial Action Objectives |
|------------------------------|---|
| WASTES AND CONTAMINATED SOIL | <p>FOR HUMAN HEALTH: Prevent soil or waste ingestion or direct contact that would contribute to an excess cancer risk equal to or greater than 10^{-6} (or a potential risk characterized as greater than negligible) from the following carcinogens: TCE, benzene, bis(2-ethylhexyl)phthalate, arsenic, cadmium, and methylene chloride.</p> <p>Reduce inhalation of carcinogens [TCE, 1,2-DCE, tetrachloroethylene, vinyl chloride, methylene chloride, benzene, chloroform, and bis(2-ethylhexyl)phthalate] at locations where these substances would contribute to excess inhalation cancer risk levels equal to or greater than 10^{-6} so that risk levels are lower than 10^{-6}.</p> <p>FOR ENVIRONMENTAL PROTECTION: 1) Prevent soil contaminant migration that would result in ground-water contamination in excess of the following concentrations for each specific contaminant:</p> |
| | <u>Inorganics</u> |
| | <p>Arsenic 0.05 mg/L Barium 1.0 (2.0) mg/L Cadmium 0.01 (0.005) mg/L Chromium 0.05 (0.1) mg/L Lead 0.05 mg/L Selenium 0.01 (0.05) mg/L Silver 0.05 mg/L</p> |
| | <u>Organics</u> |
| | <p>TCE 5 µg/L Vinyl Chloride 2 µg/L Benzene 5 µg/L cis-1,2-DCE (100) µg/L trans-1,2-DCE (70) µg/L Tetrachloroethene 8 µg/L Toluene 2,000 µg/L</p> |

(Continued)

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TABLE 2-1. (Continued)

| Environmental Medium | Remedial Action Objectives | | | | | | | | | | | | | | | | |
|-------------------------|--|-------------------|-----------------|-------------------|--------------------------|------------------|-------------------|-------------------|-----------------------|--------------------|-------------------------|----------------|---------------|--------------------|-----------------------------|------------------|-------------------|
| UPPER ZONE GROUND WATER | <p>FOR HUMAN HEALTH: Prevent ingestion of ground water that would contribute to an excess cancer risk equal to or greater than 10^{-6}.</p> <p>FOR ENVIRONMENTAL PROTECTION: Remove contaminants from the ground water to levels below the following concentrations:</p> <table border="0" style="width: 100%;"> <thead> <tr> <th style="text-align: left;"><u>Inorganics</u></th> <th style="text-align: left;"><u>Organics</u></th> </tr> </thead> <tbody> <tr> <td>Arsenic</td> <td>Vinyl Chloride</td> </tr> <tr> <td>Barium</td> <td>Benzene</td> </tr> <tr> <td>Cadmium</td> <td>cis-1,2-DCE</td> </tr> <tr> <td>Chromium</td> <td>trans-1,2-DCE</td> </tr> <tr> <td>Lead</td> <td>TCE</td> </tr> <tr> <td>Selenium</td> <td>Tetrachloroethene</td> </tr> <tr> <td>Silver</td> <td>Toluene</td> </tr> </tbody> </table> | <u>Inorganics</u> | <u>Organics</u> | Arsenic | Vinyl Chloride | Barium | Benzene | Cadmium | cis-1,2-DCE | Chromium | trans-1,2-DCE | Lead | TCE | Selenium | Tetrachloroethene | Silver | Toluene |
| <u>Inorganics</u> | <u>Organics</u> | | | | | | | | | | | | | | | | |
| Arsenic | Vinyl Chloride | | | | | | | | | | | | | | | | |
| Barium | Benzene | | | | | | | | | | | | | | | | |
| Cadmium | cis-1,2-DCE | | | | | | | | | | | | | | | | |
| Chromium | trans-1,2-DCE | | | | | | | | | | | | | | | | |
| Lead | TCE | | | | | | | | | | | | | | | | |
| Selenium | Tetrachloroethene | | | | | | | | | | | | | | | | |
| Silver | Toluene | | | | | | | | | | | | | | | | |
| SURFACE WATER | <p>FOR HUMAN HEALTH: Prevent surface water ingestion or skin contact that would contribute to an excess cancer risk equal to or greater than 10^{-6}. Prevent fish consumption that would contribute to an excess cancer risk equal to or greater than 10^{-6}.</p> <p>FOR ENVIRONMENTAL PROTECTION: Prevent future discharge of contaminated ground water to surface water. If treated ground-water effluent is discharged to Farmers Branch, it must meet the environmental protection criteria for ground water (above).</p> | | | | | | | | | | | | | | | | |

() - Final MCL as of 30 January 1991, not effective until 30 July 1992.

ADDITIONAL

2.2 Screening of Technologies

Available literature was reviewed to identify potential response actions, technologies, and process options applicable to each contaminated environmental medium in the East Area. These remedial technologies are discussed in Section 2.2.1 (wastes and contaminated soil), Section 2.2.2 (ground water), and Section 2.2.3 (surface water).

The applicability of each technology is dependent on the physical and chemical characteristics of the contaminants, the aquifer properties of the Upper Zone, and/or the physical and chemical characteristics of the soil matrix. The preliminary screening results are shown in Tables 2-2 through 2-4. Technologies which are not appropriate for conditions at the East Area sites, or which do not meet the criteria of demonstrated performance and effectiveness, constructability and implementability, and cost are indicated with an asterisk. These technologies are eliminated from further consideration because they are not applicable to the contaminants of concern, are unproven in actual field studies at this time, are not compatible with the characteristics of the East Area sites, or are too costly in comparison to other feasible technologies.

2.2.1 Wastes and Contaminated Soil

Very limited analytical data from the 1988 (Radian, 1989) effort indicated soil contamination from fuel spills and/or leaks at Sites ST14 and BSS. However, because no additional samples were collected during the 1990 effort, it is unclear what the areal extent and volumes of contaminated soil at these sites are, or if in fact the contamination currently persists in concentrations that exceed RAOs for soils. The baseline risk assessments for these and the other East Area sites, which included evaluation of the 1988 soils data, concluded that none of the sites pose a significant human health risk. Additional soil sampling and analysis will be required to determine if the areas of historically documented soil contamination require remediation.

Table 2-2 presents response actions, technologies, and process options potentially applicable to wastes and contaminated soil in the East Area, along with a brief description of each and comments on the screening. Potentially applicable response actions are no action, institutional actions, containment, removal, treatment, and disposal.

No-Action Response--The "no-action" response is included as a baseline consideration. No action is taken in this option, and all wastes and contaminated soil are left in place.

Institutional Actions--Institutional actions are already implemented in the East Area. Guards and security fences restrict access to the area. This action does not reduce the amount of contamination.

Containment--Containment actions involve both surface and subsurface control measures. Surface control consists of capping or diversion/collection of run-on. Capping waste bodies and/or contaminated soil source areas ("hot spots") reduces surface exposure and prevents surface water infiltration and potential leachate generation. Caps may consist of compacted clay, a synthetic liner, or both. Caps placed over the former waste disposal/release sites would be an effective technology. However, except for Site LF01 (Landfill 1), the potential contaminant source areas are not sufficiently well-defined at the surface to consider capping. Similarly, surface diversion/collection systems are not applicable. Site LF01 (Landfill 1) is already paved over, and furthermore, the 1990 analytical results for ground water do not indicate ongoing releases of organic or inorganic constituents at levels of concern (i.e., above MCLs). Therefore, surface containment technologies were eliminated from further consideration.

Subsurface control involves controlling or re-directing ground-water flow, as well as preventing migration of contaminants in the soil, so as to contain the contaminants within a specific area. Used alone, physical subsurface barriers do not promote any reduction in toxicity or existing concentrations of contaminants and may hinder biodegradation and volatilization of organic contaminants. If soil contamination is eliminated

TABLE 2-2. IDENTIFICATION AND SCREENING OF TECHNOLOGIES FOR WASTE MATERIAL AND CONTAMINATED SOIL

| Response Action | Remedial Technology | Process Options | Description | Screening Comments |
|-----------------------|---------------------|-----------------------|--|--|
| No Action | None | Not Applicable | No action. | Consideration required as base case. |
| Institutional Actions | Access Restriction | Fencing | Fence with locked gates placed around contaminated area. | Potentially applicable when used with other options. |
| | | Deed Restriction* | Deed to property restricts use of contaminated area. | Not applicable so long as base is federally owned/controlled. |
| Containment | Surface Controls | Capping* | Compacted clay, synthetic membrane, or both placed over contaminated area to prevent surface water infiltration or to aid in other remedial actions (e.g., soil vapor extraction). | Potentially applicable to minimize waste/leachate generation from well defined sources. Minimize exposure to waste/leachate. |
| | | Grading* | Land surface reshaped to manage run-off, to prevent ponding, and to control erosion. | Potentially applicable when used with other options. |
| | | Revegetation* | Surface of graded and capped area stabilized with shallow-rooted vegetation to reduce erosion. | May be used in conjunction with grading and capping. |
| | | Diversion/Collection* | Contaminated area surrounded with dikes, ditches, or other to prevent run-on. | Potentially applicable when used with other options. |
| | Immobilization* | Microencapsulation* | Waste physically sealed within an organic binder or resin. | In research stage. |
| | Subsurface Barriers | Liners* | Synthetic or clay liner placed beneath contaminated area. | Not applicable because waste is already in place. |
| | | Sheet Piles* | Interconnected steel sheets forced into the ground surrounding contaminated area. | Unreliable because the interlocks connecting the sheets are not sealed. |
| | | Grouting* | Grout pressure-injected in a regular pattern of drilled holes. | Does not remove or cause destruction of contaminants and may hinder natural processes. Satisfies no-migration objective, but not good for long-term remedy unless used in conjunction with other technology. |

*Remedial technologies or process options eliminated from further consideration (see Section 2.3).

(Continued)

TABLE 2-2. (Continued)

| Response Action | Remedial Technology | Process Options | Description | Screening Comments |
|---------------------|--------------------------------|---|---|--|
| Containment (Cont.) | Subsurface Barriers (Cont.) | Slurry Walls* | Trench filled with bentonite mixture or other material surrounding contaminated area. | Does not remove or cause destruction of contaminants and may hinder natural processes. Satisfies no-migration objective, but not good for long-term remedy unless used in conjunction with other technology. |
| Removal | Excavation | Hydraulic Dredging* Mechanical Excavation† | Slurried materials removed by pumping. Contaminated materials removed with conventional construction equipment such as backhoes, drag lines, front-end loaders, shovels, etc. | Not applicable. Potentially applicable. However, generally not feasible for contaminated soil under structures, roads, or near subsurface pipelines (or utilities). |
| Treatment | In Situ | Soil Flushing* | Extractant solution injected or sprayed on contaminated area to mobilize sorbed contaminants, then contaminants pumped to surface for treatment. | Potentially applicable. More expensive than other equally (or more) effective technologies in this category (e.g., soil vapor extraction). |
| | | Bio-treatment | Soil flushed with oxygenated water and nutrients to stimulate soil bacteria. | Potentially applicable. |
| | | Soil Vapor Extraction | Vapors extracted from soil using vacuum wells; vapors are treated with activated carbon or by incineration-catalytic conversion. | Potentially applicable. |
| | | Solidification/ Stabilization | Soils mixed in a closed system to depth of 30 feet with either dry or fluid treatment chemicals to produce a solidified end product. | Potentially applicable. More expensive than other equally (or more) effective technologies in this category (e.g., soil vapor extraction). |
| | | Vitrification* | Large electrodes inserted into silicate-type soils and connected to graphite on the soil surface with high current electricity passing through both. Heat causes melting downward through soil. Some organics volatilize, others along with inorganics are trapped in the melt as it cools and becomes a form of obsidian or very strong glass. | Applicable to sites with radioactive or very highly toxic waste contamination. Very expensive, hard to implement around existing structures and within project's time frame. |

*Remedial technologies or process options eliminated from further consideration (see Section 2.3)

†This remedial technology requires excavation of the contaminated soil. Excavation is generally not feasible if soil contamination exists under structures, roads, or near subsurface pipelines (or utilities).

(Continued)

TABLE 2-2. (Continued)

| Response Action | Remedial Technology | Process Options | Description | Screening Comments |
|-------------------|----------------------|--------------------------------|---|---|
| Treatment (Cont.) | Physical Treatment | Soil Shredding*† | Shredder with high speed cleated belts azrates, mixes, and pulverizes soil through a violent churning action. Essentially, air strips VOCs from soil. | Potentially applicable. More expensive than other equally (or more) effective technologies (e.g., soil piles). |
| | Biological Treatment | Landfarming*† | Waste applied to soil surface and tilled to degrade or immobilize contaminants. Chemicals, nutrients, and absorbents may aid in process. | Potentially applicable. More expensive than other equally (or more) effective technologies (e.g., soil piles). |
| | | Soil Pilest | Soil excavated and placed in a pile. Drain pipes are placed across pile and volatilization and biodegradation of the petroleum products are enhanced. | Potentially applicable. |
| | Chemical Treatment | Soil Washing*† | Contaminants extracted from excavated soil by mixing soil with extractant. The contaminated solution is then treated. | Potentially applicable. Very expensive compared to other equally (or more) effective technologies (e.g., soil piles). |
| | | Solidification/Stabilization*† | Addition to excavated soil of large amounts of a siliceous material combined with a settling agent such as lime resulting in a dewatered, stabilized, solidified waste product. | Potentially applicable. More expensive than other equally (or more) effective technologies (e.g., soil piles). |
| | | Asphalt Incorporation*† | Soil extracted and added to asphalt as an asphalt ingredient. | Potentially applicable but still in research stage. |
| | Thermal Destruction | Electric Reactor*† | Electrically heated fluid wall reactor pyrolyzes organics and inorganics from solid, liquid, or gas. | Potentially applicable. Very expensive compared to other equally effective technologies (e.g., soil piles). |
| | | Rotary Kiln Incinerator*† | Waste thermally destroyed by mixing with oxygen and fuel in a rotating vessel. | Potentially applicable. Very expensive compared to other equally effective technologies (e.g., soil piles). |

*Remedial technologies or process options eliminated from further consideration (see Section 2.3)

†This remedial technology requires excavation of the contaminated soil. Excavation is generally not feasible if soil contamination exists under structures, roads, or near subsurface pipelines (or utilities).

(Continued)

TABLE 2-2. (Continued)

| Response Action | Remedial Technology | Process Options | Description | Screening Comments |
|-------------------|-----------------------------|---------------------------------|---|---|
| Treatment (Cont.) | Thermal Destruction (Cont.) | Infrared Incineration Systems** | Solids, sludges, and contaminated soils destroyed by infrared energy provided by silicon carbide resistance heating elements. | Potentially applicable. Very expensive compared to other equally effective technologies (e.g., soil piles). |
| | | Fluidized Bed Incineration** | Wastes incinerated in a turbulent bed of inert granular material to improve transfer of heat to waste streams. | Potentially applicable. Very expensive process compared to other equally effective technologies (e.g., soil piles). |
| Disposal | Disposal | Landfill** | Land disposal of contaminated soils or waste in a RCRA-permitted facility. | Not applicable without treatment. Land ban restrictions. |
| | | On-Site Disposal† | Various potential applications for use as clean fill. | Potentially applicable. |

**Remedial technologies or process options eliminated from further consideration (see Section 2.3).

†This remedial technology requires excavation of the contaminated soil. Excavation is generally not feasible if soil contamination exists under structures, roads, or near subsurface pipelines (or utilities).

by treatment, there is no need for subsurface controls. Therefore, all four subsurface containment options--liners, sheet piles, grouting, and slurry walls--were eliminated from further evaluation.

Removal--Removal of contaminated soil/waste would be accomplished by excavation using conventional techniques. At a site such as Site ST14 (POL Tank Farm), where there are numerous surface and subsurface structures, excavation may not be feasible unless the areas of soil contamination are very localized. Excavation is required in conjunction with implementation of some other remedial options (e.g., ground-water interceptor trenches), and could be applicable to local areas of contamination suspected to be present at Site BSS (Base Service Station). Any contaminated soils that are removed could require treatment prior to disposal.

Treatment--Soil leaching, solidification/stabilization, and vitrification were eliminated from consideration as in-situ treatment options because they are too difficult to implement or are more expensive than other, equally effective (or more-effective) treatments, such as biological treatment and soil vapor extraction. In-situ biological degradation and soil vapor extraction are cost-effective technologies for remediation of organic contamination in soils and were selected for further evaluation.

Treatment technologies that require removal of contaminated soil/wastes are generally more costly and potentially more difficult to implement than in-situ technologies. Soil washing (chemical extraction), asphalt incorporation, solidification/stabilization, landfarming, and soil shredding were eliminated from further consideration because they are more expensive than soil piles, an equally effective (or more-effective) treatment technology. The soil piles method uses biological degradation and volatilization to treat organic and volatile organic contamination in soils. Soil piles were chosen for further evaluation.

Disposal--Off-site disposal of untreated soil/waste in a landfill potentially presents regulatory problems that may be difficult (or impossible) to resolve. At this time, landfills in the Fort Worth area are not accepting

untreated petroleum-contaminated soil. Once treated, off-site disposal of excavated soil/waste is feasible, but was eliminated because on-site disposal of treated material would be more easily implemented and cost-effective.

2.2.2 Ground Water

Table 2-3 presents response actions, technologies, and process options for ground water. The response actions applicable to control contaminants in ground water are no action, institutional actions, containment, extraction/recovery, treatment, and discharge.

No-Action Response--The "no-action" response is included as a baseline consideration. No action (other than long-term monitoring) is taken in this option, and the ground water is left in place, untreated and uncontained.

Institutional Actions--Two institutional actions were considered: 1) restriction of access to Upper Zone ground water and 2) using monitor wells to monitor Upper Zone ground-water quality. Since proven technologies are available for treating the ground-water contaminants detected in Upper Zone ground water on the East Area of the base, restricting aquifer use is not appropriate and was eliminated. Ground-water monitoring, in conjunction with the no-action alternative, is applicable at sites where current concentrations of indicator chemicals are below the RAOs (i.e., Sites SD13 and LF01). Ground-water monitoring is also an applicable technology when used to evaluate the effectiveness of additional remedial technologies.

Ground-Water Containment--The discussion of containment technologies for wastes and contaminated soil also applies to ground water. Additional hydraulic barriers (pumping or injection wells, or passive collection using subsurface drains/interceptor trenches) could be used both to control contaminated ground-water migration and to extract ground-water (see below).

TABLE 2-3. IDENTIFICATION AND SCREENING OF TECHNOLOGIES FOR GROUND WATER

| Response Action | Remedial Technology | Process Options | Description | Screening Comments |
|-----------------------|---------------------|--------------------|--|---|
| No Action | None | Not Applicable | No action. | Consideration required for base case. Also applicable when baseline risk is negligible. |
| Institutional Actions | Access Restriction | Deed Restriction* | Deed to property restricts use of wells in the area of influence. | Considered only if remediation is not possible. Very hard to enforce. Not applicable. |
| | Monitoring | Ground-Water Wells | Contaminated area monitored by system of upgradient and downgradient wells. | May be used alone or in conjunction with remedial actions to evaluate the effectiveness of remedial actions or the extent of contamination/ground-water movement. |
| Containment | Capping | Clay and Soil* | Compacted clay covered with soil over source areas of ground-water contamination. | Potentially applicable to prevent infiltration. However, does not remove or cause destruction of contaminants and may hinder natural processes. |
| | | Asphalt* | Asphalt sprayed over source areas of ground-water contamination. | Potentially applicable to prevent infiltration. However, does not remove or cause destruction of contaminants and may hinder natural processes. |
| | | Concrete* | Concrete slab installed over source areas of ground-water contamination. | Potentially applicable to prevent infiltration. However, does not remove or cause destruction of contaminants and may hinder natural processes. |
| | | Multi-Media Cap* | Clay and synthetic membrane covered by soil over source areas of ground-water contamination. | Potentially applicable to prevent infiltration. However, does not remove or cause destruction of contaminants and may hinder natural processes. |

*Remedial technologies or process options eliminated from further consideration (see Section 2.3).

TABLE 2-3. (Continued)

| Response Action | Remedial Technology | Process Options | Description | Screening Comments |
|----------------------------|---------------------------------|---|---|--|
| Containment (Continued) | Subsurface Barriers Vertical | Slurry Wall* | Trench around areas of contamination is filled with a soil (or cement) and bentonite slurry. | Does not remove or cause destruction of contaminants and may hinder natural processes. Satisfies no-migration objective, but not good for long-term remedy unless used in conjunction with other technology. |
| | | Grout Curtain* | Pressure injection of grout in a regular pattern of drilled holes below contaminated area. | Does not remove or cause destruction of contaminants and may hinder natural processes. Satisfies no-migration objective, but not good for long-term remedy unless used in conjunction with other technology. |
| | | Vibrating Beam* | Vibrating force to advance beams into the ground with the injection of slurry as beam is withdrawn. | Does not remove or cause destruction of contaminants and may hinder natural processes. Satisfies no-migration objective, but not good for long-term remedy unless used in conjunction with other technology. |
| | | Sheet Piles* | Interconnected steel sheets forced into the ground surrounding contaminated areas. | Unreliable because the interlocks connecting the sheets are not sealed. |
| | | Hydraulic Barriers | Series of extraction wells (or trenches) and injection wells to create a hydraulic barrier to off-site migration of contaminants. | Potentially applicable. |
| | | Liners* | Synthetic or clay liner placed beneath wastes to contain leachate. | Not feasible. Waste already in place. |
| Extraction | Collection Systems | Ground-Water Extraction Wells (Hydraulic Barrier) | Series of pumping wells to extract contaminated ground water. | Potentially applicable, used in conjunction with ground-water treatment processes. |
| | | Interceptor Trench | Buried conduit conveys and collects leachate by gravity flow. | Potentially applicable, used in conjunction with ground-water treatment process. |

*Remedial technologies or process options eliminated from further consideration (see Section 2.3).

(Continued)

TABLE 2-3. (Continued)

| Response Action | Remedial Technology | Process Options | Description | Screening Comments |
|-----------------|---------------------|------------------------------|---|--|
| Treatment | In-Situ Treatment | Aerobic Biological | Bacteria and nutrients added to contaminated ground water to enhance degradation process. | Potentially applicable. Aquifer matrix and ground water probably have enough carbon source to aid in sustaining growth. |
| | | Anaerobic Biological* | A reducing agent and nutrients added to contaminated ground water in a no-oxygen environment to enhance the degradation of low-molecular-weight halogenated organics. | Not applicable. Difficult to create anaerobic conditions in the Upper Zone Aquifer. |
| | | Adsorption or Permeable Bed* | Excavated trenches placed perpendicular to ground-water flow and filled with an appropriate material (e.g., activated carbon) to treat the plume as it flows through. | Potentially applicable but very expensive due to treatment or excavation of spent materials. |
| | | Chemical Reaction* | System of injection wells to inject oxidizer such as hydrogen peroxide to degrade contaminants. | Potentially applicable but biological treatment may be more effective. Potential for remnant oxidizer to be left in subsurface. |
| | Physical Treatment | Oil/Water Separation | Bulk separation of immiscible materials. | Potentially applicable as a pretreatment step, immiscible fluids in ground water. |
| | | Granular Media Filtration* | Pretreatment process to remove solids or colloidal material from liquids by passing ground water through a bed of granular material (sand). | Does not reduce toxicity, and Upper Zone ground water does not have high TDS/TSS. Possibly could be used as a pretreatment step. |
| | | Air Stripping | Mass transfer where volatile contaminants in ground water are transferred to air. | Potentially applicable. |
| | | Steam Stripping* | Continuous fractional distillation of volatile compounds from ground water in a packed or tray tower using clean steam. | Potentially applicable. More expensive than other equally effective treatment (e.g., air stripping). |
| | | Carbon Adsorption | Contaminated ground water flows through a series of packed bed reactors containing activated carbon or used as vapor treatment with air stripping. | Potentially applicable but very expensive as a primary treatment due to operating and maintenance (O&M) costs. Air stripping is less expensive and as effective. |

*Remedial technologies or process options eliminated from further consideration (see Section 2.3).

TABLE 2-3. (Continued)

| Response Action | Remedial Technology | Process Options | Description | Screening Comments | | |
|-----------------------|--|---------------------|---|--|---|---|
| Treatment (Continued) | Biological Treatment | Activated Sludge* | Contaminated water aerated in basin where a suspended active microbial population degrades organics. The water is then clarified. | Ground water may not have sufficient carbon source to sustain biological growth. | | |
| | | Fixed Film* | Contact of contaminated water with microbes attached to some medium for waste degradation (e.g., rotating biological contactor). | Ground water may not have sufficient carbon source to sustain biological growth. | | |
| | | Anaerobic Lagoon* | Large, deep basin where high organic loadings promote thermophilic anaerobic digestion of organics. | Not applicable for organics in East Area. | | |
| | | Chemical Treatment | Ion Exchange/Resin Adsorption* | Toxic metal ions removed from water by exchanging with an ion attached to the solid resin material. | Little evidence of metals contamination in East Area. | |
| | | | Oxidation/Reduction* | Contaminated water reacted with either an oxidizer or reducer to lower or raise the oxidation state. | Not typically used for VOC-contaminated waters. | |
| | | Thermal Destruction | Electric Reactors* | Reverse Osmosis* | Solvent forced by high pressure through a membrane that is permeable to the solvent molecules, but not the solute. | Little evidence of metals contamination in East Area. Organics may dissolve membrane. |
| | | | | Precipitation/Flocculation/Sedimentation* | Chemicals added to contaminated water to precipitate metals from the water, agglomerate the precipitate, and allow the precipitate to settle. | Little evidence of metals contamination in East Area. |
| | | | | Rotary Kiln* | Waste combusted in a horizontally rotating cylinder designed for uniform heat transfer. | More applicable for concentrated waste streams; very expensive. |
| | | | | Fluidized Bed* | Waste injected into hot agitated bed of sand where combustion occurs. | More applicable for concentrated waste streams; very expensive. |
| | | Discharge | On Site/Off Site | Fume Incineration-Catalytic Conversion | Electrically heated fluid wall reactor that pyrolyzes organics and inorganics. | More applicable for concentrated waste streams; very expensive. |
| Local Stream | Vapor wastes thermally treated and catalyzed. Generally used in conjunction with air stripping. Extracted water discharged to a local stream. | | | May be used in secondary treatment. Potentially applicable but requires prior treatment. | | |

*Remedial technologies or process options eliminated from further consideration (see Section 2.3).

TABLE 2-3. (Continued)

| Response Action | Remedial Technology | Process Options | Description | Screening Comments |
|-----------------------|---------------------------------|----------------------|---|--|
| Discharge (Continued) | On Site/Off Site (Continued) | Aquifer Recharge | Extracted water reinjected or allowed to percolate into aquifer using injection wells or sprinkling system. | Potentially applicable, but requires prior treatment. |
| | | Deep Well Injection* | Extracted water discharged to deep well injection system. | Not applicable due to regulatory problems. |
| | | POTW | Extracted water discharged to local POTW for treatment. | May require treatment before discharging to POTW, otherwise may not be accepted. |

*Remedial technologies or process options eliminated from further consideration (see Section 2.3).

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Ground-Water Extraction--Two ground-water extraction technologies were considered: extraction well fields and interceptor trenches. Interceptor trenches are potentially applicable because of the shallow depth of the Upper Zone ground water throughout much of the East Area. Ground-water extraction wells are also a feasible technology, especially in those areas where greater ground-water depth makes subsurface drain systems less cost-effective and/or difficult to implement. In addition, properly designed and constructed ground-water extraction technologies would also create a hydraulic barrier that would restrict the further migration of contaminated ground water.

Ground-Water Treatment--Five categories of treatment technologies were considered for ground water: in-situ, physical, biological, chemical, and thermal.

Three in-situ treatments were eliminated from further consideration: anaerobic biological treatment, adsorption bed treatment, and chemical reaction. These treatments were either inappropriate or too difficult to implement (anaerobic biological treatment and chemical reaction); or too costly (adsorption bed treatment) when compared to other equally effective technologies. Aerobic biological treatment, which uses bacteria and nutrients to enhance biodegradation, is potentially applicable for remediation of ground water contaminated with hydrocarbon constituents.

Several physical treatment options were considered for treating contaminated ground water extracted from the East Area. The two pretreatment processes were granular media filtration and oil/water separation. The three treatment processes were air stripping, steam stripping, and carbon adsorption.

Oil/water separation is the only pretreatment option considered potentially applicable (or necessary) for remediation of ground-water contamination in the East Area. Free-phase hydrocarbon was observed in one well at Site ST14 (POL Tank Farm) during the 1990 sampling event. While the data suggest a limited occurrence of free-phase contaminant, oil/water

separation may be required before ground-water treatment. Suspended solids are not expected to be a problem, so granular media filtration was eliminated from further evaluation.

Air and steam stripping are both considered potential primary treatment options for removing volatile organic compounds (the main contaminants) from the ground water. Air stripping is the preferred choice of the two if no secondary treatment of off-gas is required. A cost comparison of air and steam stripping units showed that the capital costs of the two technologies are comparable. In the absence of secondary treatment requirements for the air stripper, the operating costs of steam stripping are greater than those of air stripping. However, if secondary treatment, such as carbon, is required, the operation and maintenance costs of air stripping approach those of steam stripping. Steam stripping was eliminated from further consideration for the following reasons:

- Possibly higher operating and maintenance costs than air stripping for the same level of treatment; and
- Use of a more complicated process, requiring a higher level of expertise for operation than air stripping.

Carbon adsorption is also a viable technology for primary and secondary treatment. This technology is used primarily to remove organic compounds from waste streams. Activated carbon can also remove other contaminants that are non-volatile. However, the operating and maintenance (O&M) costs of carbon adsorption units are much greater than those of air stripping because of the significant cost in handling, transporting, and disposing of spent carbon, which is a hazardous waste. Because of the cost difference, and because both methods are expected to achieve similar removal efficiencies for the expected contaminant loadings, carbon adsorption was eliminated from further consideration as a primary treatment option. However, carbon adsorption will be considered for a secondary treatment option (e.g., as a vapor phase treatment for air stripping).

Biological Treatment--Three biological treatment technologies were screened: activated sludge, fixed film, and anaerobic lagoon.

Two of these processes (activated sludge and fixed film) are performed under aerobic conditions. In general, the hydrocarbon constituents found in the East Area can be effectively degraded by these processes. However, the extracted contaminated ground water may not have a sufficient carbon source to sustain growth of the microorganisms. Degrading the ground-water contaminants in anaerobic lagoons is inefficient, requiring long retention times. Therefore, biological treatment processes, other than in-situ bio-treatment (see page 2-18 for description) were eliminated from further consideration.

Chemical Treatment--Four chemical treatment technologies were evaluated: ion exchange/resin adsorption, oxidation/reduction, reverse osmosis, and precipitation/flocculation/sedimentation. All are effective in treating ground water contaminated with metals; however, all but oxidation/reduction are ineffective for treating organic compounds. Since there is little evidence to suggest a metals contamination problem at the East Area sites, the chemical treatment options were eliminated from further consideration.

Certain oxidation/reduction processes have been developed to treat organics (e.g., ultraviolet radiation/peroxidation). The oxidation reduction processes can be quite effective in destroying organic contaminants in ground water, but color, turbidity, and naturally occurring organics (such as humic and fulvic acids) can reduce the effectiveness of the process. Oxidation/reduction processes are typically used when less expensive or rigorous processes are not effective. Since air stripping is equally effective for the contaminants present in the East Area and usually less costly, oxidation/reduction processes were eliminated from further consideration.

Thermal Destruction--Thermal destruction processes such as 1) electric reactors, 2) rotary kiln, and 3) fluidized bed incineration could be used to destroy contaminants in ground water. However, these processes are not usually feasible for liquid streams unless high concentrations of organic

compounds reduce or eliminate the need for supplemental fuel. Fume incineration (catalytic conversion) could be used as a secondary treatment with other remedial techniques such as air stripping. Considering the typical ground-water contaminant concentrations in the Upper Zone ground water, fume incineration was the only thermal destruction technology retained for further consideration.

Discharge of Ground Water--Options for discharging untreated ground water to a local stream, by aquifer recharge, or by deep well injection were evaluated and rejected because they do not meet regulatory requirements. Discharge of untreated effluent to the local publicly owned treatment works (POTW) is unlikely to be allowed under the local ordinances and was also eliminated. However, once the water is treated, all of these become feasible options that will be considered in developing remedial alternatives.

2.2.3 Surface Water

Table 2-4 presents response actions, technologies, and process options that apply to surface water. All of the treatment technologies for surface water were also presented as ground-water treatment technologies and were discussed in Section 2.2.2. The only surface water body within the East Area that was sampled during the IRP is Unnamed Stream. As previously described, the source of Unnamed Stream is ground water discharging from an oil-water separator/french drain system that collects ground water from Site ST14 (POL Tank Farm) upgradient of the stream. Although benzene was detected above the MCL at a maximum concentration of 120 $\mu\text{g}/\text{L}$ in a first-round sample collected in 1988, no benzene was detected in any of the second-round surface water samples (Radian, 1989). Furthermore, no volatile organic compounds or verified concentrations of dissolved metals exceeded MCLs in any samples collected from Unnamed Stream in 1990. Therefore, the only applicable technology listed in Table 2-4 is continued monitoring of surface water (or ground water at points of discharge to surface water).

TABLE 2-4. (Continued)

| Response Action | Remedial Technology | Process Options | Description | Screening Comments |
|-------------------|---------------------------|---|--|---|
| Treatment (Cont.) | In Situ Treatment (Cont.) | Adsorption* | Excavated trenches placed perpendicular to surface water flow and filled with an appropriate material to treat the plume as it flows through. | Not applicable. |
| | Physical Treatment | Air Stripping* | Mass transfer where volatile contaminants in water are transferred to air. | Not needed, little evidence of surface water contamination. |
| | | Steam Stripping* | Continuous fractional distillation of volatile compounds from surface water in a packed or tray tower using clean steam. | Not needed, little evidence of surface water contamination. |
| | | Carbon Adsorption* | Contaminated surface water flows through a series of packed bed reactors containing activated carbon. | Not needed, little evidence of surface water contamination. |
| | Biological Treatment | Activated Sludge* | Contaminated water aerated with air in basin where a suspended active microbial population degrades organics. The water is then clarified. | Not needed, little evidence of surface water contamination. |
| | | Fixed Film* | Contact of contaminated water with microbes attached to some medium for waste degradation (e.g., rotating biological contactor). | Not needed, little evidence of surface water contamination. |
| | | Anaerobic Lagoon* | Large, deep basin where high organic loadings and an impervious surface grease layer promote thermophilic anaerobic digestion of organics. | Not needed, little evidence of surface water contamination. |
| | Chemical Treatment | Ion Exchange/Resin Adsorption* | Toxic metal ions removed from water by exchanging with an ion attached to the solid resin material. | Not applicable. Little evidence of metals contamination. |
| | | Oxidation/Reduction* | Contaminated water reacted with either an oxidizer or reducer to lower or raise the oxidation state. | Not needed, little evidence of surface water contamination. |
| | | Reverse Osmosis* | Solvent forced by high pressure through a membrane that is permeable to the solvent molecules, but not the solute. | Not needed, little evidence of surface water contamination. |
| | | Precipitation/Flocculation/Sedimentation* | Chemicals added to contaminated water to precipitate metals from the water, agglomerate the precipitate, and allow the precipitates to settle. | Not needed, little evidence of metals contamination. |
| | Thermal Destruction* | Electric Reactors* | Electrically heated fluid wall reactor that pyrolyzes organics and inorganics. | Not needed, little evidence of organic contamination. |

*Remedial technologies or process options eliminated from further consideration.

(Continued)

TABLE 2-4

TABLE 2-4. (Continued)

| Response Action | Remedial Technology | Process Options | Description | Screening Comments |
|-------------------|----------------------|-----------------|---|---|
| Treatment (Cont.) | Thermal Destruction* | Rotary Kiln* | Waste combusted in a horizontally rotating cylinder designed for uniform heat transfer. | Not needed, little evidence of organic contamination. |
| | | Fluidized Bed* | Waste injected into hot agitated bed of sand where combustion occurs. | Not needed, little evidence of organic contamination. |

*Remedial technologies or process options eliminated from further consideration.

TABLE 2-5. SUMMARY OF REMEDIAL ACTION OPTIONS FOR THE EAST AREA
IRP SITES

| | Site | | | |
|---|------|------|------|-----|
| | LF01 | SD13 | ST14 | BSS |
| No Action | ■ | ■ | ■ | ■ |
| <u>Institutional</u> | | | | |
| Long-Term Monitoring | ■ | ■ | ■ | ■ |
| <u>Containment</u> | | | | |
| Hydraulic Barrier (see ground-water extraction) | | | ■ | ■ |
| <u>Ground-Water Extraction</u> | | | | |
| Extraction Well Fields | | | ■ | ■ |
| Interceptor Trenches | | | ■ | ■ |
| <u>Ground-Water Pretreatment</u> | | | | |
| Oil/Water Separator | | | ■ | |
| <u>Primary Ground-Water Treatment</u> | | | | |
| Air Stripping | | | ■ | ■ |
| In-Situ Biological Treatment | | | ■ | ■ |
| <u>Treated Ground-Water Discharge</u> | | | | |
| Discharge to POTW | | | ■ | ■ |
| Discharge to Stream | | | ■ | ■ |
| Aquifer Recharge | | | ■ | ■ |
| <u>Soil Treatment</u> | | | | |
| Soil Vapor Extraction | | | ■ | ■ |
| In-Situ Biological Treatment | | | ■ | ■ |
| Excavation/Soil Piles | | ■ | ■ | ■ |
| <u>Secondary Treatment</u> | | | | |
| Carbon Adsorption | | | ■ | ■ |
| Fume Incineration | | | ■ | ■ |
| <u>Treated Soil Disposal</u> | | | | |
| On Site | | ■ | | ■ |

2.3.3 Interceptor Trenches

Interceptor trenches constitute a passive ground-water extraction technology that can also act as a hydraulic barrier to control ground-water flow (and contaminant migration). Construction of interceptor trenches requires excavation (of potentially contaminated material), installation of piping and a pumping system, and backfilling. This technology is most cost-effective in settings where ground water occurs at shallow depth, and where the saturated zone is relatively thin and underlain by a low permeability confining zone. Interceptor trenches can be used in geologic materials where relatively low permeability limits the effectiveness of pumping wells.

2.3.4 Air Stripping Treatment System

The air stripping process is designed to remove volatile organic contaminants. Once extracted from the aquifer, ground water is pumped to storage tanks at a treatment pad through a pipeline. In one possible design, the ground water is then contacted with countercurrent or cross-current air in a packed tower. Other types of air stripping equipment use stacked trays or spray aeration chambers. Figure 2-1 is a schematic of the overall process. In addition to a stripping tower or chamber and water storage tanks, the system includes liquid-circulating pumps and an air blower.

Air-stripping equipment consists of simple gas-liquid contacting devices consisting of a shell containing packing material or trays, and a liquid-distributing device designed to effectively irrigate the packing (trays). The contaminated ground water enters the top of the column and flows by gravity counter-current to the air. As the water passes down through the column, it becomes progressively less contaminated. The volatile organic compound (VOC)-laden air is discharged at the top of the column. The dissolved organic compounds are stripped from the ground water because these compounds tend to volatilize into the gas phase until their vapor and liquid concentrations reach thermodynamic equilibrium. Because multiple VOCs, each with a somewhat different equilibrium constant, are present in the Upper Zone

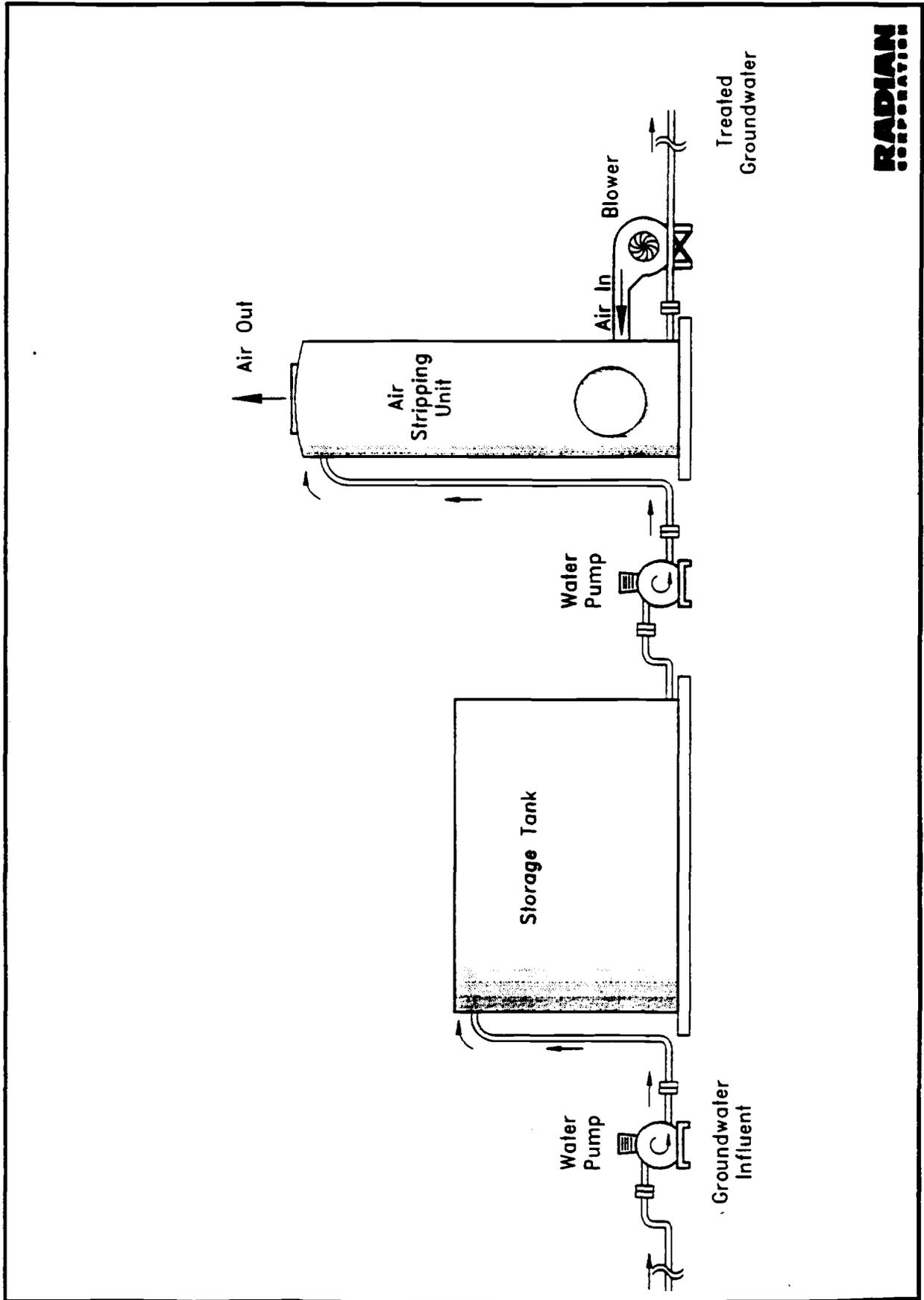


Figure 2-1. Schematic of Air Stripping Treatment System

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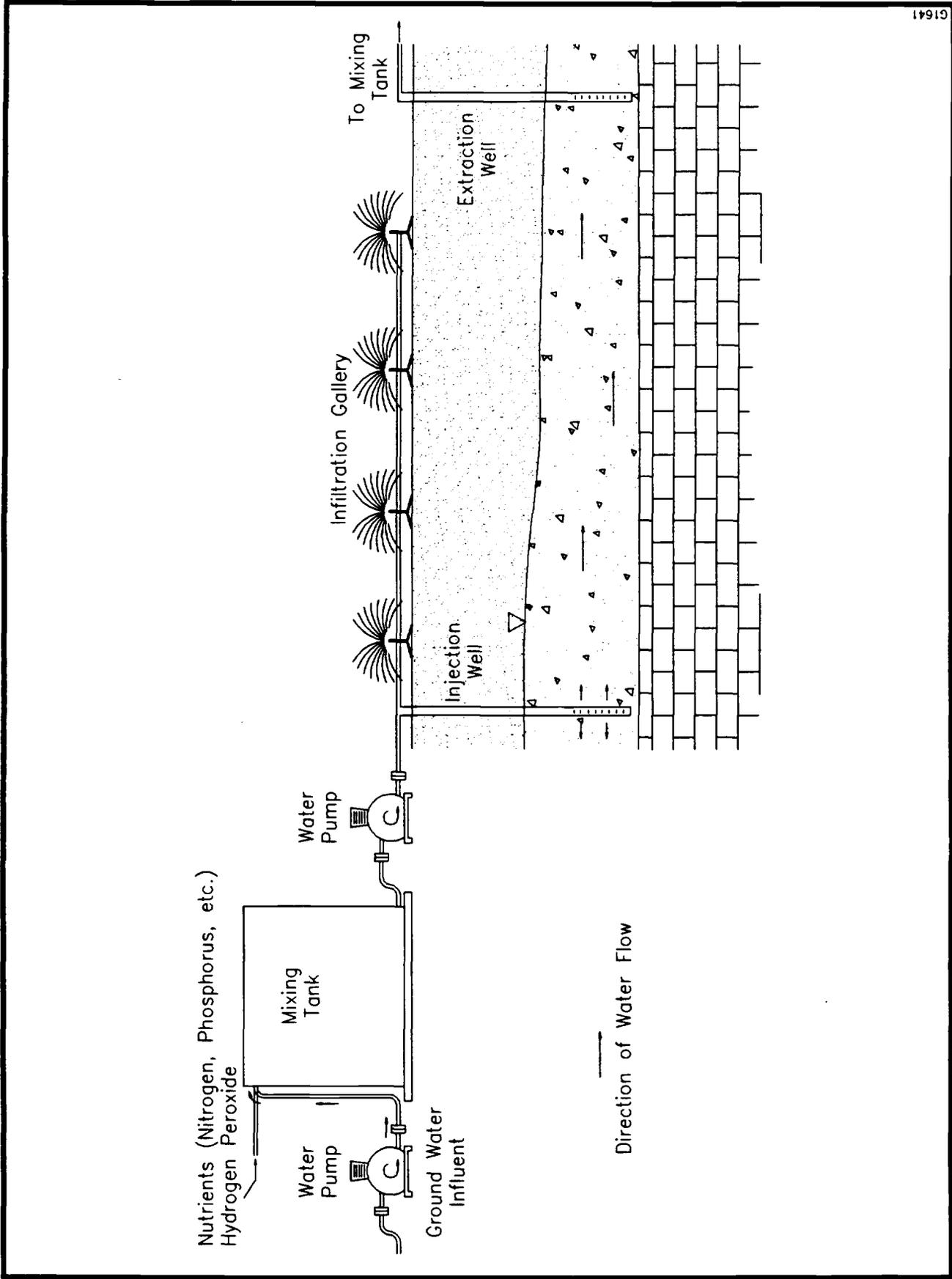
ground water beneath the East Area, the final design of the air stripper will be determined by the total amount of VOCs requiring removal.

2.3.5 In-Situ Biological Treatment

Biodegradation occurs by microbial activity naturally present in ground water and soils. In-situ biological degradation involves the stimulation of this process in order to break down certain organic compounds such as petroleum hydrocarbons. Microorganisms use organic compounds which contain only carbon, hydrogen, and oxygen for nourishment. Certain cyanobacteria, yeasts, and molds have been shown to aerobically oxidize petroleum hydrocarbons. The microorganisms feed on the organic compounds found in the ground water and the aquifer matrix and require oxygen and water in order to survive.

While the biological treatment of ground water occurs in-situ, the water is initially pumped to the surface. A mixing tank is used to add nutrients (such as nitrogen, phosphorus, and trace elements) and oxygen sources (such as hydrogen peroxide) in order to optimize microbial activity. The ground water is then returned to the aquifer either by an infiltration gallery or by injection wells (see Figure 2-2). Treatment of contaminated soil may also be achieved by percolating water mixed with nutrients and an oxygen source through the affected soil. Factors influencing biodegradation include:

- Levels of contamination;
- Dissolved oxygen levels;
- Oxidation reduction potential;
- Temperature;
- Water and soil pH;
- Aquifer and soil permeability;
- Natural microbial community; and
- Nutrient availability.



1641

Figure 2-2. Schematic of In-Situ Biological Treatment System

Few of the listed data have been collected for the sites in the East Area. Prior to design, the collection of these data on a site-specific basis would be necessary.

2.3.6 Soil Vapor Extraction

To treat petroleum hydrocarbon contamination with soil vapor extraction, a blower is used to induce a vacuum in the soil through a series of trenches or wells (Figure 2-3). The petroleum hydrocarbon compounds then volatilize and are transported to the surface. As with air stripping, the off-gas may require treatment to acceptable air limits. To aid in inducing the vacuum the treated area could be covered with a synthetic membrane.

Factors influencing soil vapor extraction are:

- Soil moisture content;
- Soil porosity and permeability;
- Clay content of soil;
- Organic/mineral content of soil;
- Temperature;
- Wind and barometric pressure;
- Evaporation; and
- Precipitation.

Prior to design, the collection and evaluation of these data would be necessary on a site-specific basis.

Increases in soil moisture content, clay content, organic/mineral content, and precipitation decrease volatilization and increase treatment time. Increases in soil porosity, soil permeability, temperature, wind, barometric pressure, and evaporation increase volatilization.

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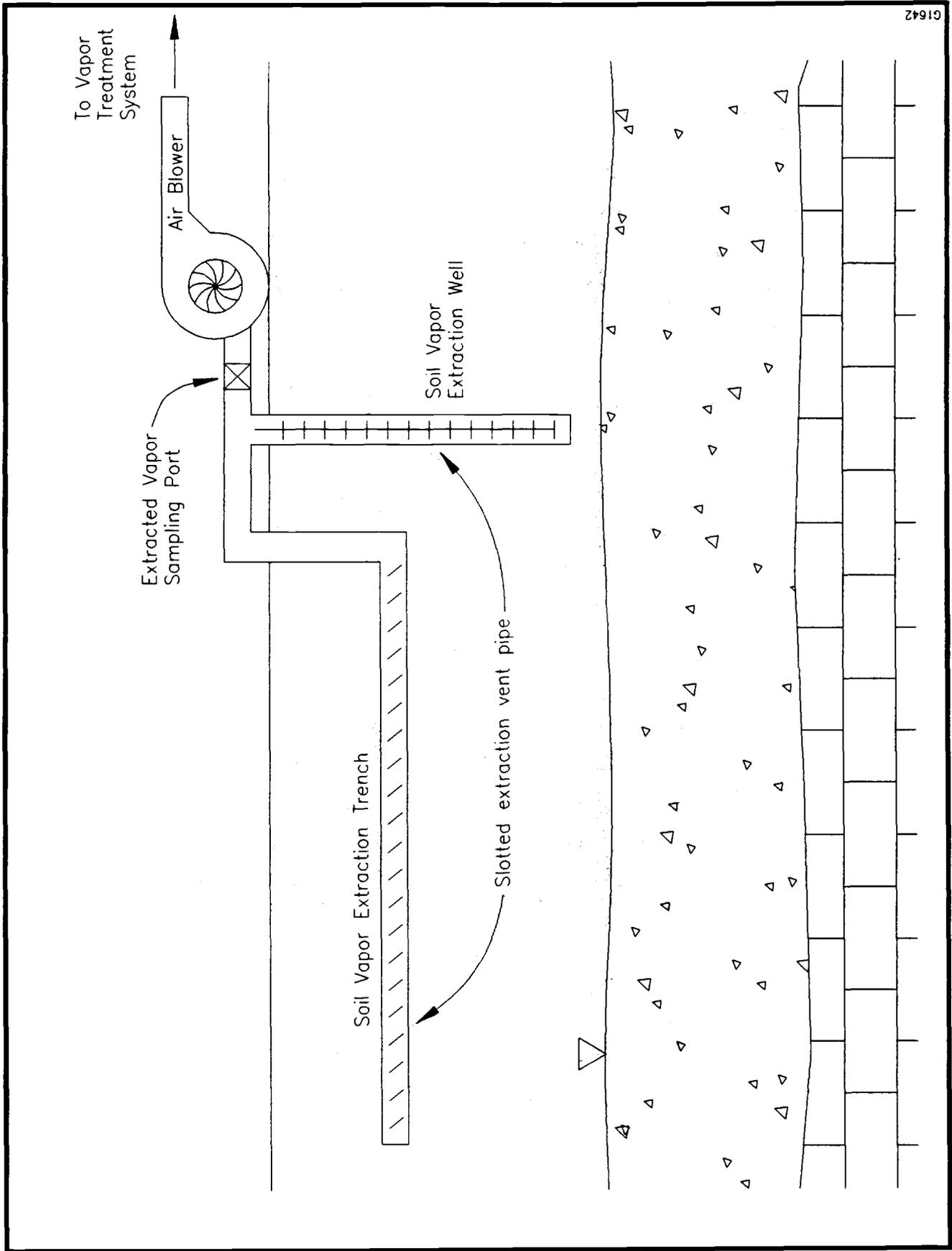


Figure 2-3. Schematic of Soil Vapor Extraction System

2.3.7 Soil Piles

In this technology, the contaminated soil is excavated and placed in a pile at a remote location for treatment. The soil pile is constructed such that volatilization and biodegradation are enhanced in the soil. The pile is built by placing a plastic liner on the ground on which 1 to 2 feet of contaminated soil is placed. Drain pipes are then laid across the pile and more soil is added. The next pipe layer is placed cross-wise to the first. This is continued until the desired number of lifts are reached. Fertilizer may be added between lifts to promote biodegradation. The pile is covered with black plastic to control run-off, and by absorbing heat, increases the volatilization and biodegradation rates. Volatile gases are collected by pipes and discharged. To enhance treatment, air can be drawn through pipes by a blower.

2.3.8 Secondary Treatment Systems

Air stripping is the only primary treatment option considered which may require secondary treatment. If the air/vapor emissions from the stripping tower exceed state standards, a secondary treatment will be required.

Regulatory Requirements

Two exemptions (68 and 118) from the Texas Air Control Board (TACB) Standard Exemption List (August 11, 1989) define the criteria for requiring emission control devices for air stripping, soil vapor extraction, or soil piles. Exemption 68 allows steam, air, or inert gas stripping provided that the total emissions or air contaminants, excluding nitrogen, do not exceed 5 pounds per hour (lb/hr). Furthermore, the exemption allows combustion of stripped vapors as long as the total emissions of contaminants (excluding nitrogen, carbon dioxide, air, oxygen, and water vapor) do not exceed 5 lb/hr. Exemption 68 requires soil stripping operations to be at least 1,000 feet from any residence, structure, or recreational area not occupied or used solely by the operator or owner of the property on which the operations are conducted.

Compounds not specifically listed in the exemption may be stripped as long as they meet the requirements of Standard Exemption 118 paragraphs (b), (c), and (d).

Exemption 118 presents air emission screening levels for benzene. As a component of the final design process, the performance of air dispersion modeling will be needed to verify that the treatment locations proposed in this study are acceptable relative to the screening level. Exemption 118(b) further restricts the placement of the air or soil stripping treatment system. The exemption states that "emission points associated with the facilities or changes shall be located at least 100 feet from any off-plant receptor."

To prevent emissions of air contaminants from exceeding the 5 lb/hr allowed by Standard Exemption 68, the maximum VOC concentration in the ground water at Carswell AFB that could be treated without air emission control devices (assuming a 100% stripping efficiency) would be 990 g/L at a ground-water flow rate of 10 gpm. For soil treatment, the maximum VOC concentration and vapor extraction rate cannot be determined until additional soil sampling and analysis is performed.

The two potential sites for the treatment pad(s) at Carswell AFB were selected to comply with the requirements of Standard Exemptions 68 and 118. No other special considerations or construction requirements are necessary for air stripping, soil vapor extraction, or soil piles.

Secondary Treatment Options

Two types of secondary treatments considered for the air/vapor stream are granular activated carbon (GAC) adsorption and fume incineration-catalytic conversion.

Activated carbon treatment removes organic substances from the air/vapor stream by adsorption onto the large internal surface area of specially prepared carbon. When the adsorptive capacity of activated carbon

is exhausted, the activated carbon is then removed and is either thermally regenerated or disposed of as a hazardous waste.

Fume incineration-catalytic conversion converts the VOC contaminants to carbon dioxide and water vapor. The gas stream is pulled off the air-stripping unit or vacuum extraction blower and is passed through a burner. The burner pre-heats or combusts the gases to catalyzing temperature. The heated gases then pass over the catalyst where an exothermic reaction breaking down the hydrocarbons takes place. The gas stream is then discharged to the atmosphere.

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3.0 DEVELOPMENT AND SCREENING OF ALTERNATIVES

Remedial actions for the East Area of Carswell AFB should reduce the concentrations of volatile organic contaminants in the Upper Zone ground water and soils to meet the established remedial action objectives (RAOs) and criteria. Remedial action alternatives that achieve RAOs for the four East Area sites were developed using the technologies identified in Section 2.

The screening conducted (see Section 2) identified applicable technologies for remedial actions in the East Area. The technologies are generally media-specific, so a complete remedial action could consist of several technologies. Some technologies are applicable only in the support of other, "primary" technologies. Good examples of "secondary" technologies, or those that support a primary technology, are oil/water separation pretreatment, carbon or fume incineration treatment for off-gases, and effluent disposal options. Secondary technologies may be common to all alternatives or specific to a few. Primary technologies are technologies upon which a remedial action alternative may be based. Typically, primary technologies are treatment technologies (e.g., air stripping and in-situ bio-treatment). Remedial action alternatives are then developed by combining applicable primary technologies with applicable secondary technologies for each medium.

For the East Area, remedial action alternatives were developed for each affected medium at each of the four sites. As stated in Section 1, the need for and potential magnitude of soils remedial action is unresolved. Therefore, the remedial action alternatives for soils have not been combined with the remedial action alternatives for ground water and surface water. Remedial action alternatives developed for the four East Area sites are described in Section 3.1. The opportunities for combining or coordinating soils remedial actions with other media-specific and site-specific remedial actions is discussed in Section 4.6.

Once developed, each of the remedial actions were evaluated against the short- and long-term aspects of three broad criteria: effectiveness,

implementability, and cost. The evaluations were used as a screening tool to eliminate inappropriate remedial action alternatives and to identify alternatives for a more detailed evaluation. Evaluations for each of the alternatives are given in Section 3.2. A summary of the remedial action alternatives remaining after screening is given in Section 3.3.

3.1 Development of Alternatives

Sections 3.1.1 through 3.1.4 discuss alternatives for the four sites.

3.1.1 Site LF01--Landfill 1

Alternative 1, the no-action alternative, is the only alternative applicable to current Upper Zone ground-water conditions at Site LF01 [i.e., no contaminants detected above MCLs in the latest (1990) sampling round]. No records exist concerning the type of waste disposed of at or near the landfill. While the Stage 1, Stage 2, and the most recent investigations have detected evidence of solvent- and metal-bearing wastes, the constituent concentrations in the ground water do not exceed the criteria established for satisfaction of the remedial action objectives (RAOs). The combined effects of the proximity of the landfill to the West Fork of the Trinity River, the permeability of the upper hydraulic zone, and the length of time the waste has been buried could have resulted in the migration of a significant portion of the waste constituents from the landfill. The data also suggest that some natural degradation of the waste has occurred, as evidenced by the presence of cis-1,2 dichloroethene and vinyl chloride, which were not historically used on base, but are transformation products of tetrachloroethene and TCE. Any attempts to contain or otherwise isolate the waste source may hinder natural attenuation processes.

The baseline risk assessment for the site indicated that the total hazard index for non-carcinogenic effects was significantly lower than the level of concern established by EPA, and that the individual cancer risk for the maximum on-site and off-site exposed individual was 10^{-10} . Furthermore, assuming that the river is the only practical pathway for terrestrial

organisms to be exposed to any contaminants released from the landfill, then the risk to terrestrial wildlife that use the river as a drinking water source and to aquatic organisms in the river is interpreted to be minimal. Attempts to pump and treat ground water from Site LF01 would increase the risk of exposure by bringing contaminated water to the surface. Treatment of ground water extracted from Site LF01 would remove minimal amounts of contaminants. Poor treatment efficiencies for such low concentrations in ground water would be expected. Because there are no apparent risks to human health or the environment from the site, and because pumping and treating ground water would achieve minimal reductions in contaminant mass, the no-action alternative is the only feasible alternative for Site LF01.

The no-action alternative for Site LF01 would include long-term monitoring of contaminant concentrations in the ground water. Since there are no records of the nature of wastes formerly disposed of in Landfill 1, samples should be analyzed for aromatic and chlorinated volatile organics and dissolved metals on a quarterly basis; and semivolatile organics, pesticides, herbicides, and PCBs on an annual basis. Evidence of increased migration, such as significantly or consistently higher contaminant concentrations, or significant changes in the occurrence of contaminants, would justify the initiation of further evaluation.

3.1.2 Site SD13--Abandoned Gasoline Station and Unnamed Stream

As in the case of Site LF01, Alternative 1, the no-action alternative, is the only alternative applicable to current Upper Zone ground water and surface water conditions at Site SD13 [i.e., no dissolved metals or volatile organic compound concentrations above MCLs in the latest (1990) sampling round]. The source of contaminants detected above MCLs in the past in Unnamed Stream is interpreted to be fuel releases from Site ST14 (POL Tank Farm) which were channeled to the stream through a french drain system and an oil/water separator. Alternatives to address contamination from Site ST14 are described in Section 3.1.3. Although low levels of volatile organic compounds were detected in ground-water samples collected in 1990 from monitor wells installed around the abandoned gasoline station, no concentrations were above

the remedial action objectives (RAOs). Furthermore, based upon contaminant concentrations, the source does not appear to be the abandoned station, and may be located at the POL Tank Farm. Surface water samples collected in 1990 also satisfied the RAOs.

The baseline risk assessment for Site SD13 indicated that the total hazard index for non-carcinogenic effects was significantly lower than the level of concern established by EPA, and that the individual cancer risk for inhalation of ambient concentrations of volatile organic contaminants did not exceed 1.4×10^{-8} . The exposure pathways and risks to terrestrial wildlife are similar to those presented by Site LF01. Attempts to pump and treat contaminated ground water would increase the risk of exposure to the extracted ground water and to treatment by-products. As they would at Site LF01, treatment processes would be expected to remove only minimal concentrations (and indirectly minimal masses) of contaminants from the ground water, because of the difficulty in extracting them from the formation and the low treatment efficiencies expected for such low influent concentrations. Because Site SD13 presents minimal, if any, risks to human health and the environment, and because pumping and treating ground water would achieve insignificant reductions in contaminant mass, the no-action alternative is the only feasible alternative for Site SD13.

The no-action alternative for Site SD13 would include long-term monitoring of contaminant concentrations in the ground water and surface water in Unnamed Stream. Based on the ground-water and surface water constituents detected historically, existing monitor wells and established surface water sampling points on Unnamed Stream should be sampled quarterly and analyzed for volatile aromatic compounds and dissolved metals. Evidence of increased migration such as significantly or consistently higher contaminant concentrations, or significant changes in the occurrence of the contaminant plume, would justify the initiation of further evaluation.

3.1.3 Site ST14--POL Tank Farm

Because of the limitations of the soils analytical data for Site ST14 (previously discussed), media-specific remedial alternatives for this site were developed and screened separately. Section 3.1.3.1 describes preliminary remedial alternatives for ground water at Site ST14, and Section 3.1.3.2 discusses potentially applicable preliminary remedial alternatives for contaminated soils.

3.1.3.1 Preliminary Ground-Water Alternatives

Nine remedial alternatives (including the no-action alternative) were developed to address Upper Zone ground-water contamination at Site ST14. The component technologies of each of these alternatives are identified and numbered in Table 3-1. Except for the no-action alternative, two secondary technologies are common to all alternatives: oil/water separation prior to primary ground-water treatment, and long-term ground-water monitoring.

Oil/water separation is included as a pre-treatment technology because more than 2 feet of immiscible hydrocarbon was present in one of the site monitor wells sampled in 1990. Pre-treatment of the hydrocarbon/water mixture will separate the hydrocarbon from the ground water, thus increasing the treatment efficiency, decreasing the operating and maintenance requirements, and removing a large mass of concentrated contaminants using a relatively simple process. The separated hydrocarbon phase will be temporarily stored on-site (less than 90 days) and will be periodically shipped off-site for recycling, if possible, or for disposal.

Long-term monitoring at Site ST14 will make use of the existing monitoring well network plus additional wells. The Upper Zone monitor well network currently in place at Site ST14 consists of nine wells. It is anticipated that all existing wells, and up to five additional wells, installed beyond the downgradient limits of the existing plumes of

TABLE 3-1. PRELIMINARY GROUND-WATER REMEDIAL ALTERNATIVES^a FOR
SITE ST14--POL TANK FARM

| Technology | Alternatives | | | | | | | | | |
|----------------------------------|--------------|----|----|----|---|----|----|----|---|---|
| | 1 | 2A | 2B | 2C | 3 | 4A | 4B | 4C | 5 | |
| Monitoring | • | • | • | • | • | • | • | • | • | • |
| Interceptor Trenches | NA | • | • | • | • | | | | | |
| Extraction Wells | NA | | | | | • | • | • | • | |
| Oil/Water Separator | NA | • | • | • | • | • | • | • | • | |
| Air Stripping | NA | • | • | • | | • | • | • | | |
| In-Situ Bio-Treatment | NA | | | | • | | | | | • |
| Treated Ground-Water ReInjection | NA | • | | | • | • | | | | • |
| Ground-Water Disposal to POTW | NA | | • | | | | • | | | |
| Ground-Water Discharge to Stream | NA | | | • | | | | | • | |

NA - No Action

^a Preliminary remedial alternatives do not include secondary ground-water treatment (i.e., fume incineration or carbon adsorption for stripped contaminants).

contamination and the ground-water extraction system, will be required to monitor the effectiveness of the selected ground-water remedial alternative. These wells will be sampled and analyzed for volatile aromatic compounds, total petroleum hydrocarbons, and dissolved metals on a quarterly basis for the duration of site remediation.

Each preliminary alternative developed for Site ST14 is described below.

Alternative 1--Alternative 1, the no-action alternative, provides a baseline for comparison of other alternatives that involve implementation of remedial actions. The no-action alternative consists solely of the previously described long-term monitoring of Upper Zone ground water in the vicinity of Site ST14. If an imminent risk becomes apparent from the monitoring data, further action would then be undertaken.

Alternative 2 (A, B, C)--The three variations of Alternative 2 (2A, 2B, and 2C) differ only in the treated ground-water disposal option. The primary remedial technology utilized in Alternative 2 is air stripping. The secondary remedial technologies that support air stripping are ground-water extraction/interceptor trenches and effluent disposal. The contaminant plume in the ground water would be intercepted by two extraction/interceptor trenches, the approximate locations of which are shown in Figures 3-1 through 3-3. Placement of the trenches is based on passive interception of the interpreted benzene plumes shown in the figures. The extraction/interceptor trenches should also serve as a hydraulic barrier for downgradient containment of the existing ground-water plumes. The ground water extracted from the trenches would be pumped to an air stripper where volatile organic contaminants would be removed. At the hydrocarbon constituent concentrations expected in ground water, it is assumed the air stripper can be operated at a rate that does not require secondary treatment of emissions (i.e., fume incineration and/or activated carbon). The treated ground water would then be disposed of in one of three ways, described below.

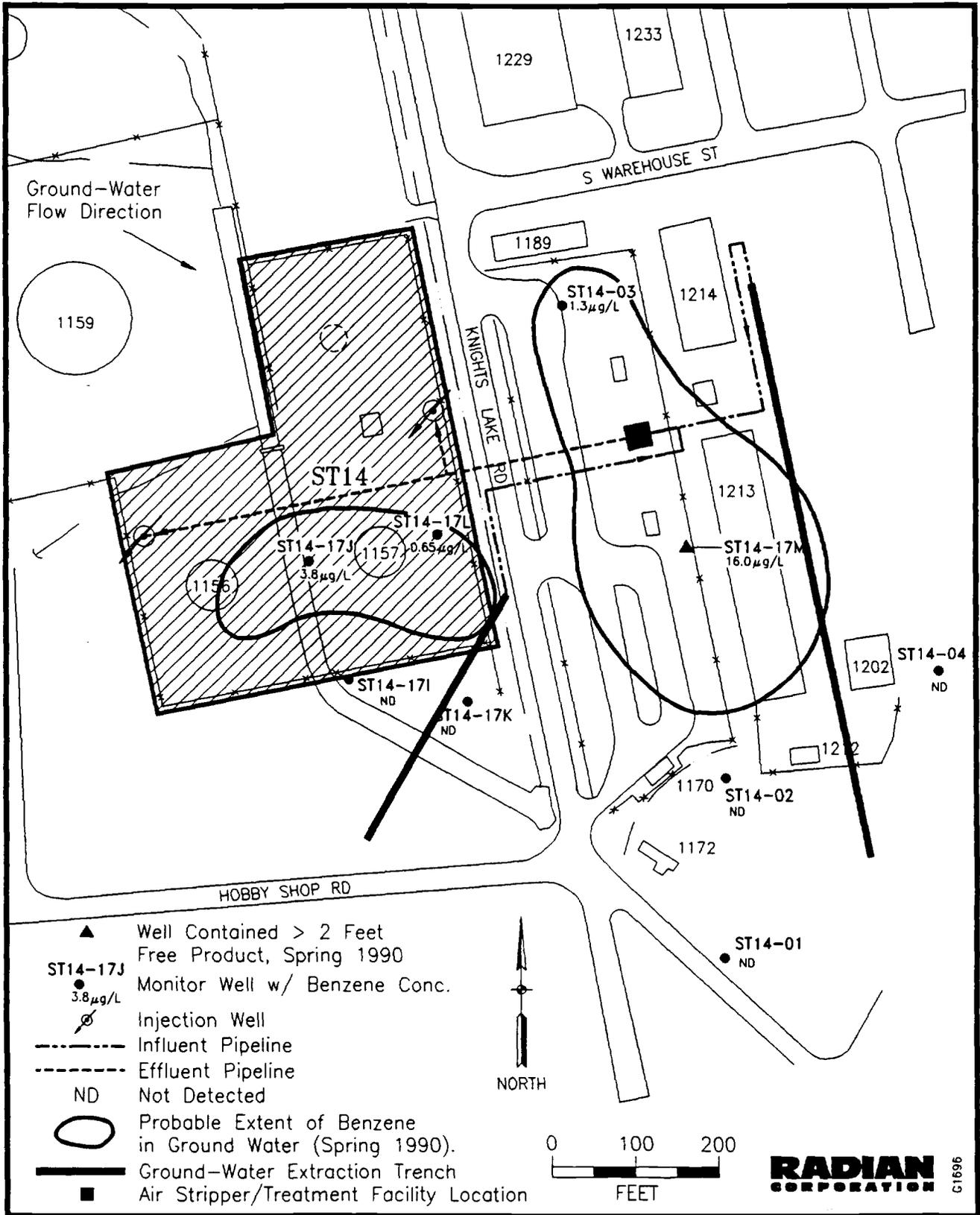


Figure 3-1. Basic Remedial Action Components of Alternative 2A, Site ST14, East Area, Carswell AFB, Texas

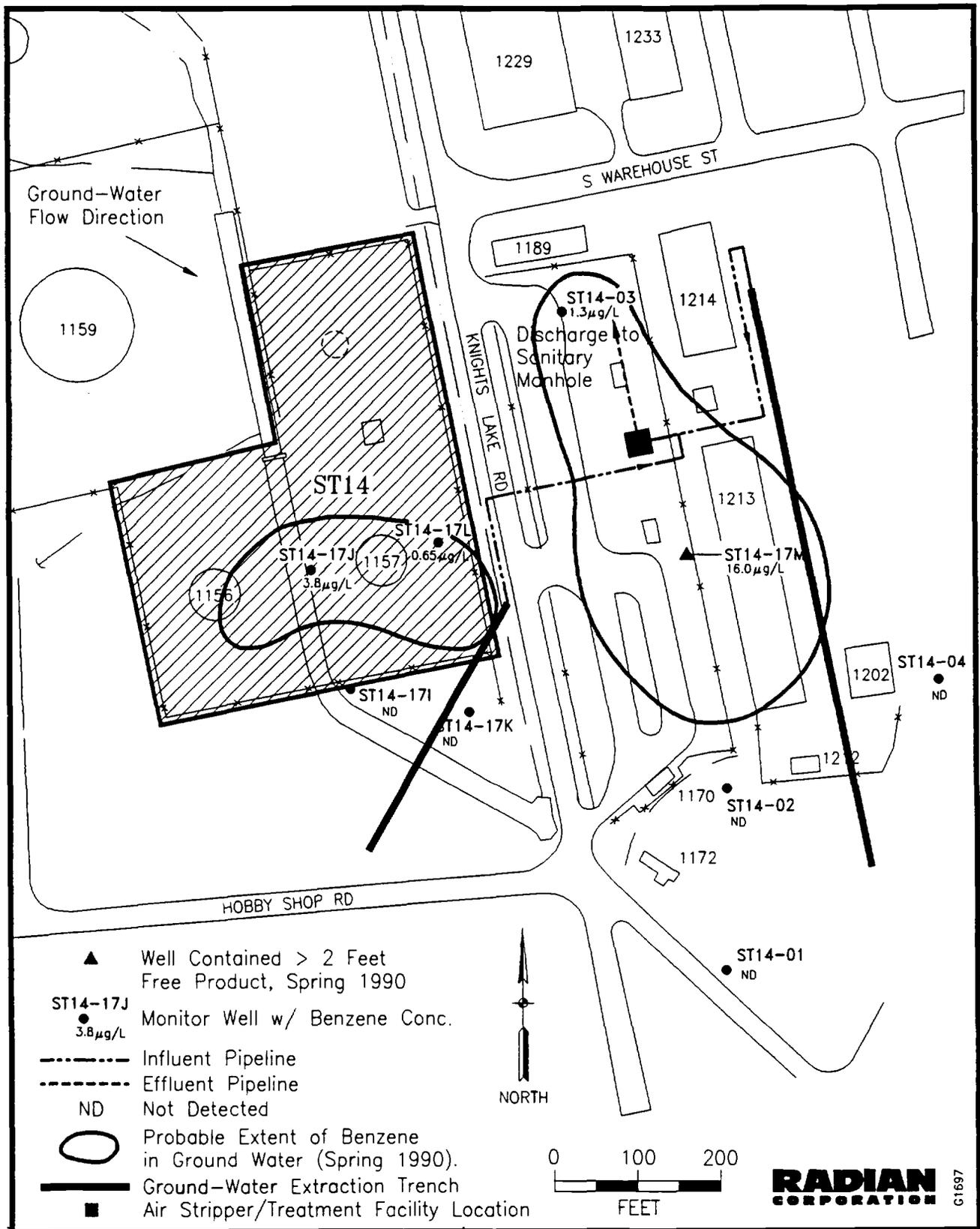


Figure 3-2. Basic Remedial Action Components of Alternative 2B, Site ST14, East Area, Carswell AFB, Texas

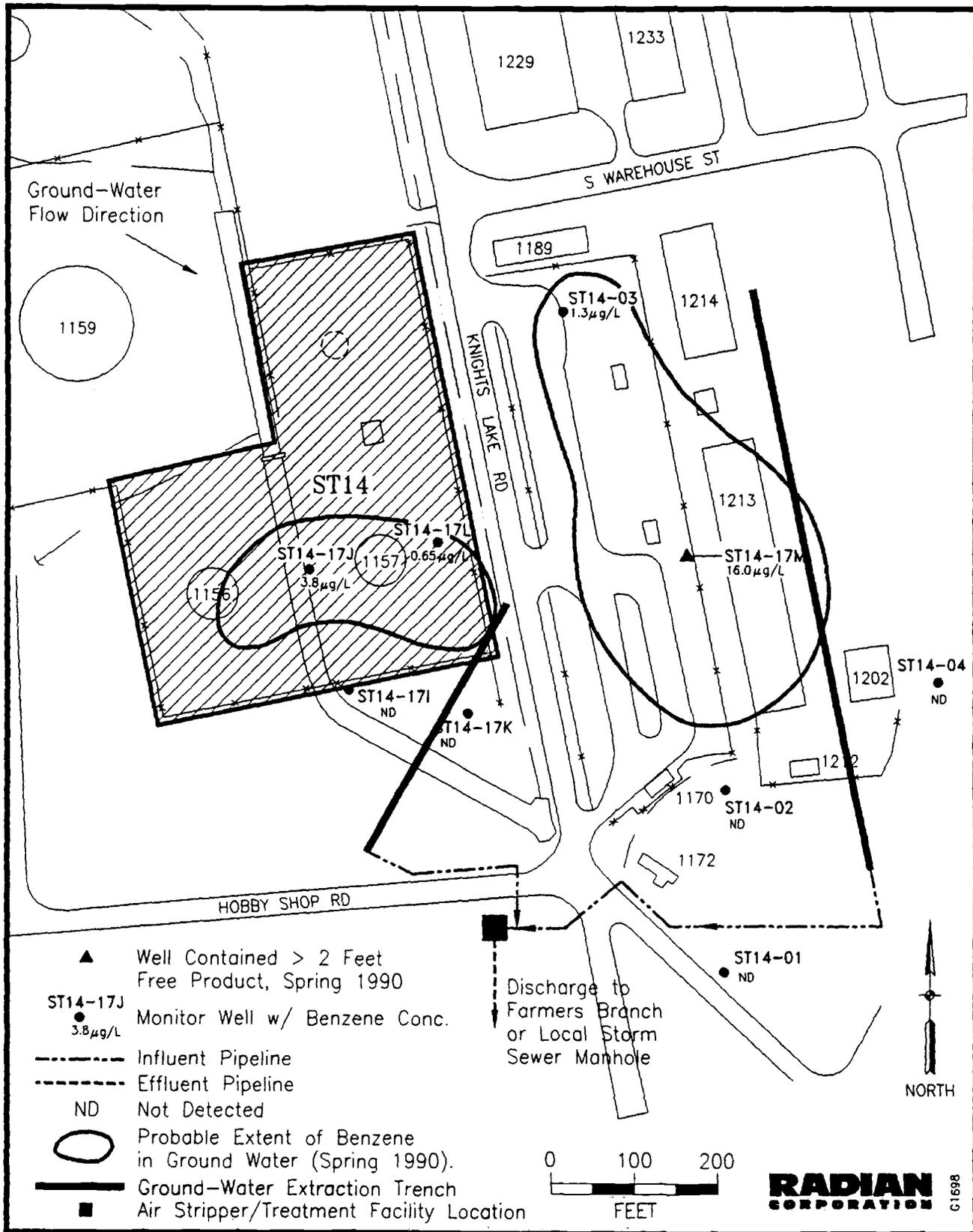


Figure 3-3. Basic Remedial Action Components of Alternative 2C, Site ST14, East Area, Carswell AFB, Texas

The three variations of Alternative 2 (2A, 2B, and 2C) differ only in the method of disposal for treated effluent. In Alternative 2A, treated ground water is re-injected into the upper hydrogeologic zone. Re-injection would be accomplished through the use of infiltration galleries or extraction wells located upgradient of the contaminant plume. Re-injection of the treated effluent would promote additional ground-water flow through the contaminated portion of the Upper Zone Aquifer, thus potentially enhancing remediation. The components for Alternative 2A are shown conceptually in Figure 3-1. In Alternative 2B, treated effluent is discharged to a sanitary sewer in the vicinity and ultimately re-treated at the local POTW. Discharge to the sanitary sewer with additional treatment at the POTW provides a contingency for treatment even in the event of an upset condition at the air stripper. The components for Alternative 2B are shown conceptually in Figure 3-2.

In Alternative 2C, the treated effluent is discharged to the base storm sewer or nearby drainage ditch, which ultimately flows into Farmers Branch and the West Fork of the Trinity River. During upset conditions at the air stripper, on- and off-base personnel, as well as wildlife, could potentially be exposed to contaminated ground water or to volatilized constituents. The components for Alternative 2C are shown conceptually in Figure 3-3.

In all three variations of Alternative 2, construction of the ground-water extraction/interceptor trenches potentially involves excavation of contaminated soils. It should be noted that treatment of any contaminated soils generated in implementation of Alternative 2 will be required for all three variations. Because of the lack of data regarding contaminated soils in the vicinity of Site ST14, disposal and/or treatment options for contaminated soils will be deferred until appropriate data have been collected. Contaminated soils generated during the ground-water remediation will be temporarily stored (less than 90 days) on-site until a suitable alternative has been selected for all of the contaminated soils at Site ST14.

Alternative 3--Alternative 3 differs from Alternative 2 in that it includes in-situ biological treatment instead of air stripping as the primary ground-water treatment technology. As discussed in Section 2.3.5, the in-situ biological treatment technology involves extraction of ground water, mixing ground water with specialized bacteria and nutrients, and re-injecting the water into the Upper Zone. This technology thereby precludes the other two treated effluent disposal options (discharge to POTW or stream). The major components of Alternative 3 are shown in Figure 3-4.

Construction of the ground-water extraction/interceptor trenches for Alternative 3 may involve excavation of potentially contaminated soils. Treatment of any contaminated soils generated from the remedial action will be required. However, because of the lack of data regarding contaminated soils in the vicinity of Site ST14, disposal and/or treatment options for contaminated soils will be deferred until appropriate data have been collected. Soils generated during the ground-water remediation will be temporarily stored (less than 90 days) on-site until a suitable alternative has been selected for all of the contaminated soils at Site ST14.

Alternative 4 (A, B, C)--Alternative 4 utilizes the same primary remedial technology, air stripping, as Alternative 2. The difference between Alternatives 2 and 4 is the secondary technology used to extract/intercept contaminated ground water. An extraction well is used instead of an extraction/interceptor trench to create the hydraulic barrier (cone of depression) and for recovery of contaminated ground water for treatment. Figures 3-5 through 3-7 illustrate the basic components of Alternative 4.

The discharge rate for the extraction well for Site ST14 is estimated to be between 10 and 20 gpm. The proposed well location was chosen to capture all existing ground-water contamination. Although the interpreted plumes shown in Figure 1-6 are based on benzene concentrations detected in 1990, the well location was selected to capture any related hydrocarbon constituents. Calculations assumed steady state flow conditions, a

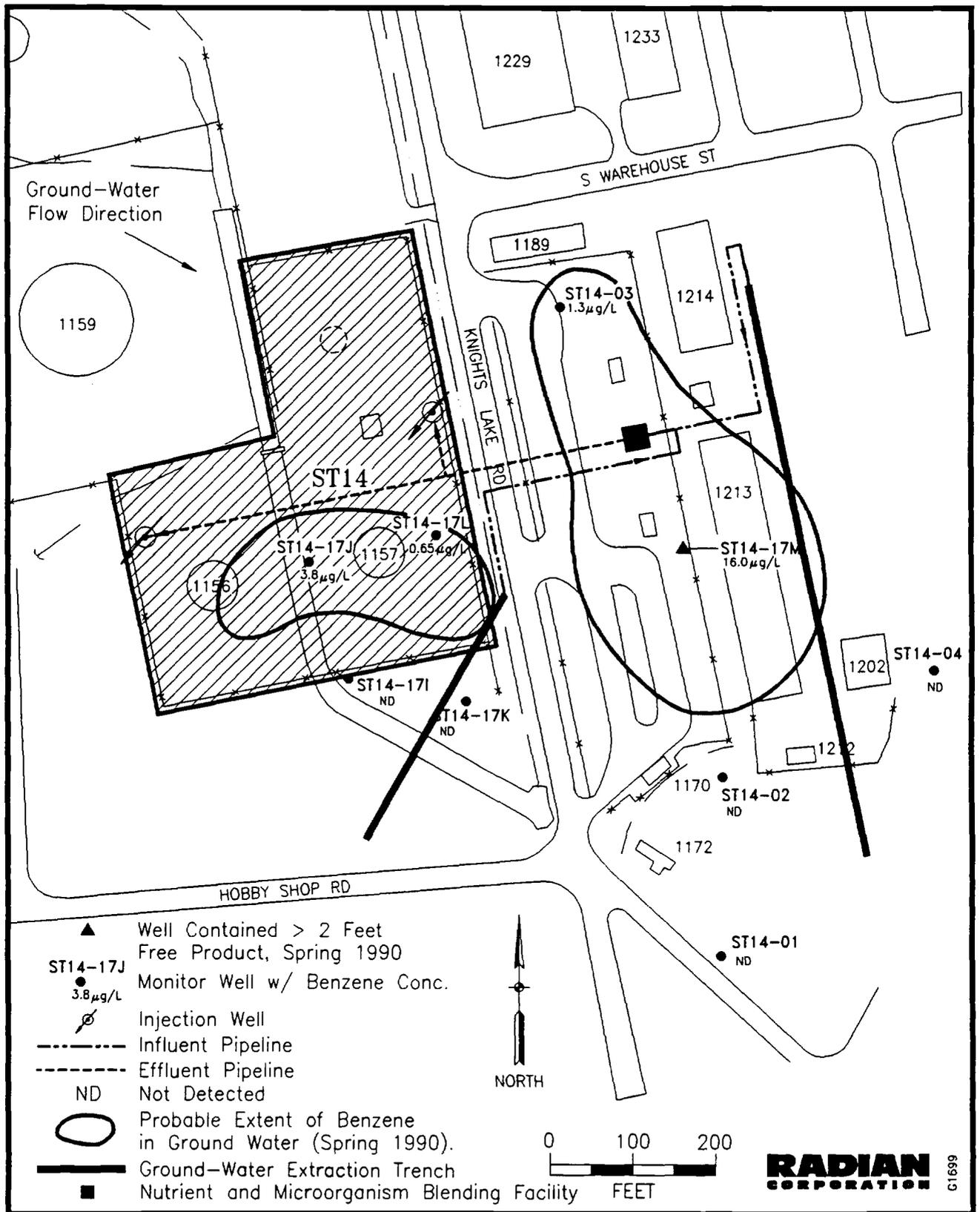


Figure 3-4. Basic Remedial Action Components of Alternative 3, Site ST14, East Area, Carswell AFB, Texas

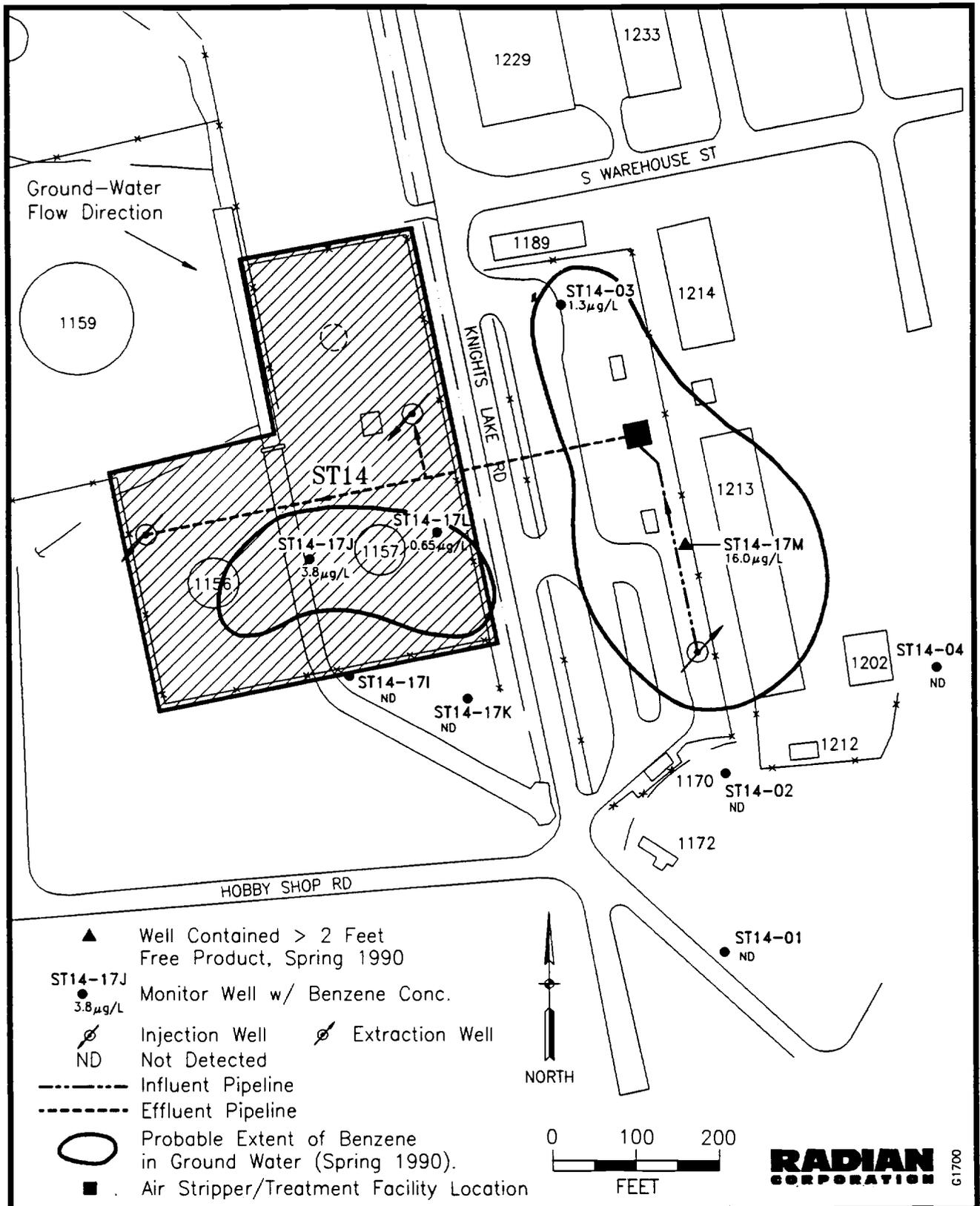


Figure 3-5. Basic Remedial Action Components for Alternative 4A, Site ST14, East Area, Carswell AFB, Texas

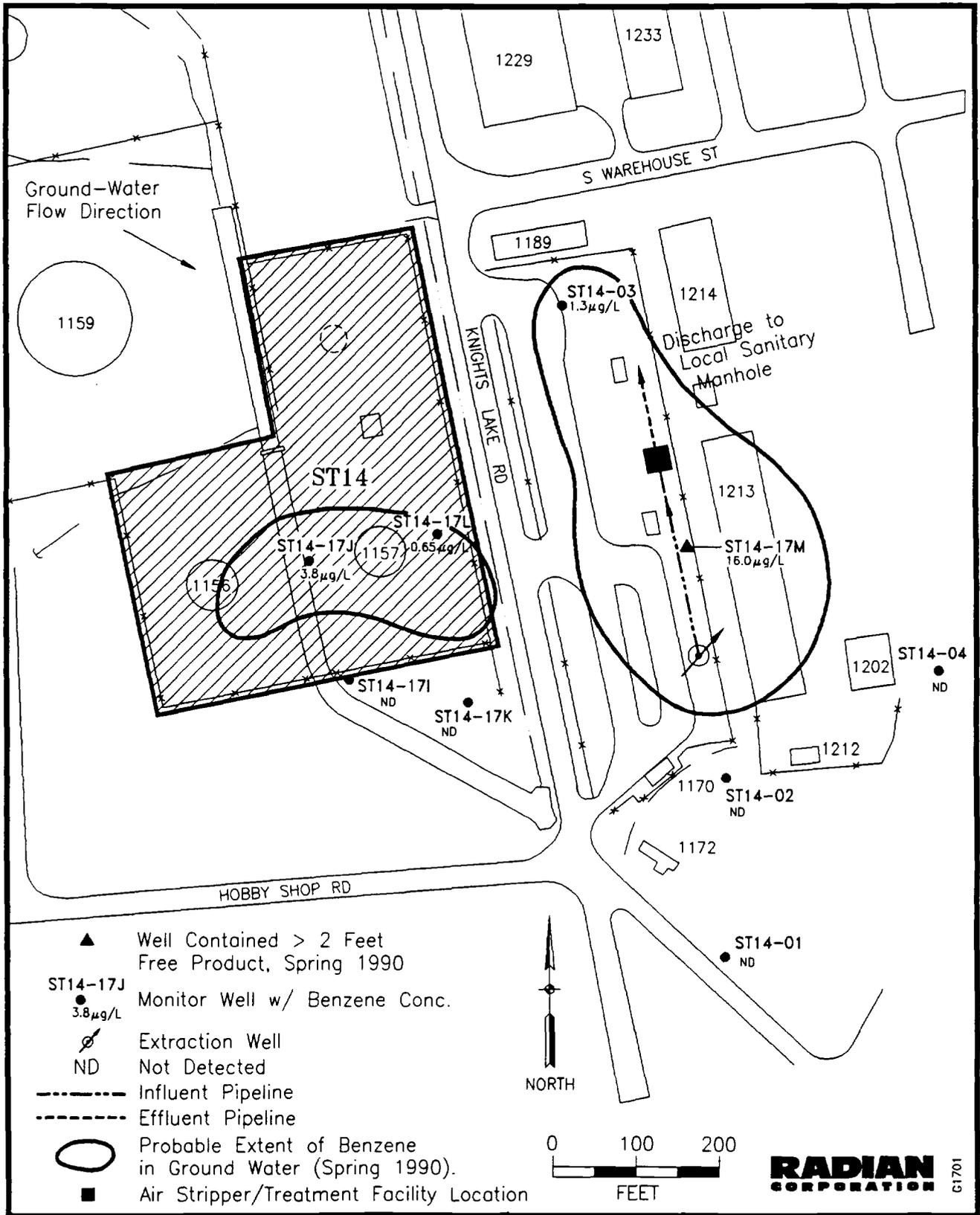


Figure 3-6. Basic Remedial Action Components for Alternative 4B, Site ST14, East Area, Carswell AFB, Texas

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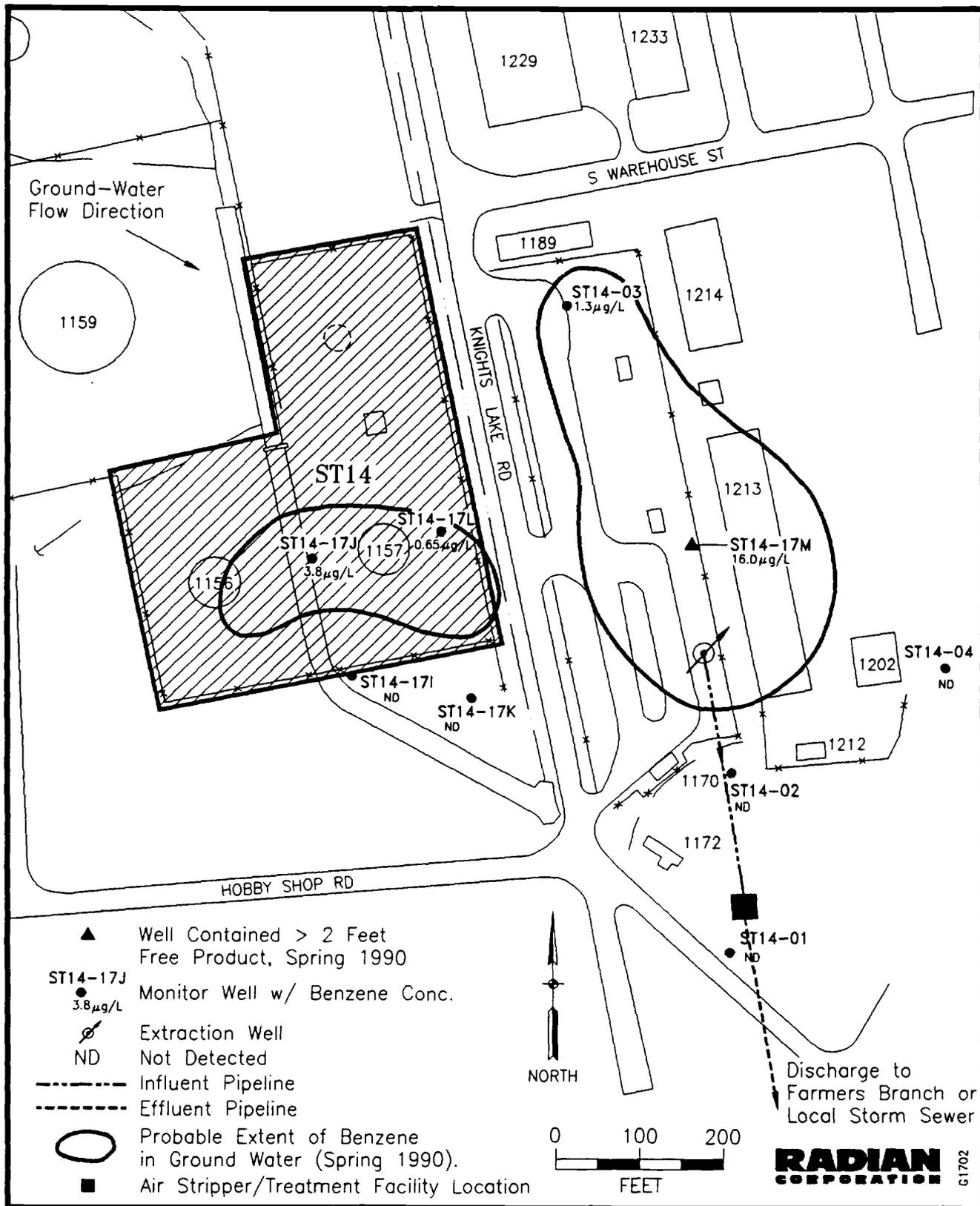


Figure 3-7. Basic Remedial Action Components for Alternative 4C, Site ST14, East Area, Carswell AFB, Texas

homogenous, isotropic, infinite aquifer, and a fully penetrating extraction well. The aquifer properties were estimated by using the data from the East Area RI report (Radian 1991). The regional flow gradient was assumed to be 0.01 to the southeast and the saturated hydraulic conductivity was assumed to be 0.3 ft/day. The saturated thickness was estimated to be 8 feet. The proposed ground-water extraction well location and estimated extraction rates are preliminary estimates based on limited information on aquifer hydraulic properties. They would require field verification to support detailed design prior to remedial action implementation, if selected.

Alternative 5--Alternative 5 is the same as Alternative 3, except that an extraction well is substituted for the interceptor trenches. As a consequence, no excavation (and potentially no soil treatment) is required in this alternative. The basic components for Alternative 5 are shown in Figure 3-8.

3.1.3.2 Preliminary Soil Alternatives--Site ST14

Four remedial alternatives (including the no-action alternative) were developed to address soil contamination potentially present at Site ST14. The component technologies of each alternative are identified in Table 3-2.

As previously noted, the only soils data for this site are from 1988. At that time, the evidence of soils contamination consisted primarily of detectable levels of total petroleum hydrocarbons (TPH) in three boreholes located in two separate areas of the site. Therefore, soil sampling to confirm the current existence of contamination at levels requiring remedial action, and the extent of soil contamination, if present, is a common element of all four alternatives. Each remedial alternative is described briefly below.

Alternative 1--Alternative 1, the no-action alternative, is similar to the no-action alternative described previously for ground water. The only

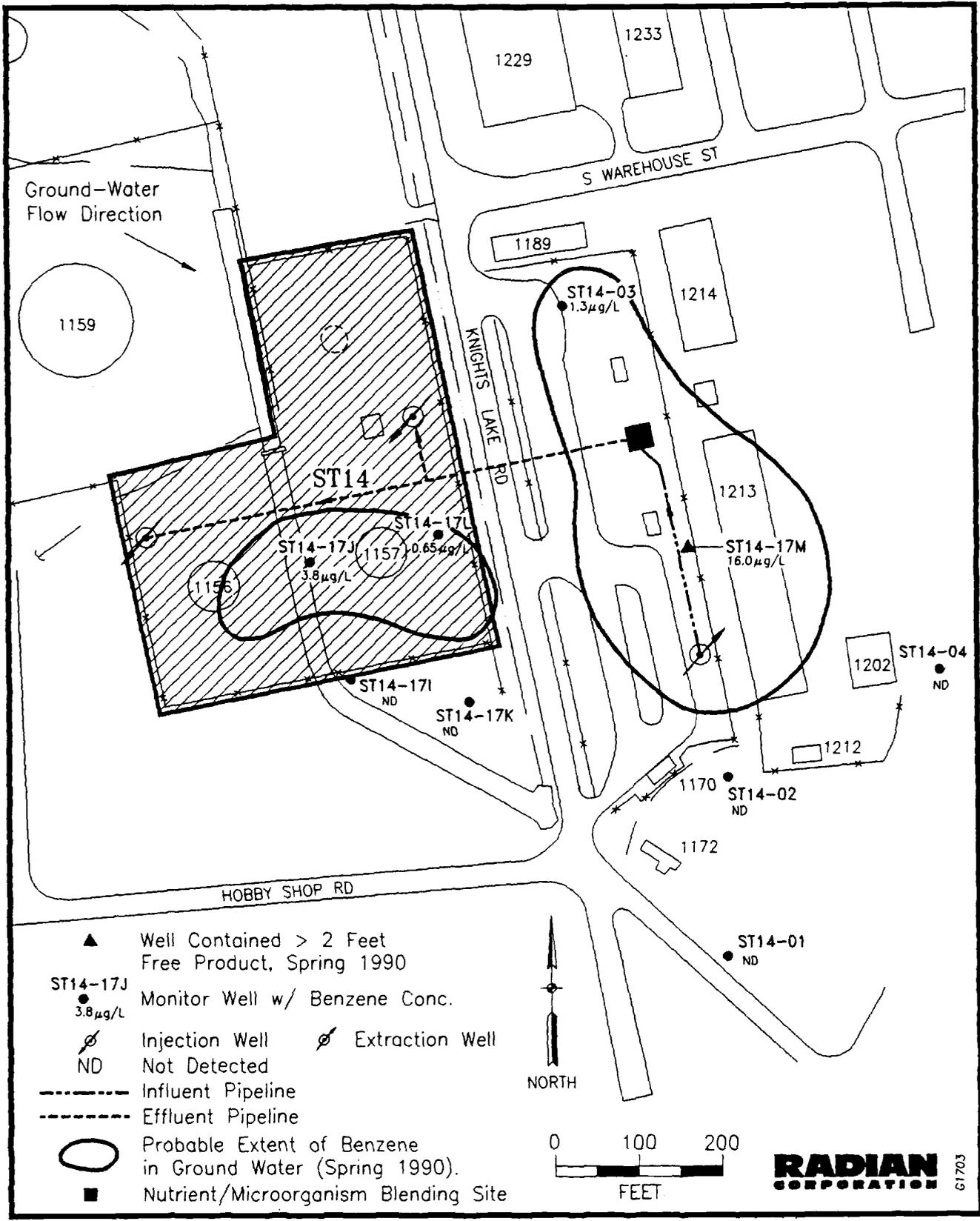


Figure 3-8. Basic Remedial Action Components of Alternative 5, East Area, Carswell AFB, Texas

TABLE 3-2. PRELIMINARY SOIL REMEDIAL ALTERNATIVES^a
FOR SITE ST14--POL TANK FARM

| Technology | Alternatives | | | | |
|-------------------------------|--------------|----|----|---|---|
| | 1 | 2A | 2B | 3 | 4 |
| Confirmation Sampling | • | • | • | • | • |
| Excavation | NA | | | • | |
| In-Situ Bio-Treatment | NA | | | | • |
| Soil Vapor Extraction | NA | • | • | | |
| Extraction Trenches | NA | • | | | |
| Extraction Wells | NA | | • | | |
| Soil Piles | NA | | | • | |
| On-Site Treated Soil Disposal | NA | | | • | |

NA = No Action

^a If required, pending results of additional soil sampling and analysis-- preliminary remedial alternatives do not include secondary treatment.

difference is that instead of long-term quarterly monitoring, a single round of soil and soil gas samples would be collected. Soil samples would be analyzed for TPH and BTEX to determine if previously detected (i.e., 1988) hydrocarbon constituents are currently present in concentrations that exceed RAOs, or constitute an unacceptable level of risk.

Alternative 2--Alternative 2 uses soil vapor extraction as the primary technology for remediation of contaminated soils. Soil vapors are removed using vapor extraction wells. Two variations of Alternative 2 were developed based on different methods of extraction. In Alternative 2A, extraction trenches are used to intercept soil gas, while in Alternative 2B soil gas is extracted using vapor extraction wells. If necessary, secondary vapor treatment (fume incineration or carbon adsorption) could be added to the system to meet air emission standards.

Alternative 3--In Alternative 3, contaminated soils will be excavated and treated in soil piles. Confirmation sampling and analysis are included to ensure that all contaminated soils are removed (laterally and vertically) and are treated to attain ARARs. Treated soils will be disposed of or used as clean fill at the base.

Alternative 4--In Alternative 4, soils are treated in-situ by introducing nutrient-enriched water to enhance biological degradation of hydrocarbon constituents. The in-situ biological treatment process for soils could be used in conjunction with in-situ biological treatment of the ground water. Sampling and analysis would be necessary to define the areas requiring treatment, as well as to confirm the effectiveness and completeness of the treatment process.

3.1.4 Site BSS--Base Service Station

As in the case of Site ST14, the limited soils data available for Site BSS require the development and screening of remedial alternatives on a media-specific basis.

3.1.4.1 Preliminary Ground-Water Alternatives

Nine remedial alternatives (including the no-action alternative) were developed to address Upper Zone ground-water contamination at Site BSS. The component technologies of each of these alternatives are identified in Table 3-3. These alternatives correspond to the alternatives identified by the same numbers for Site ST14, except that none of the alternatives for Site BSS include oil/water separation. No immiscible hydrocarbon lens has ever been observed in any of the Site BSS wells during IRP activities. Refer to the descriptions of the ground-water alternatives presented in Section 3.1.3.

The only technology common to all alternatives for Site BSS is long-term ground-water monitoring. Long-term monitoring at Site BSS will make use of the existing monitoring well network and additional monitor wells. The Upper Zone monitoring well network currently in place at Site BSS consists of three wells. It is expected that three or four additional monitor wells will be required downgradient of existing contamination to evaluate the effectiveness of the selected remedial alternative. Monitor wells should be sampled and analyzed for volatile aromatic compounds, TPH, and dissolved metals on a quarterly basis for the duration of the remedial action. However, because of the thin saturated zone and local variability in the occurrence of Upper Zone ground water at this site, it is possible that some wells may be dry during any given sampling event, especially after ground-water control technologies are in place.

As described in Section 3.1.3, Alternatives 2 through 5 are various combinations of ground-water treatment and disposal technologies and either extraction wells or interceptor trenches for ground-water recovery and hydraulic control. Figures 3-9 through 3-16 illustrate the fundamental components of Alternatives 2 through 5.

TABLE 3-3. PRELIMINARY GROUND-WATER REMEDIAL ALTERNATIVES^a FOR
SITE BSS--BASE SERVICE STATION

| Technology | Alternatives | | | | | | | | | |
|----------------------------------|--------------|----|----|----|---|----|----|----|---|--|
| | 1 | 2A | 2B | 2C | 3 | 4A | 4B | 4C | 5 | |
| Monitoring | • | • | • | • | • | • | • | • | • | |
| Interceptor Trenches | NA | • | • | • | • | | | | | |
| Extraction Wells | | | | | | • | • | • | • | |
| Air Stripping | NA | • | • | • | | • | • | • | | |
| In-Situ Bio-Treatment | NA | | | | • | | | | • | |
| Treated Ground-Water ReInjection | NA | • | | | • | • | | | • | |
| Ground-Water Disposal to POTW | NA | | • | | | | • | | | |
| Ground-Water Discharge to Stream | NA | | | • | | | | • | | |

NA - No Action

^a Preliminary remedial alternatives do not include secondary ground-water treatment.

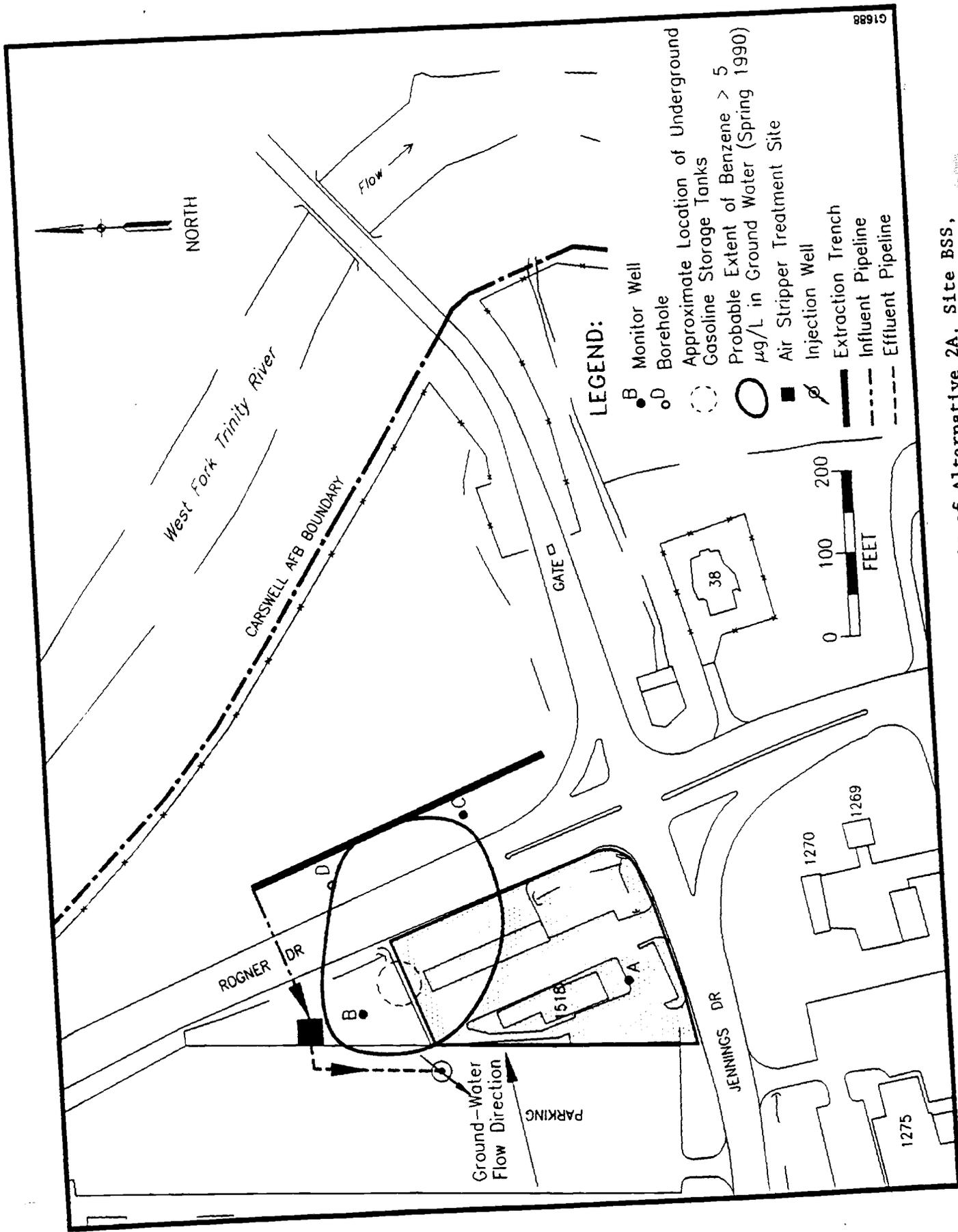
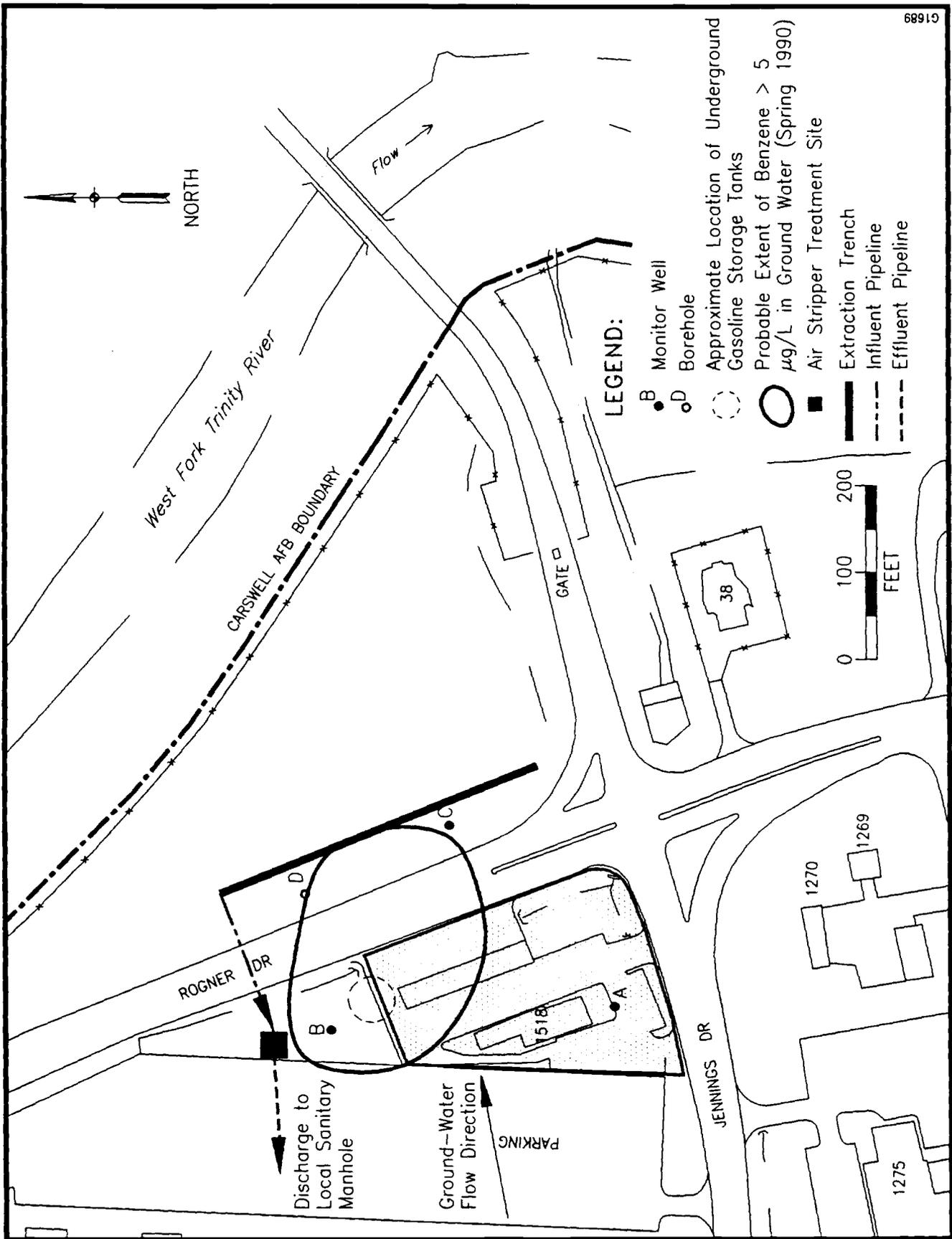
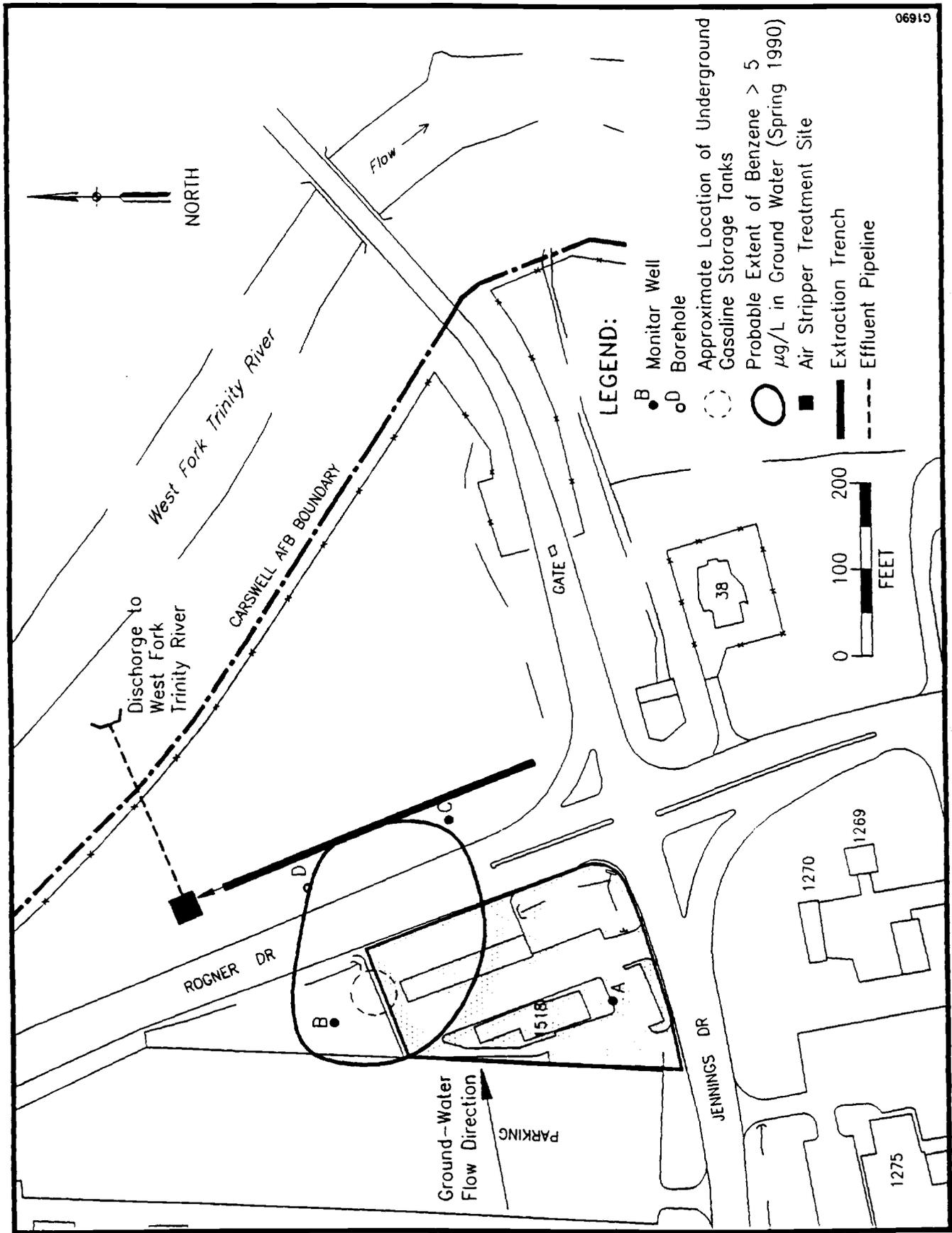


Figure 3-9. Basic Remedial Action Components of Alternative 2A, Site BSS, East Area, Carswell AFB, Texas



68910

Figure 3-10. Basic Remedial Action Components of Alternative 2B, Site BSS, East Area, Carswell AFB, TX



06915

Figure 3-11. Basic Remedial Action Components of Alternative 2C, Site BSS, East Area, Carswell AFB, Texas

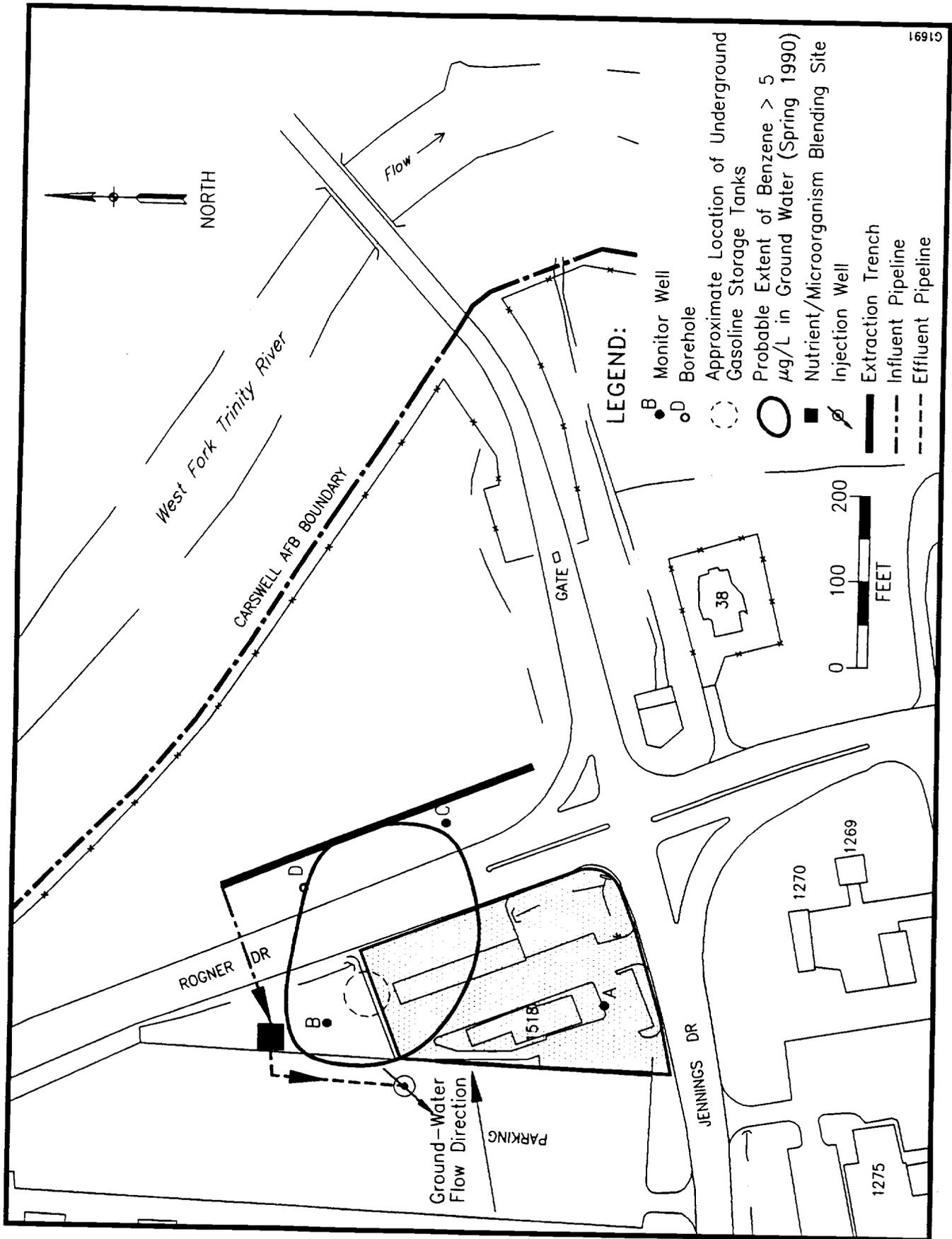


Figure 3-12. Basic Remedial Action Components of Alternative 3, Site BSS, East Area, Carswell AFB exas

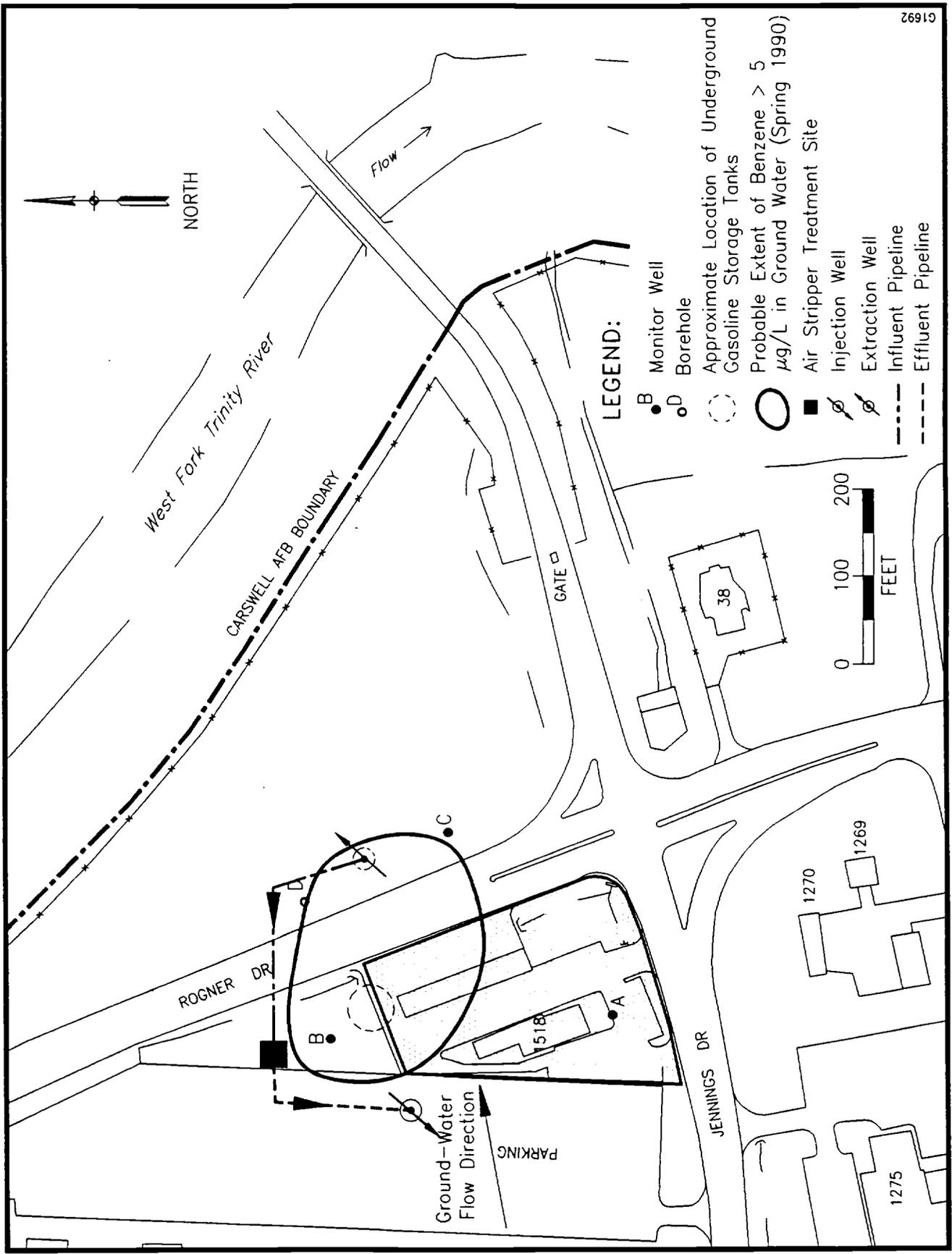


Figure 3-13. Basic Remedial Action Components of Alternative 4A, Site BSS, East Area, Carswell AFB, Texas

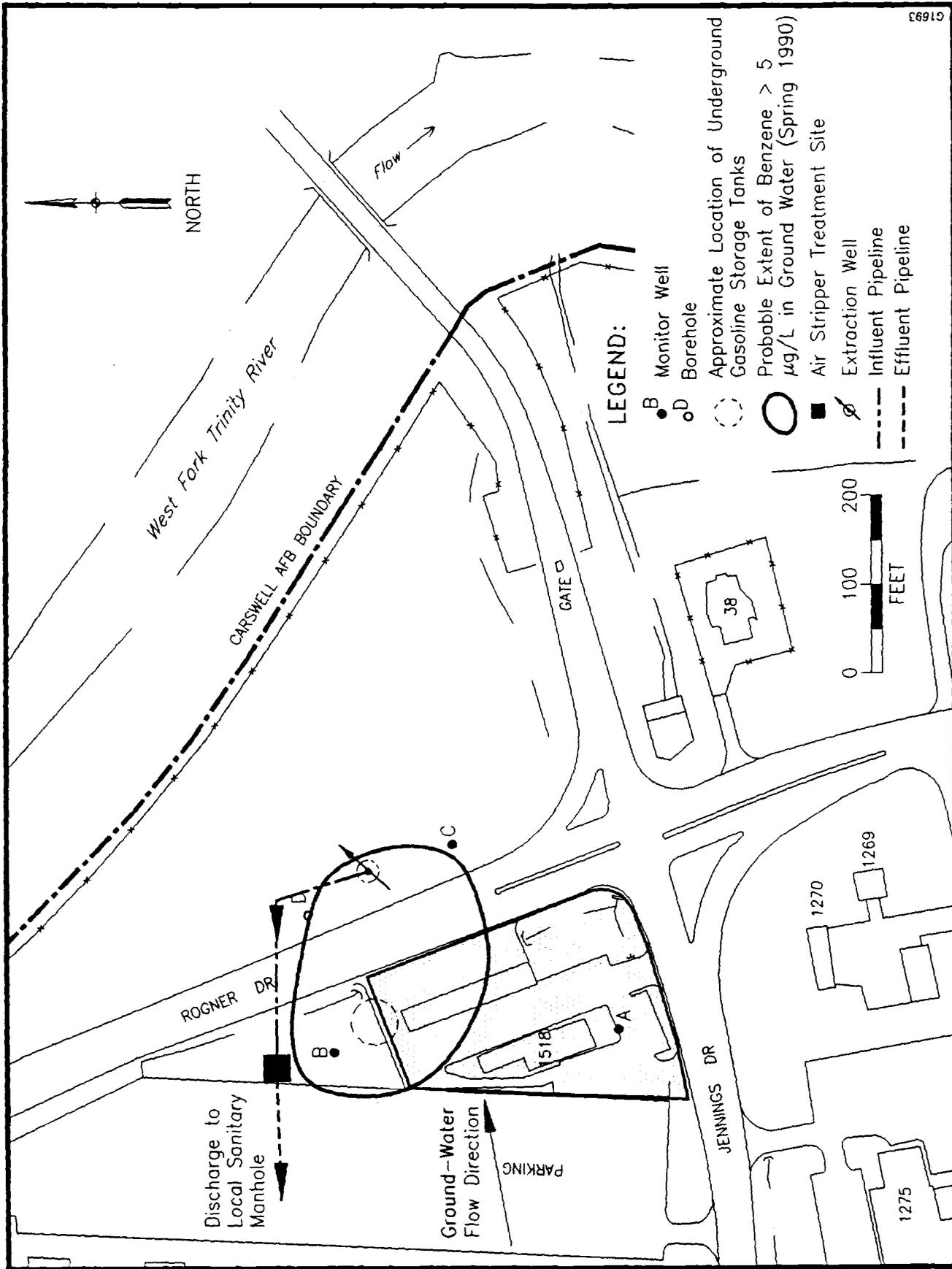


Figure 3-14. Basic Remedial Action Components of Alternative 4B, Site BSS, Carswell AFB, T

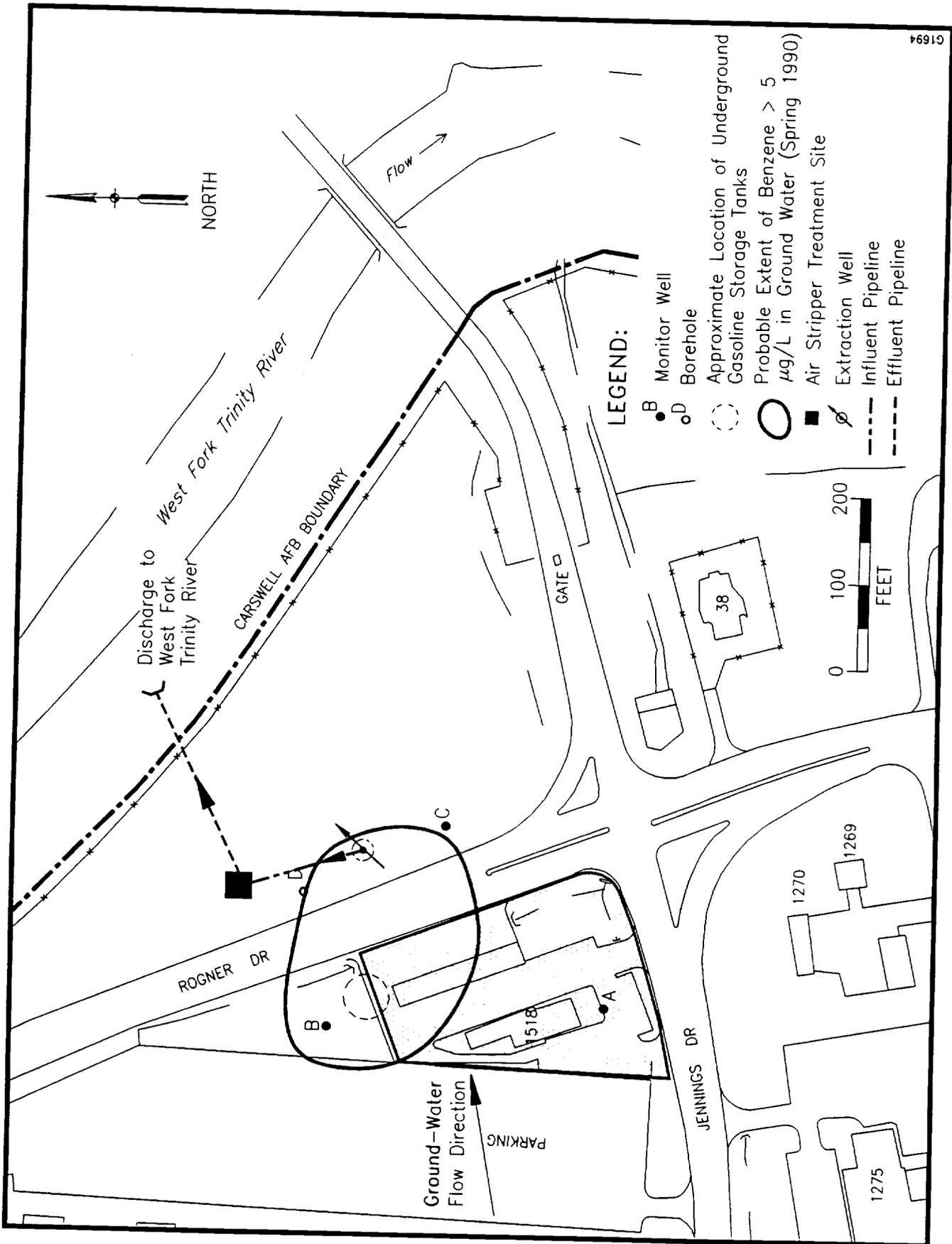
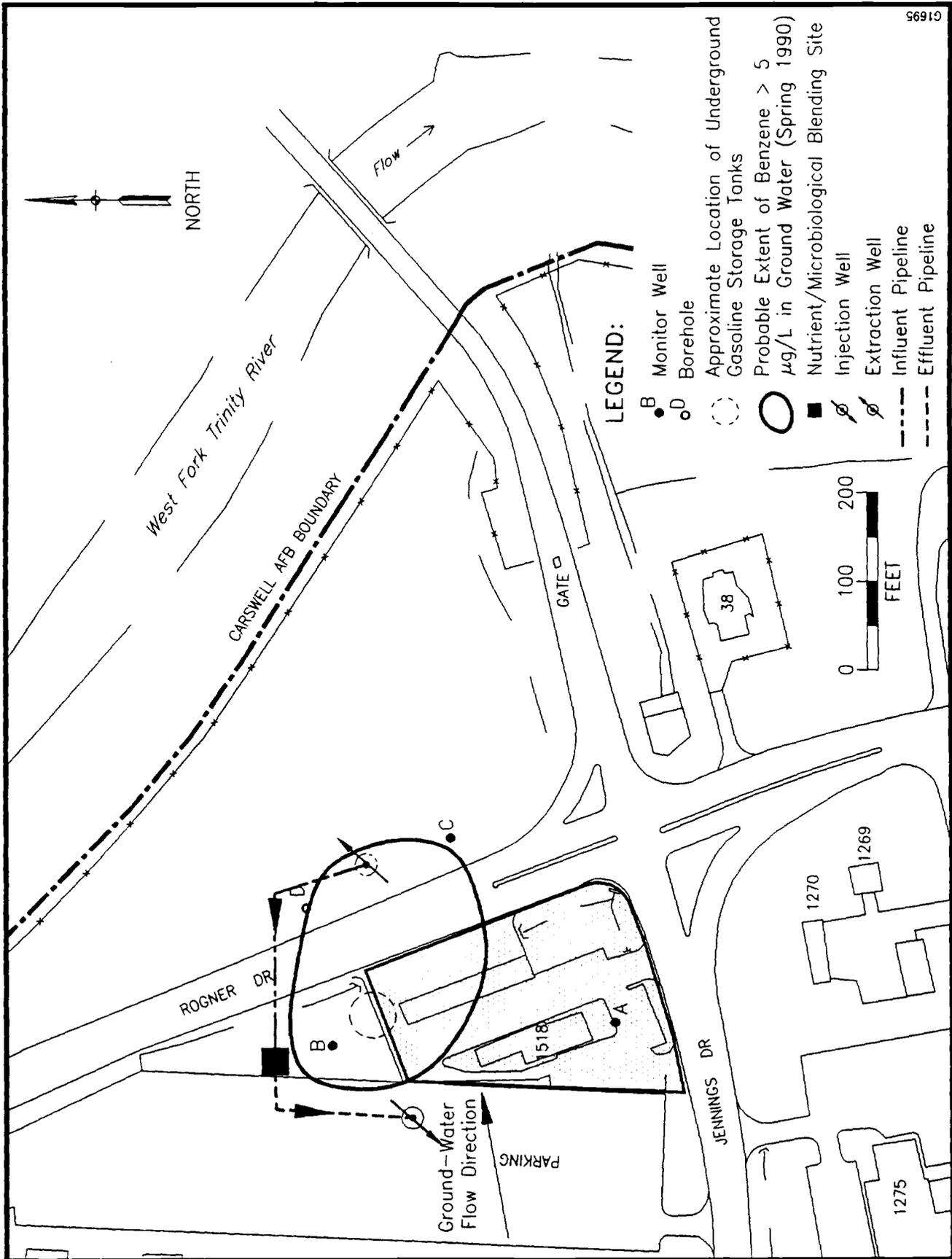


Figure 3-15. Basic Remedial Action Components of Alternative 4C, Site BSS, East Area, Carswell AFB, Texas



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Figure 3-16. Basic Remedial Action Components of Alternative 5, Site BSS, East Area, Carswell AFB, Texas

3.1.4.2 Preliminary Soil Alternatives

The same four remedial alternatives (including the no-action alternative) developed to address soil contamination potentially present at Site ST14 are applicable to Site BSS. They are listed in Table 3-4.

3.2 Screening of Preliminary Alternatives

The CERCLA guidance (EPA, 1988) describes a method of screening alternatives to reduce the number that will undergo a more thorough and extensive evaluation during the detailed analysis phase of the FS (see Section 4). The alternatives are evaluated against the short- and long-term aspects of three broad criteria: effectiveness, implementability, and cost. Effectiveness is a measure of the degree to which the remedial action protects human health and the environment. Specifically, it is a measure of how well the treatment reduces toxicity, mobility, and volume. Implementability is a measure of the relative ease of installation and operation and a measure of the time required to reach a given level of improvement. Federal, state, and local regulatory requirements relevant to the remedial action alternatives are also considered when evaluating the implementability of an alternative. The cost of each alternative is used for comparative purposes. During this phase, the cost of each alternative is compared on an order-of-magnitude basis. For example, an alternative will be eliminated only if its cost is at least one order of magnitude greater than that of the other options.

3.2.1 Site LF01--Landfill 1

The no-action alternative allows continued potential for leachate generation and migration of contaminants because buried wastes remain in place and no mechanisms for reduction of their toxicity, mobility, or volume are instituted. As stated in Section 3.1.1, the ground water at Site LF01 currently meets or exceeds the remedial action objectives. The no-action alternative does include long-term monitoring to detect any changes (degradation) in ground-water quality. The network of Upper Zone monitor

TABLE 3-4. PRELIMINARY SOIL REMEDIAL ALTERNATIVES^a
FOR SITE BSS--BASE SERVICE STATION

| Technology | Alternatives | | | | |
|-------------------------------|--------------|----|----|---|---|
| | 1 | 2A | 2B | 3 | 4 |
| Confirmation Sampling | • | • | • | • | • |
| Excavation | NA | | | • | |
| In-Situ Bio-Treatment | NA | | | | • |
| Soil Vapor Extraction | NA | • | • | | |
| Extraction Trenches | NA | • | | | |
| Extraction Wells | NA | | • | | |
| Soil Piles | NA | | | • | |
| On-Site Treated Soil Disposal | NA | | | • | |

NA - No Action

^a If required, pending results of additional soil sampling and analysis-- preliminary remedial alternatives do not include secondary treatment.

wells existing at the site is considered sufficient for long-term use, so implementation of Alternative 1 should not present any difficulties. The cost of the no-action alternative for Site LF01 would be minimal (essentially the cost for sampling, analysis, and monitor well maintenance).

3.2.2 Site SD13--Abandoned Gasoline Station and Unnamed Stream

The no-action alternative at Site SD13 allows continued potential for migration of contaminants and provides no mechanisms for reduction of their toxicity, mobility, or volume. As stated in Section 3.1.2, the ground water and surface water at Site SD13 currently meets the RAOs. The no-action alternative does include long-term monitoring to detect any changes (degradation) in ground-water or surface water quality. The network of Upper Zone monitor wells existing at the site is considered sufficient for long-term use, so implementation of this alternative should not present any difficulties. The cost of Alternative 1 for Site SD13 would be minimal (essentially the cost for sampling, analysis, and monitor well maintenance).

3.2.3 Site ST14--POL Tank Farm

Ground water and soil are discussed in Sections 3.2.3.1 and 3.2.3.2, respectively.

3.2.3.1 Preliminary Ground-Water Alternatives

Alternatives 1 through 5 and the results of their screening are discussed in this section.

Alternative 1--Because no remedial technologies (except for long-term ground-water monitoring) are implemented, this alternative allows continued potential for release and migration of contaminants in ground water, and degradation of the Upper Zone ground-water quality. The no-action alternative provides no mechanisms for reduction in toxicity, mobility, or volume of wastes or waste constituents in ground water through treatment. It fails to meet any of the RAOs, including MCLs. This alternative also provides

no reduction in toxicity, mobility, or volume of waste or waste constituents in Upper Zone ground water. The no-action alternative for Site ST14 should not present any implementation problems. The cost of Alternative 1 is negligible in comparison to the other alternatives.

Alternatives 2 and 3--Alternatives 2 and 3 include interceptor trenches to collect contaminated ground water and to act as a hydraulic barrier to further plume migration and oil/water separation for pretreatment. Alternatives 2A, 2B, and 2C utilize air stripping to treat contaminated ground water. Alternative 3 utilizes in-situ biological treatment to treat the contaminated ground water. Both alternatives should effectively mitigate the ground-water contamination at Site ST14, and should result in a reduction of the mobility and volume of contamination.

For Alternatives 2A, 2B, and 2C, the use of an air stripper to treat contaminated ground water transfers the contaminants to the air. As stated in Section 2, the mass of contaminants transferred on a daily basis is not expected to exceed TACB standards, but if they do, secondary treatment would be implemented to treat the contaminants. For Alternatives 2A and 2B, process upsets should not result in increased exposure to contaminants. For Alternative 2C, a process upset could result in a release of contaminated ground water to Farmers Branch (or another receiving water body). It is expected that any release would be discovered and corrected rapidly. Considering the dilution and volatilization expected to occur in the receiving stream, increased exposure to contaminants should be minimal.

For Alternative 3, the use of in-situ biological treatment should result in in-place destruction of contaminants. Therefore, the toxicity would be reduced or eliminated.

Installation of an interceptor trench at this site presents some implementability concerns. The Upper Zone Aquifer at Site ST14 has an average saturated thickness of approximately 8 feet. The depth to the base of the aquifer in the area of proposed ground-water extraction is about 18 feet below ground level. In addition, there are many buried pipelines and conduits in

this area. Therefore, it would be difficult to install an interceptor trench at this location.

Some additional difficulties may be involved in implementing Alternative 3. Regulatory acceptance of the in-situ biological treatment system would be necessary prior to implementation. Treatability studies may be required to demonstrate the effectiveness and timeliness of treatment, before the regulatory agencies would approve the alternative.

For Alternative 2C, additional implementability concerns could result from NPDES permitting requirements for discharge into Farmers Branch (or another receiving stream). Permitting could require six months to one year. The permit would have to be issued prior to implementation of the alternative. Public perception and acceptance could delay the permit longer or even result in denial of the permit.

Alternative 2B may also require a permit to discharge into the sanitary sewer. However, this permit would be issued under the POTW's sewer use ordinance. Preliminary conversations with the City of Fort Worth indicated that the expected volume and quality of the treated ground water from the air stripper should not present a problem to the treatment plant and should meet the sewer use ordinance requirements.

The cost of constructing the extraction/interceptor trenches will be greater than that of constructing an extraction well with the same capability. However, because other costs for Alternatives 2 and 3 should be in the same order of magnitude as Alternatives 4 and 5, the total costs should be comparable to Alternatives 4 and 5.

Alternative 4--Alternatives 4A, 4B, and 4C all include an extraction well for plume containment and ground-water extraction; oil/water separation for pretreatment; and air stripping as the primary treatment technology. All of these are proven technologies that can be implemented with minimal disruption of base activities. The effectiveness of Alternatives 4A,

4B, and 4C is identical to Alternatives 2A, 2B, and 2C, because, with the exception of the extraction method, the same technologies are used.

The use of an extraction well for Alternative 4 should be easily implemented at Site ST14. Unlike extraction trenches, the extraction well (and re-injection wells in Alternative 4A) can be placed to avoid existing structures and utilities. Other implementation concerns for Alternatives 4A, 4B, and 4C are identical to those described for Alternatives 2A, 2B, and 2C.

The costs for Alternative 4 are within the same order-of-magnitude range as the other alternatives, even though the extraction well should cost less to install than the extraction trenches in Alternative 2. Therefore, Alternative 4 poses no concerns relative to the cost criterion.

Alternative 5--Alternative 5 includes proven technologies for ground-water containment, extraction, and pretreatment that are all readily implementable considering site-specific conditions. While in-situ biological treatment has become more commonplace in recent years, it still has not gained the widespread acceptance of other, more-established treatment methods. The effectiveness of the alternative should be the same as that described for Alternative 3. The use of an extraction well for Alternative 5 eliminates the implementability concerns associated with extraction trenches used in Alternative 3. However, the other implementability concerns stated for Alternative 3 also apply to Alternative 5. The costs for Alternative 5 are in the same order-of-magnitude range as the other alternatives. Therefore, Alternative 5 poses no concerns related to the cost criterion.

Results of Ground-Water Alternatives Screening--Alternatives 2A, 2B, 2C, and 3 were eliminated from further consideration because they could be implemented only with great difficulty and large scale disruption of Base operations near Site ST14. Alternative 4C was eliminated from further consideration because of potential problems with public acceptance and permitting. While Alternative 5 may pose some regulatory acceptance problems, it was retained for further evaluation to provide a basis for comparison to the air stripping alternative.

3.2.3.2 Preliminary Soil Alternatives

Available soils analytical data are insufficient to support screening of preliminary soil remedial alternatives. To apply the screening criteria of effectiveness, implementability, and cost, the volumes, locations and extent, depth, and concentrations of hydrocarbon contaminants in soil, if any, must be documented. On a qualitative basis, Alternative 3, which includes excavation of contaminated soils, is probably more difficult to implement than the other alternatives (because of potential interference with surface and subsurface structures), unless contaminated soils are restricted to shallow depths and are volumetrically small. The cost to implement Alternative 1 (no action) is negligible compared to the other three, which are expected to be in the same order-of-magnitude range. As in the case of ground-water alternatives, the no-action alternative is ineffective, providing no reduction in the toxicity, mobility, or volume of contaminants. Alternatives 2, 3, and 4 consist of technologies that are proven to be effective for the contaminants of concern.

3.2.4 Site BSS--Base Service Station

Ground water and soil are discussed in Sections 3.2.4.1 and 3.2.4.2, respectively.

3.2.4.1 Preliminary Ground-Water Alternatives

Alternatives 1 through 5 and the results of their screening are discussed in this section.

Alternative 1--Because no remedial technologies (except for long-term ground-water monitoring) are implemented, this alternative allows continued potential for release and migration of contaminants in ground water, and degradation of the Upper Zone ground-water quality. The no-action alternative provides no mechanisms for reduction in toxicity, mobility, or volume of wastes or waste constituents in ground water through treatment. It fails to meet any of the RAOs, including MCLs. This alternative also provides

no reduction in toxicity, mobility, or volume of waste or waste constituents in Upper Zone ground water. The no-action alternative for Site BSS should not present any implementation problems. The cost of Alternative 1 is negligible in comparison to the other alternatives.

Alternatives 2 and 3--Alternatives 2 and 3 include interceptor trenches to collect contaminated ground water and to act as a hydraulic barrier to further plume migration. Alternatives 2A, 2B, and 2C utilize air stripping to treat contaminated ground water. Alternative 3 utilizes in-situ biological treatment to treat the contaminated ground water. Both alternatives should effectively mitigate the ground-water contamination at Site BSS, and should result in a reduction of the mobility and volume of contamination.

For Alternatives 2A, 2B, and 2C, the use of an air stripper to treat contaminated ground water transfers the contaminants to the air. As stated in Section 2, the mass of contaminants transferred on a daily basis is not expected to exceed TACB standards, but if they do, secondary treatment would be implemented to treat the contaminants. For Alternatives 2A and 2B, process upsets should not result in increased exposure to contaminants. For Alternative 2C, a process upset could result in a release of contaminated ground water to the West Fork of the Trinity River (or another receiving water body). It is expected that any release would be discovered and corrected quickly. Considering the dilution and volatilization expected to occur in the receiving stream, any increased exposure to contaminants should be minimal.

For Alternative 3, the use of in-situ biological treatment should result in in-place destruction of contaminants. Therefore, the toxicity of the contaminant plume would be reduced or eliminated.

Installation of the interceptor trench for Alternatives 2 and 3 to collect contaminated ground water and to act as a hydraulic barrier to further plume migration should be easily implemented. Very few structures or utilities are located at or around Site BSS. Due to the generally thin (approximately 2 feet) saturated thickness, and shallow depth to the base of

the Upper Zone (generally 10 feet or less), interceptor trenches would be very effective. Other implementation issues for Alternatives 2 and 3 are described in the following paragraphs.

Regulatory acceptance of the in-situ biological treatment system used in Alternative 3 would be necessary prior to implementation. Treatability studies may be required to demonstrate the effectiveness and timeliness of treatment, before the regulatory agencies would approve the alternative.

For Alternative 2C, additional implementability concerns could result from NPDES permitting requirements for discharge into the West Fork of the Trinity River (or another receiving stream). Permitting could require six months to one year. The permit would have to be issued prior to implementation of the alternative. Public perception and acceptance could delay the permit longer or even result in denial of the permit.

Alternative 2B may also require a permit to discharge into the sanitary sewer. However, this permit would be issued under the POTW's sewer use ordinance. Preliminary conversations with City of Fort Worth personnel have indicated that the expected volume and quality of the treated ground water from the air stripper should not present a problem to the treatment plant and should meet the sewer use ordinance requirements.

The cost criterion does not pose a problem for Alternatives 2 or 3. The cost of constructing the extraction/interceptor trenches will be greater than that of constructing an extraction well with the same capability. However, because other costs for Alternatives 2 and 3 should be in the same order of magnitude as Alternatives 4 and 5, the total costs should be comparable to Alternatives 4 and 5.

Alternatives 4 and 5--Alternatives 4 and 5 include an extraction well for plume containment and ground-water withdrawal, with either air stripping (Alternatives 4A, 4B, and 4C) or in-situ biological treatment (Alternative 5) as the primary treatment option. All of the component

technologies are implementable and are in an acceptable range of costs. However, sustained withdrawal of contaminated ground water at even a low pumping rate may not be feasible due to the small volume and variable occurrence of Upper Zone ground water at this site. Therefore, Alternatives 4 and 5 may not be effective because extraction wells are not suited to the site-specific hydrogeologic conditions at Site BSS. Other effectiveness and implementability issues for Alternatives 4 and 5 are similar to those discussed for Alternatives 2 and 3. The costs for Alternatives 4 and 5 are in the same order of magnitude as Alternatives 2 and 3, so the cost criterion does not present a problem.

Results of Ground-Water Alternative Screening--Alternatives 4A, 4B, 4C, and 5 were eliminated from further evaluation because they are incompatible with the site-specific hydrogeologic conditions and, therefore, do not meet the effectiveness criterion. Alternative 2C was eliminated from further consideration because of potential problems with public acceptance and permitting. While Alternative 3 may pose some regulatory acceptance problems, it was retained for further evaluation to provide a basis for comparison to the air stripping alternative.

3.2.4.2 Preliminary Soil Alternatives

Available soils analytical data for Site BSS are also insufficient to support screening of preliminary soil remedial alternatives. To apply the screening criteria of effectiveness, implementability, and cost, the volumes, locations and extent, depth, and concentrations of hydrocarbon contaminants in soil, if any, must be documented. On a qualitative basis, Alternatives 2 and 3, which include excavation, are probably more difficult to implement than Alternative 4 (because of potential disruption of service station operations during excavation for soil removal or vapor extraction trench construction), unless contaminated soils are restricted to shallow depths and are volumetrically small. The cost to implement Alternative 1 (no action) is negligible compared to the other three, which are expected to be in the same order-of-magnitude range. As in the case of ground-water alternatives, the no-action alternative is ineffective, providing no reduction in the toxicity,

mobility, or volume of contaminants. Alternatives 2, 3, and 4 consist of technologies that are proven to be effective for the contaminants of concern.

3.3 Summary of Preliminary Alternative Development and Screening

For Sites LF01 (Landfill 1) and SD13 (Unnamed Stream and Abandoned Gasoline Service Station), only the no-action alternative was retained for detailed evaluation.

For Site ST14 (POL Tank Farm), the no-action alternative (Alternative 1), two air stripping alternatives (Alternatives 4A and 4B), and one in-situ biological treatment alternative (Alternative 5) were retained for detailed evaluation.

For Site BSS (Base Service Station), the no-action alternative (Alternative 1), two air stripping alternatives (Alternatives 2A and 2B) and one in-situ biological treatment alternative (Alternative 3) were retained for detailed evaluation.

As previously explained, preliminary soil remedial alternatives cannot undergo detailed analysis until additional data become available.

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tunities for coordination of remedial activities at multiple sites, and Section 4.7 summarizes the comparative analysis of alternatives based on cost-effectiveness.

4.1 Description of Evaluation Criteria and Analysis Method

Descriptions of the evaluation criteria are provided below.

The evaluation of each alternative with respect to the overall protection of human health and the environment focuses on how each alternative can reduce the risk from potential exposure pathways by implementing treatment, engineering, or institutional controls. This criterion is also used to assess whether the alternatives pose any unacceptable short-term or cross-media effects.

The ability of each alternative to comply with all ARARs (as defined by the RAOs), or the need to justify a waiver if some ARARs cannot be achieved, is evaluated for each alternative using this criterion.

The long-term effectiveness and permanence of each alternative is evaluated with respect to the magnitude of the residual risk, and to the adequacy and reliability of the controls used to manage the remaining untreated ground water and treatment residuals over the long term. Alternatives that afford the highest degree of long-term effectiveness and permanence are those that leave little or no contamination remaining at the site, so long-term maintenance and monitoring are unnecessary. Thus, reliance on institutional controls is minimized.

The discussion of how reduction of contaminant toxicity, mobility, or volume would be achieved focuses on the anticipated performance of the treatment technologies used in each alternative. This evaluation relates to the statutory preference for selecting a remedial action that can reduce the toxicity, mobility, or volume of hazardous substances. Other important treatment characteristics are the irreversibility of the treatment process,

the type and quantity of residuals resulting from any treatment process, and the amount of waste treated or destroyed.

The evaluation of the short-term effectiveness of each alternative focuses on the protection of military personnel, workers, and the community during the remedial action, the environmental impacts of implementing the action, and the time required to reach cleanup goals.

The analysis of the implementability of each alternative emphasizes the technical and administrative feasibility of implementing the alternatives as well as the availability of necessary goods and services. Implementability includes such characteristics as: the ability to obtain services, equipment, and specialists; the ability to monitor the performance and the effectiveness of the technologies; and the ability to obtain necessary approval from other agencies.

The cost estimates presented in this report are order-of-magnitude level estimates meant to be used for comparative purposes only. These cost estimates are based on a variety of information: quotes from suppliers in the area of the site, generic unit costs, vendor information, conventional cost estimating guides, design manuals, and experience. The feasibility study-level cost estimates shown have been prepared to help guide the evaluation and implementation of the project. The actual costs of the project will depend on the true labor and material costs, actual site conditions, competitive market conditions, final project scope, the implementation schedule, and other variables. A significant uncertainty that will affect the cost is the actual volume of contaminated ground water. Such uncertainties, however, would affect the costs of all the alternatives.

Capital costs are all costs (other than O&M costs) that are required to implement the remedial action. Both direct and indirect costs are considered in the development of capital cost estimates. Direct costs are construction costs for the equipment, labor, and materials needed to implement a remedial action. Indirect costs are those associated with engineering,

permitting (as required), construction management, and other services necessary to carry out the remedial action.

Annual operating and maintenance (O&M) costs, which include operating labor, maintenance materials and labor, energy, and purchased services, have also been estimated. The estimates include those O&M costs that may be incurred even after the initial remedial activity is complete. Determination of the present worth costs is based on a 30-year period of performance and a five-percent discount rate.

4.2 Detailed Evaluation of the No-Action Alternative for Site LF01

The following subsections describe the alternative and discuss each of the CERCLA evaluation criteria.

4.2.1 Description of the Alternative

Except for long-term monitoring, no remedial activities would be implemented at Site LF01 with the no-action alternative. Long-term monitoring of Site LF01 will involve sampling the five existing monitor wells at the site. No new monitor wells are required for Site LF01. Since there are no records of the nature of wastes formerly disposed of in Landfill 1, samples should be analyzed for aromatic and chlorinated volatile organics and dissolved metals on a quarterly basis; and semivolatile organics, pesticides, herbicides, and PCBs on an annual basis. Evidence of increased migration, such as significantly or consistently higher contaminant concentrations, or significant changes in the occurrence of the contaminants, would justify the initiation of further evaluation.

4.2.2 Protection of Human Health and the Environment

The no-action alternative does not reduce the risk to human health or the environment resulting from contamination at Site LF01. Recent data indicate that ground water at the site is in compliance with the remedial action objective criteria, and that the risk presented by site contamination

is insignificant (10^{-10}). Ground-water flow at Site LF01 is currently towards the West Fork of the Trinity River. If the detected contaminants reach the river, the concentrations will be further reduced by the effects of dilution and volatilization. Therefore, the risk to human health or the environment would be the same or lower than that determined in the baseline risk assessment.

4.2.3 Compliance with ARARs

While the no-action alternative provides no mechanisms for ground-water cleanup, ground-water contaminant concentrations determined in 1990 were lower than the applicable RAOs (i.e., MCLs and 70-year cancer risk criterion).

4.2.4 Long-Term Effectiveness and Permanence

Because no remedial activity is implemented for the no-action alternative, the residual risk remains the same as the baseline risk. Natural attenuation should result in some long-term reduction in risks. Contamination is left on site and long-term monitoring and other institutional controls may be necessary in perpetuity.

4.2.5 Reduction in Toxicity, Mobility, or Volume

No reduction in the toxicity, mobility, or volume of contamination occurs from implementation of the no-action alternative. It neither inhibits nor prevents continued leachate generation and migration of contaminants, nor does it prevent further degradation of Upper Zone ground-water quality. However, the 1990 data suggest that the waste mass has either degenerated or stabilized so that leachate production and contaminant migration are minimal. The detected contaminant concentrations are near detection levels, and are less than MCLs. Long-term monitoring of the ground water at Site LF01 will allow initiation of remedial actions if significant changes in contaminant concentrations are detected.

4.2.6 Short-Term Effectiveness

The baseline risk assessment for Site LF01 indicates that the risks to human health and the environment are insignificant. Implementation of the no-action alternative will not increase these risks. Numerical remedial action objectives are satisfied at this time. However, cleanup of residual contaminants to background levels will occur only by natural attenuation.

4.2.7 Implementability

Implementation of the no-action alternative should present no problems.

4.2.8 Cost

The present worth cost estimate for the no-action alternative for Site LF01 is approximately \$384,300. Capital costs for the no-action alternative are negligible, because no action is required. The annual O&M cost estimate is approximately \$25,000.

4.3 Detailed Evaluation of the No-Action Alternative for Site SD13

The following subsections describe the alternative and discuss each of the CERCLA evaluation criteria.

4.3.1 Description of the Alternative

Except for long-term monitoring, no remedial activities would be implemented at Site SD13 with the no-action alternative. Long-term monitoring of Site SD13 will involve sampling the four existing monitor wells and established surface water sampling points on Unnamed Stream. No new monitor wells or surface water sampling points are considered necessary to adequately monitor Site SD13. Based on the ground-water and surface water constituents detected historically, existing monitor wells and established surface water sampling points on Unnamed Stream should be sampled and analyzed quarterly for

volatile aromatic compounds and dissolved metals. Evidence of increased migration, such as significantly or consistently higher contaminant concentrations, or significant changes in the occurrence of the contaminants, would justify the initiation of further evaluation.

4.3.2 Protection of Human Health and the Environment

The no-action alternative does not reduce the risk to human health or the environment resulting from contamination at Site SD13. Recent data indicate that ground water at the site is in compliance with the RAOs, and that the risk presented by site contamination is insignificant (10^{-8}). Ground-water flow at Site SD13 is currently toward Unnamed Stream and the West Fork of the Trinity River. Even if the detected contaminants reach the stream or the river, the concentrations will be further reduced by the effects of dilution and volatilization. Therefore, the risk to human health or the environment would be the same or lower than that determined in the baseline risk assessment.

4.3.3 Compliance with ARARs

While the no-action alternative provides no mechanisms for ground-water cleanup, ground-water contaminant concentrations determined in 1990 were lower than the applicable RAOs (i.e., MCLs and 70-year cancer risk criterion).

4.3.4 Long-Term Effectiveness and Permanence

Because no remedial activity is implemented for the no-action alternative, the residual risk remains the same as the baseline risk. Natural attenuation should result in some long-term reduction in risks. Contamination is left on site and long-term monitoring and other institutional controls may be necessary in perpetuity.

4.3.5 Reduction in Toxicity, Mobility, or Volume

No reduction in the toxicity, mobility, or volume of contamination occurs from implementation of the no-action alternative. It neither inhibits nor prevents continued migration of contaminants, nor does it prevent further degradation of Upper Zone ground-water or surface water quality. The contaminant concentrations detected in 1990 are near detection levels and are less than MCLs. Long-term monitoring of the ground water and surface water at Site SD13 will allow initiation of remedial actions if significant changes in contaminant concentrations are detected.

4.3.6 Short-Term Effectiveness

The baseline risk assessment for Site SD13 indicates that the risks to human health and the environment are insignificant. Implementation of the no-action alternative will not increase these risks. Numerical remedial action objectives are satisfied at this time. However, cleanup of detected contaminants to background levels will occur only by natural attenuation.

4.3.7 Implementability

Implementation of the no-action alternative for Site SD13 should present no problems.

4.3.8 Cost

The present worth cost estimate for the no-action alternative for Site SD13 is approximately \$387,400. Capital costs for the no-action alternative are negligible, because no action is required. The annual O&M cost estimate is approximately \$25,200.

4.4 Detailed Evaluation of Alternatives for Site ST14

Alternatives 1, 4A, 4B, and 5 are evaluated in the following subsections.

4.4.1 Alternative 1--No Action

The following subsections describe the alternative and discuss each of the CERCLA evaluation criteria.

4.4.1.1 Description of the Alternative

Except for long-term monitoring, no remedial activities would be implemented at Site ST14 with the no-action alternative. Long-term monitoring at Site ST14 will make use of the existing Upper Zone monitoring well network and additional wells. The existing monitoring well network consists of nine wells. It is anticipated that all existing wells, and up to five additional wells installed beyond the downgradient limits of the existing contaminant plumes and the location of the ground-water extraction system, will be required to monitor the effectiveness of the selected ground-water remedial alternative. These wells will be sampled and analyzed for volatile aromatic compounds, total petroleum hydrocarbons, and dissolved metals on a quarterly basis for the duration of site remediation. Evidence of increased migration, such as significantly or consistently higher contaminant concentrations, or significant changes in the occurrence of the contaminants, would justify the initiation of further evaluation.

4.4.1.2 Protection of Human Health and the Environment

The no-action alternative does not reduce the risk to human health or the environment resulting from contamination at Site ST14. Ground-water contamination currently exceeds the requirements for satisfying the remedial action objectives. The baseline risk assessment for the site determined that the noncarcinogenic health effects originating from the site were insignificant compared to the standards set by EPA. Carcinogenic health effects associated with the site were approximately 10^{-8} based on inhalation exposure. The risk assessment concluded that the ingestion and dermal exposure pathways were insignificant. Ground-water flow at Site ST14 is currently toward Unnamed Stream and the West Fork of the Trinity River. If contaminants reach the stream or the river, the concentrations will be further reduced by the

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effects of dilution and volatilization. Therefore, the risk to human health or the environment would be the same or lower than that determined in the baseline risk assessment.

4.4.1.3 Compliance with ARARs

The no-action alternative does not meet the RAOs established for the site. Immiscible hydrocarbon contamination observed at the site in 1990 has the potential to migrate and contaminate previously uncontaminated areas. Some contaminant concentrations in the ground water at Site ST14 were in excess of MCLs in 1990.

4.4.1.4 Long-Term Effectiveness and Permanence

Because no remedial activity is implemented for the no-action alternative, the residual risk remains the same as the baseline risk. Natural attenuation could result in some long-term reduction in risks. However, natural attenuation with the waste mass in place would occur over a long period of time, so long-term reduction in risk due to natural attenuation should be insignificant. Long-term monitoring will identify changes in contaminant concentrations and the extent of the contaminant plume. Further remedial action may become necessary if these changes appear to present additional risks or hazards not apparent at this time. Because contamination is left on site, long-term monitoring and other institutional controls may be necessary in perpetuity.

4.4.1.5 Reduction in Toxicity, Mobility, or Volume

No reduction in the toxicity, mobility, or volume of contamination occurs from implementation of the no-action alternative. It neither inhibits nor prevents continued migration of contaminants, nor does it prevent further degradation of Upper Zone ground-water quality. Long-term monitoring of the ground water at Site ST14 will allow initiation of remedial actions if significant changes in contaminant concentrations or extent are detected.

4.4.1.6 Short-Term Effectiveness

The baseline risk assessment for Site ST14 indicates that the risks to human health and the environment are insignificant. Implementation of the no-action alternative will not increase these risks. Remediation of the contaminant plume to meet the criteria used to measure successful achievement of remedial action objectives can occur only by natural attenuation and only after a long period of time.

4.4.1.7 Implementability

Implementation of the no-action alternative for Site ST14 involves the design and execution of a long-term monitoring program and the installation of five monitor wells, neither of which activities should present problems. The primary obstacle to implementation of the no-action alternative will be securing approval from regulatory agencies and gaining public acceptance. The alternative calls for leaving a potentially significant volume of untreated free-phase hydrocarbon, as well as a large volume of contaminated ground-water, untreated and uncontained. Regulatory acceptance will be difficult unless other options are technically infeasible for Site ST14.

4.4.1.8 Cost

The present worth cost estimate for the no-action alternative for Site ST14 is approximately \$844,200. Estimated capital costs for the no-action alternative include the costs of installing five additional ground-water monitor wells and are approximately \$26,400. The annual O&M cost estimate is approximately \$53,200.

4.4.2 Alternative 4A--Air Stripping and Re-injection

The following subsections describe the alternative and discuss each of the CERCLA evaluation criteria.

4.4.2.1 Description of the Alternative

The components of Alternative 4A are illustrated in Figure 4-1.

They consist of:

- Long-term ground-water monitoring as described in Alternative 1, Section 4.4.1.1;
- One ground-water extraction well tentatively located near the southwest corner of Building 1213;
- An oil/water separator located at the air stripping treatment site near the northwest corner of Building 1213;
- An air stripping tower and required ancillary equipment located at the air stripping treatment site near the northwest corner of Building 1213;
- Approximately 250 feet of 2-inch/4-inch dual-wall containment pipe for conveyance of contaminated ground water;
- Approximately 670 feet of 2-inch, Schedule 80 PVC pipe for conveyance of treated ground water; and
- Two ground-water injection wells located within the limits of Site ST14 as shown on Figure 4-1.

The treated effluent will be re-injected into the Upper Zone upgradient of the two contaminant plumes present at Site ST14.

4.4.2.2 Protection of Human Health and the Environment

Alternative 4A should reduce the risk to human health and the environment resulting from ground-water contamination at Site ST14. This

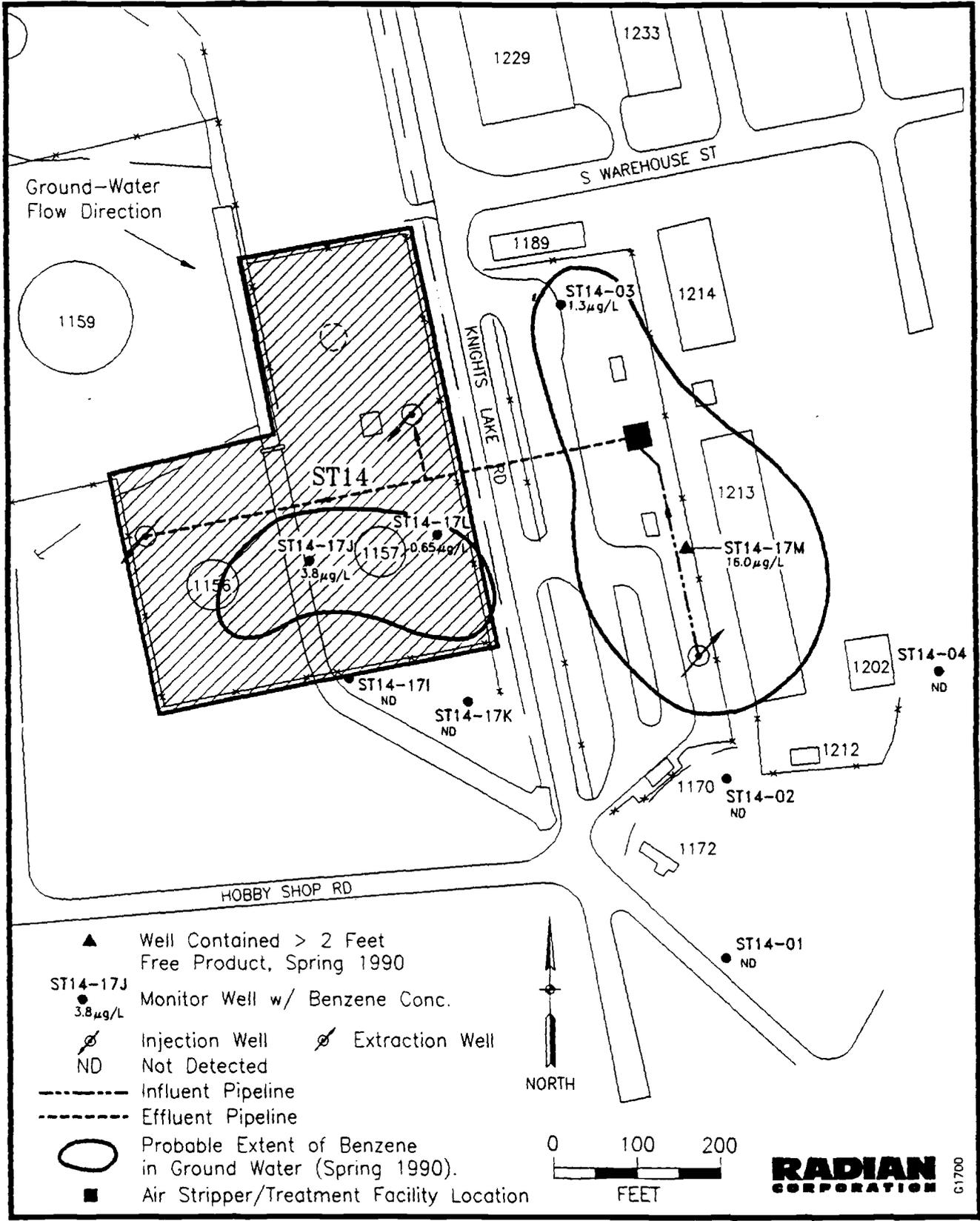


Figure 4-1. Remedial Alternative 4A, Site ST14, East Area, Carswell AFB, Texas

alternative will extract contaminated ground water and immiscible hydrocarbon from the Upper Zone. The immiscible hydrocarbon will be removed in the oil/water separator and either recycled or destroyed off site. The air stripper will remove soluble hydrocarbons and other volatile organic compounds from the ground water prior to re-injecting it into the aquifer. Re-injection should result in increased flushing of the Upper Zone and thus potentially decreased remediation time. Migration of contaminated ground water to other portions of the Upper Zone, as well as to nearby Unnamed Stream or Farmers Branch, should be minimized and possibly prevented by Alternative 4A. The only potential risk of exposure to site contaminants could be from the contaminant-laden air stripper off-gas. The mass of contaminants released from the air stripper will be limited to 5 lb/day. If the emissions rate exceeds that, secondary treatment, such as fume incineration or activated carbon adsorption, will be implemented. Therefore, the risk of exposure to contaminants from the air stripper should be minimal.

4.4.2.3 Compliance with ARARs

Alternative 4A should achieve all remedial action objectives established for the site. The immiscible hydrocarbons will be removed and disposed of off site. Contaminant concentrations in site ground water will be reduced below MCLs. Therefore, further contamination of ground water and contaminant migration to other portions of the Upper Zone or to other media should be minimized. Measures to prevent and contain spills originating from pipelines conveying contaminated ground water, treatment equipment, and by-product storage will all be incorporated into the design and implementation of the alternative.

4.4.2.4 Long-Term Effectiveness and Permanence

Once Alternative 4A has been implemented, residual risks from contamination at Site ST14 should be less than the baseline risk. The majority of contaminants in the ground water will be removed, and the remaining concentrations of contaminants (less than MCLs, as required) will be further reduced by natural attenuation. Unless a previously unidentified

contaminant source exists, the residual risks should be acceptable and the remedy should be considered permanent. The alternative relies on ground water to flush contaminants from Upper Zone materials. Therefore, insoluble compounds which may be strongly adsorbed onto soils will not be removed. Long-term monitoring of the ground water after remediation will identify changes in contaminant concentrations and will identify significant changes in contaminant distribution which might indicate new contaminant sources or leaching of remnant contamination. Additional remedial measures could be determined and evaluated at that time.

4.4.2.5 Reduction in Toxicity, Mobility, or Volume

By hydraulically containing and removing contamination from the Upper Zone at Site ST14, Alternative 4A should reduce the mobility and volume of contamination. The oil/water separator and the air stripper should remove contaminants from the ground water, but they will not reduce the toxicity of the contaminants. Immiscible hydrocarbon from the oil/water separator will be recycled or destroyed, thus reducing the toxicity for that portion of the contaminants. Soluble contaminants in the ground water should be transferred out of solution into the air phase in the air stripper. Airborne contaminants would be significantly diluted or, if necessary, will be treated using fume incineration or activated carbon adsorption. Therefore, toxicity is effectively reduced.

4.4.2.6 Short-Term Effectiveness

The baseline risk assessment for Site ST14 indicates that the risks to human health and the environment are insignificant. Remedial activities conducted for Alternative 4A should not result in any increase in risk to on- or off-base personnel. Drill cuttings may temporarily introduce the risk of exposure for on-site personnel and for contaminant migration. However, if drill cuttings are handled, stored, and disposed of correctly, the temporary increase in risk should be insignificant. RAOs should be achieved within 1 to 5 years after implementation of the alternative.

4.4.2.7 Implementability

Alternative 4A makes use of proven, reliable technologies for remediation of Site ST14, and no outstanding impediments to implementation should occur. Some minor disruptions of base traffic may occur while the effluent line is constructed under Knights Lake Road. However, these disruptions should be minimized if boring and jacking rather than open cut techniques are used to construct the crossing. No permitting or regulatory approval problems are anticipated for Alternative 4A.

4.4.2.8 Cost

The present worth cost estimate for Alternative 4A for Site ST14 is approximately \$1,307,000. The estimated capital cost for Alternative 4A is approximately \$510,600. The annual O&M cost estimate is approximately \$94,300.

4.4.3 Alternative 4B--Air Stripping and Discharge to the Sanitary Sewer

The following subsections describe the alternative and discuss each of the CERCLA evaluation criteria.

4.4.3.1 Description of the Alternative

Alternative 4B (see Figure 4-2) includes most of the components of Alternative 4A. However, rather than re-injecting the treated ground water, it will be discharged to a nearby sanitary sewer. The differences between Alternative 4A and 4B are as follows:

- No ground-water injection wells will be used in Alternative 4B;
- A new "drop" manhole will be constructed on a nearby 8-inch sanitary sewer line; and

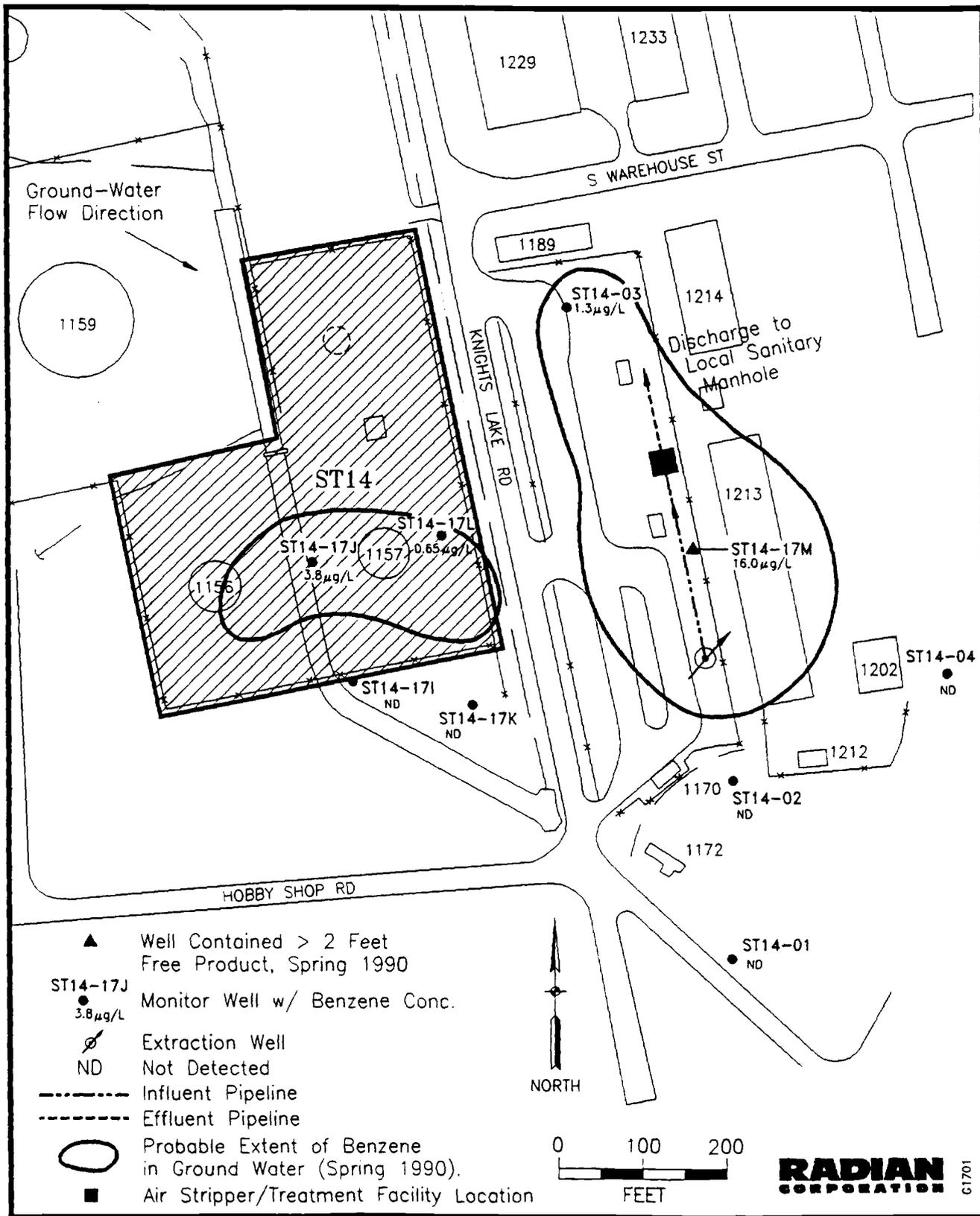


Figure 4-2. Alternative 4B, Site ST14, East Area, Carswell AFB, Texas

- Approximately 250 feet of 4-inch, Schedule 80 PVC pipe will be used for conveying treated effluent to the sanitary manhole (in lieu of the 670 feet of 2-inch PVC pipe used in Alternative 4A).

The remaining components will be the same as those for Alternative 4A.

4.4.3.2 Protection of Human Health and the Environment

The evaluation of Alternative 4B for this criterion is the same as for Alternative 4A, with the following additional concerns, caused by the fact that in Alternative 4B, treated ground water would be discharged to a nearby sanitary sewer. During a process upset, contaminated ground water could be discharged to the sanitary sewer and some volatilization of contaminants could occur. With dilution in the ambient air, the risk of exposure to contaminants should be minimal. Also under an upset condition, contaminated ground water could leak from the sanitary sewer and contaminate other water-bearing and non-water-bearing zones. Again, the dilution and volatilization factor in the sewer should be sufficient to minimize any additional risk.

4.4.3.3 Compliance with ARARs

The evaluation of Alternative 4B for this criterion should be the same as that for Alternative 4A. However, Alternative 4B must also meet the pretreatment requirements of the City of Fort Worth's sanitary sewer use ordinance. Preliminary conversations with City of Fort Worth personnel indicate that the air stripping process provides adequate removal of volatile organic contaminants to achieve the limits established by the City.

4.4.3.4 Long-Term Effectiveness and Permanence

The evaluation of Alternative 4B for this criterion should be the same as that for Alternative 4A, with the following exception: if at any time the City of Fort Worth changes its sewer use ordinance or limits the incoming flow to the POTW, an alternate disposal method for the treated effluent may be

required. Presumably, adequate notice would be given to allow evaluation of other discharge options and to prevent disruption of operations.

4.4.3.5 Reduction in Toxicity, Mobility, or Volume

The evaluation of Alternative 4B for this criterion should be the same as that for Alternative 4A. However, during upset conditions the potential exists for contaminant discharge to the sanitary sewer. Such discharges could result in the migration of contaminants through leaking sewer pipes and in the exposure of City workers to volatilized contaminants.

4.4.3.6 Short-Term Effectiveness

The evaluation of Alternative 4B for this criterion is the same as that for Alternative 4A.

4.4.3.7 Implementability

The evaluation of Alternative 4B for this criterion should be the same as that for Alternative 4A, with the following exception: implementation of Alternative 4B may require a permit to discharge into the sanitary sewer. This permit would be issued under the POTW's sewer use ordinance. Preliminary conversations with City of Fort Worth personnel have indicated that the volume and quality of the treated ground water from the air stripper should not present a problem to the treatment plant and should meet the sewer use ordinance requirements.

4.4.3.8 Cost

The present worth cost estimate for Alternative 4B for Site ST14 is approximately \$1,880,600. The estimated capital cost for Alternative 4B is approximately \$469,000. The annual O&M cost estimate is approximately \$91,900.

4.4.4 Alternative 5--In-Situ Biological Treatment

The following subsections describe the alternative and discuss each of the CERCLA evaluation criteria.

4.4.4.1 Description of the Alternative

Alternative 5 (see Figure 4-3) uses many of the components of Alternative 4A. However, Alternative 5 involves the use of in-situ biological degradation rather than air stripping to treat the contaminated ground water. Changes in components between Alternatives 4A and 5 are as follows:

- A nutrient and microorganism blending facility will be substituted for the air stripping tower; and
- 670 feet of 2-inch/4-inch dual-wall containment pipe will be used (in lieu of the 670 feet of 2-inch, Schedule 80 PVC pipe used in Alternative 4A).

In Alternative 5, treatment of contaminated ground water will occur in the Upper Zone. Therefore, the piping from the blending facility to the injection wells will be conveying contaminated ground water. Dual containment piping is necessary to minimize contaminant migration resulting from pipe breaks or leaks.

4.4.4.2 Protection of Human Health and the Environment

Alternative 5A should reduce the risk to human health and the environment resulting from ground-water contamination at Site ST14. This alternative will extract contaminated ground water and immiscible hydrocarbon from the Upper Zone. The immiscible hydrocarbon will be removed in the oil/water separator and either recycled or destroyed off site. The remaining ground water contaminated with dissolved organic contaminants will be blended

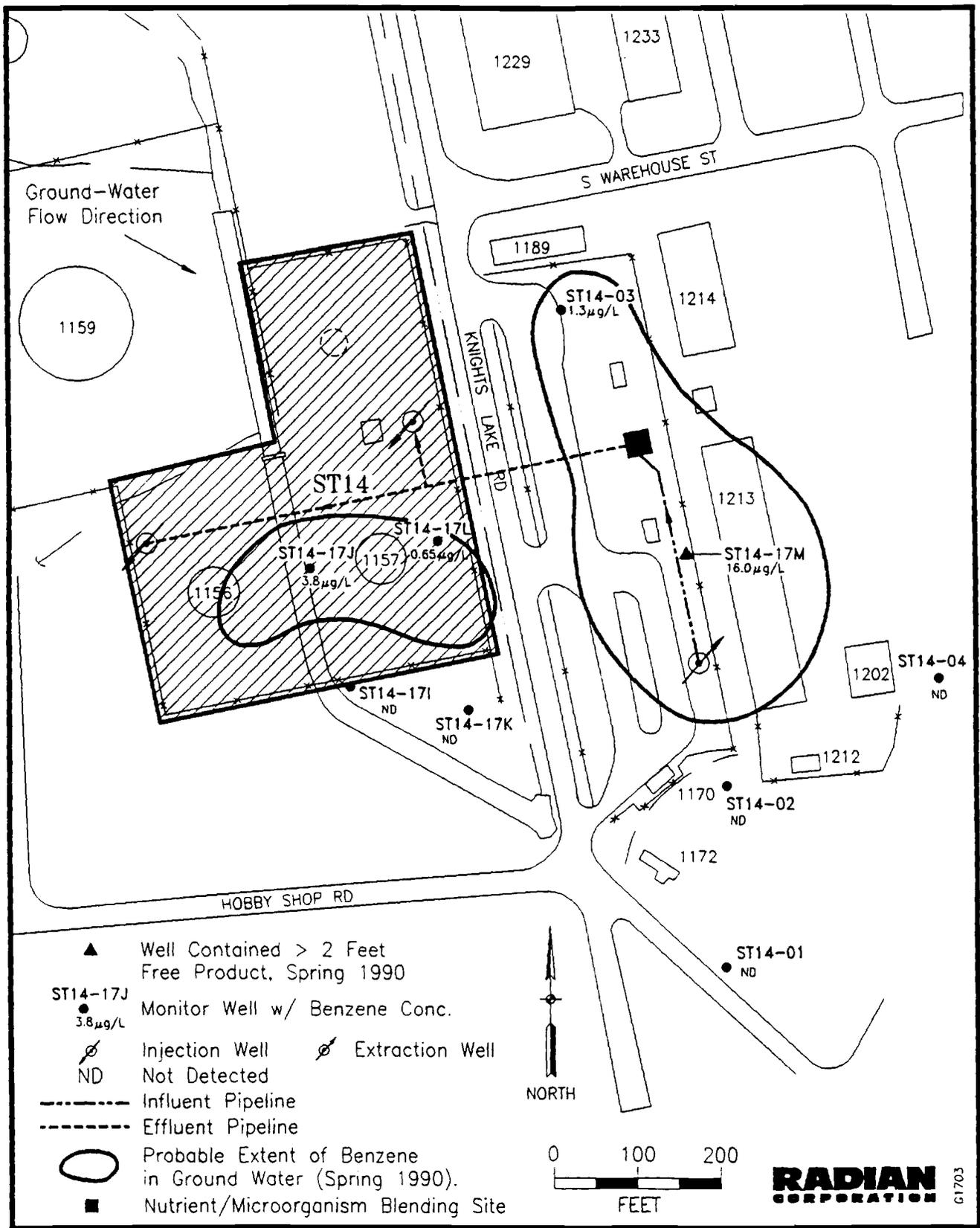


Figure 4-3. Alternative 5, Site ST14, East Area, Carswell AFB, Texas

with nutrients and microorganisms and re-injected into the Upper Zone. The microorganisms will utilize the carbon from the contaminants as an energy source, converting it to carbon dioxide and water. Contaminants adsorbed onto soil particles in the saturated portions of the Upper Zone may also be degraded. As a result of the extraction and re-injection, the Upper Zone should experience increased flushing and thus potentially reduced remediation time. Migration of contaminated ground water to other portions of the Upper Zone, as well as to Unnamed Stream or Farmers Branch, should be minimized and possibly prevented by Alternative 5. Potential spills from the blending facility, the oil/water separator, and influent and effluent pipelines will be minimized through the use of appropriate containment designs.

4.4.4.3 Compliance with ARARs

Alternative 5 should achieve all remedial action objectives established for the site. Immiscible hydrocarbon and dissolved contaminants in the Upper Zone will be biologically oxidized in situ to concentrations below MCLs. Further contamination of ground water and contaminant migration to other portions of the Upper Zone or to other media should be minimized, if not prevented. Measures to contain spills originating from pipelines conveying contaminated ground water, blending equipment, and by-product storage will all be incorporated into the design and implementation of the alternative, thus minimizing inadvertent migration of contaminants from treatment equipment.

4.4.4.4 Long-Term Effectiveness and Permanence

The evaluation of Alternative 5 for this criterion should be the same as that for Alternative 4A. However, the expected simultaneous biological treatment of the ground water and the aquifer materials should virtually eliminate residual contamination in the Upper Zone.

4.4.4.5 Reduction in Toxicity, Mobility, or Volume

The evaluation of Alternative 5 for this criterion is essentially the same as that for Alternative 4A. Alternative 5 provides an additional

benefit by biologically destroying the contaminants of concern, thus reducing the toxicity.

4.4.4.6 Short-Term Effectiveness

The evaluation of Alternative 5 for this criterion is essentially the same as that for Alternative 4A, with one exception. Alternative 5 may require additional time to achieve the RAOs. The length of time that the biological treatment requires to achieve the RAOs will depend on the microorganism population and on physical conditions in the Upper Zone.

4.4.4.7 Implementability

Alternative 5 makes use of several proven, reliable technologies in support of a somewhat new and innovative approach to biological treatment. Physically, the implementation of Alternative 5 depends on the Upper Zone being sufficiently homogeneous and isotropic such that microorganisms and nutrients injected into it will contact all of the contamination. The permeability and porosity of the soil must be adequate to allow for the growth of microorganisms without impeding flow. The in-situ biological process has been used in recent years to clean up a number of sites. However, regulatory acceptance of the in-situ biological treatment system would be necessary prior to implementation. Treatability studies may be required to demonstrate the effectiveness and timeliness of treatment before the regulatory agencies approve the alternative.

4.4.4.8 Cost

The present worth cost estimate for Alternative 5 for Site ST14 is approximately \$1,933,000. The estimated capital cost for Alternative 5 is approximately \$391,900. The annual O&M cost estimate is approximately \$100,300.

4.5 Detailed Evaluation of Alternatives for Site BSS

Alternatives 1, 2A, 2B, and 3 are evaluated in the following subsections.

4.5.1 Alternative 1--No Action

The following subsections describe the alternative and discuss each of the CERCLA evaluation criteria.

4.5.1.1 Description of the Alternative

Except for long-term monitoring, no remedial activities would be implemented at Site BSS with the no-action alternative. Long-term monitoring at Site BSS will make use of the existing Upper Zone monitoring well network and additional wells. The existing monitoring well network consists of three wells. It is expected that three or four additional monitor wells will be required downgradient of existing contamination to evaluate the effectiveness of the selected remedial alternative. Monitor wells should be sampled and analyzed for volatile aromatic compounds, total petroleum hydrocarbons, and dissolved metals on a quarterly basis for the duration of the remedial action. However, because of the thin saturated zone and local variability in the occurrence of Upper Zone ground water at this site, it is possible that some wells may be dry during any given sampling event, especially once ground-water control technologies are in place. Evidence of increased migration, such as significantly or consistently higher contaminant concentrations, or significant changes in the occurrence of the contaminants, would justify the initiation of further evaluation.

4.5.1.2 Protection of Human Health and the Environment

The no-action alternative does not reduce the risk to human health or the environment resulting from contamination at Site BSS. Ground-water contamination currently exceeds the requirements for satisfying the remedial action objectives. The baseline risk assessment for the site determined that

the noncarcinogenic health effects originating from the site were insignificant compared to the standards set by EPA. Carcinogenic health effects associated with the site were approximately 10^{-9} based on inhalation exposure. The risk assessment concluded that the ingestion and dermal exposure pathways were insignificant. Ground-water flow at Site BSS is currently toward the West Fork of the Trinity River. If contaminants reach the river, the concentrations will be further reduced by the effects of dilution and volatilization. Therefore, the risk to human health or the environment would be the same or lower than that determined in the baseline risk assessment.

4.5.1.3 Compliance with ARARs

The no-action alternative does not meet the RAOs established for the site. Some contaminant concentrations in ground water at Site BSS were in excess of MCLs in 1990.

4.5.1.4 Long-Term Effectiveness and Permanence

Because no remedial activity is implemented for the no-action alternative, the residual risk remains the same as the baseline risk. Natural attenuation could result in some long-term reduction in risks. However, natural attenuation would occur over a long period of time, so long-term reduction in risk should be insignificant. Long-term monitoring will identify changes in contaminant concentrations and the extent of the contaminant plume. Further remedial action may become necessary if these changes appear to present additional risks or hazards not currently apparent. Because contamination is left on site, long-term monitoring and other institutional controls may be necessary in perpetuity.

4.5.1.5 Reduction in Toxicity, Mobility, or Volume

No reduction in the toxicity, mobility, or volume of contamination occurs from implementation of the no-action alternative. It neither inhibits nor prevents continued migration of contaminants, nor does it further prevent degradation of Upper Zone ground-water quality. Long-term monitoring of the

ground water at Site BSS will allow initiation of remedial actions if significant changes in contaminant concentrations or extent are detected.

4.5.1.6 Short-Term Effectiveness

The baseline risk assessment for Site BSS indicates that the risks to human health and the environment are insignificant. Implementation of the no-action alternative will not increase these risks. Remediation of the contaminant plume to meet the criteria used to measure successful achievement of remedial action objectives can occur only by natural attenuation and only after a long period of time.

4.5.1.7 Implementability

Implementation of the no-action alternative for Site BSS involves the design and execution of a long-term monitoring program and the installation of four ground-water monitoring wells, neither of which activities should present problems. The primary obstacle to implementation of the no-action alternative will be securing approval from regulatory agencies and gaining public acceptance. The alternative calls for leaving an unknown volume of untreated hydrocarbon residue, as well as contaminated ground water, untreated and uncontained. Regulatory acceptance will be difficult unless other options are technically infeasible for Site BSS.

4.5.1.8 Cost

The present worth cost estimate for the no-action alternative for Site BSS is approximately \$430,000. The estimated capital cost for the no-action alternative including the cost of four additional ground-water monitor wells is approximately \$21,100. The annual O&M cost estimate is approximately \$26,600.

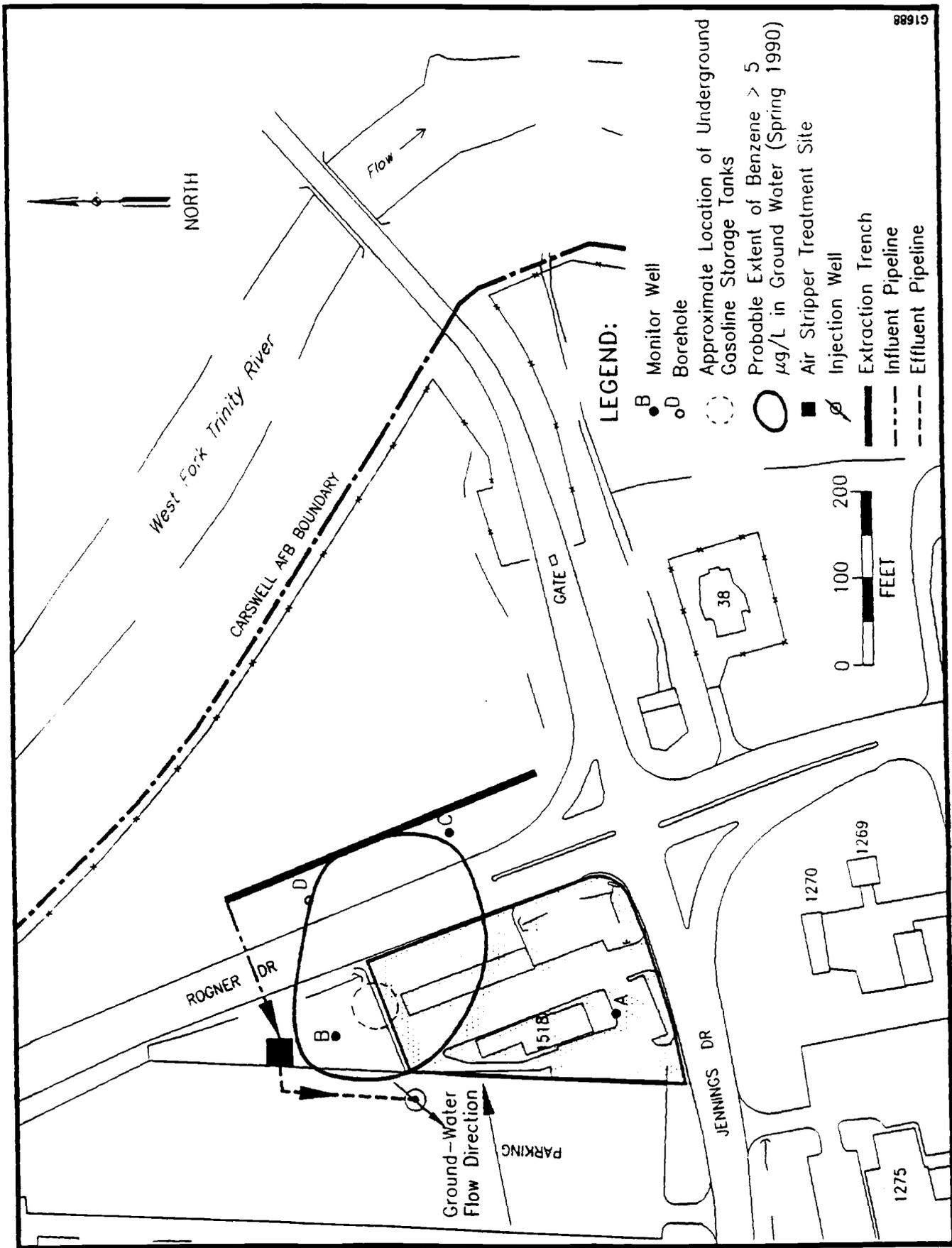


Figure 4-4. Alternative 2A, Site BSS East Area, Carswell AFB, Texas

4.5.2.2 Protection of Human Health and the Environment

Alternative 2A should reduce the risk to human health and the environment resulting from ground-water contamination at Site BSS. The alternative will extract contaminated ground water from the Upper Zone. The air stripper will remove soluble hydrocarbons and other volatile organic compounds from the ground water prior to re-injecting it into the aquifer. Re-injection should result in increased flushing of the Upper Zone and thus potentially decreased remediation time. Migration of contaminated ground water to other portions of the Upper Zone, as well as to the nearby West Fork of the Trinity River, should be minimized and possibly prevented by Alternative 2A. The only potential risk of exposure to site contaminants could be from the contaminant-laden air stripper off-gas. The mass of contaminants released from the air stripper will be limited to 5 lb/day, beyond which secondary treatment, such as fume incineration or activated carbon adsorption, will be implemented. Therefore, the risk of exposure to contaminants from the air stripper should be minimal.

4.5.2.3 Compliance with ARARs

Alternative 2A should achieve all remedial action objectives established for the site. Contaminant concentrations in site ground water should be reduced below MCLs. Therefore, further contamination of ground-water and contaminant migration to other portions of the Upper Zone or to other media should be minimized. Measures to prevent and contain spills originating from pipelines conveying contaminated ground water, treatment equipment, and by-product storage will all be incorporated into the design and implementation of the alternative.

4.5.2.4 Long-Term Effectiveness and Permanence

Once Alternative 2A has been implemented, residual risks from contamination at Site BSS should be less than the baseline risk. The majority of contaminants in the ground water will be removed, and the remaining concentrations of contaminants (less than MCLs, as required) will be further

reduced by natural attenuation. Unless a previously unidentified contaminant source exists, the residual risks should be acceptable and the remedy should be considered permanent. The alternative relies on ground water to flush contaminants from Upper Zone materials. Therefore, insoluble compounds which may be strongly adsorbed onto soils will not be removed. Long-term monitoring of the ground water after remediation will identify changes in contaminant concentrations and will identify significant changes in contaminant distribution which might indicate new contaminant sources or leaching of remnant contamination. Additional remedial measures could be determined and evaluated at that time.

4.5.2.5 Reduction in Toxicity, Mobility, or Volume

By hydraulically containing and removing contamination from the Upper Zone at Site BSS, Alternative 2A should reduce the mobility and volume of contamination. The air stripper should remove contaminants from the ground water, but it will not reduce the toxicity of the contaminants. No by-products are expected from the remedial action. Soluble contaminants in the ground water should be transferred out of solution into the air phase in the air stripper. Airborne contaminants would be significantly diluted or, if necessary, will be treated using fume incineration or activated carbon adsorption. Therefore, toxicity is effectively reduced.

4.5.2.6 Short-Term Effectiveness

The baseline risk assessment for Site BSS indicates that the risks to human health and the environment are insignificant. Remedial activities conducted for Alternative 2A should not result in any increase in risk to on- or off-base personnel. Soil excavated during construction of the trench may temporarily introduce the risk of exposure for on-site personnel and for contaminant migration. However, if soil is handled, stored, and disposed of correctly, the temporary increase in risk from the soil should be insignificant. Remedial action objectives should be achieved relatively quickly (1 to 5 years) once implementation of the alternative has begun.

4.5.2.7 Implementability

Alternative 2A makes use of proven, reliable technologies for remediation of Site BSS, and no outstanding impediments to implementation should occur. The extraction trenches should operate well under the conditions at Site BSS. Passive extraction procedures such as trenches are optimum for the variable occurrence and small volume of contaminated ground water found at Site BSS. Some minor disruptions of base traffic may occur while the effluent line is constructed under Rogner Drive. However, these disruptions should be minimized if boring and jacking rather than open cut techniques are used to construct the crossing. No permitting or regulatory approval problems are anticipated for Alternative 2A.

4.5.2.8 Cost

The present worth cost estimate for Alternative 2A for Site BSS is approximately \$1,570,400. The estimated capital cost for Alternative 2A is approximately \$528,900. The annual O&M cost estimate is approximately \$67,800.

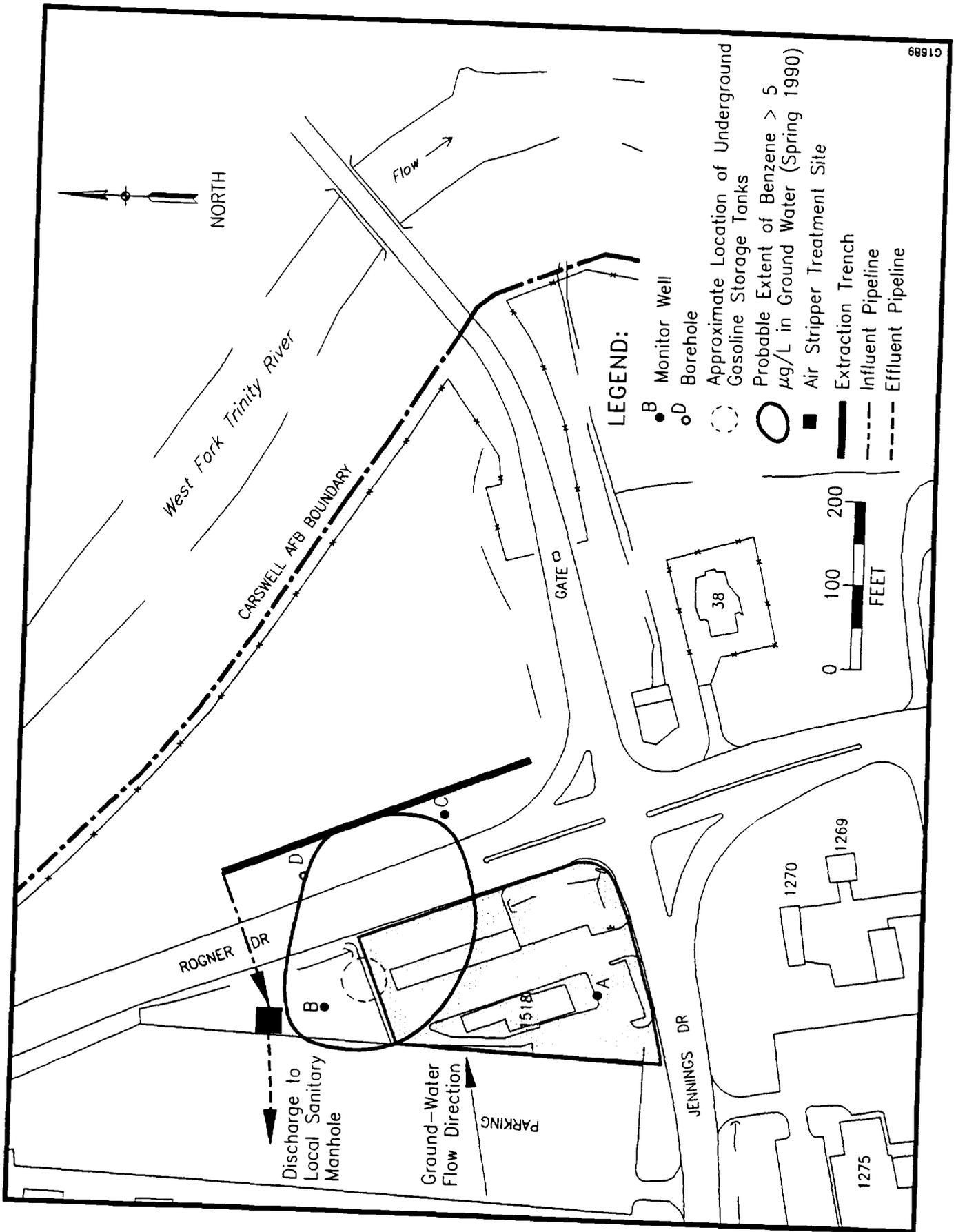
4.5.3 Alternative 2B--Air Stripping and Discharge to the Sanitary Sewer

The following subsections describe the alternative and discuss each of the CERCLA evaluation criteria.

4.5.3.1 Description of the Alternative

Alternative 2B (see Figure 4-5) includes most of the components of Alternative 2A. However, rather than re-injecting the treated ground water, it will be discharged to a nearby sanitary sewer. The differences between Alternative 2A and 2B are as follows:

- No ground-water injection wells will be used in Alternative 2B;



68810

Figure 4-5. Alternative 2B, Site R5S, East Area, Carswell AFB, Texas

- A new "drop" manhole will be constructed on a nearby 8-inch sanitary sewer line; and
- Approximately 200 feet of 4-inch, Schedule 80 PVC pipe will be used to convey treated effluent to the sanitary manhole (in lieu of the 200 feet of 2-inch PVC pipe used in Alternative 2A).

The remaining components will be the same as those for Alternative 2A.

4.5.3.2 Protection of Human Health and the Environment

The evaluation of Alternative 2B for this criterion is the same as for Alternative 2A, with the following additional concerns, caused by the fact that in Alternative 2B, treated ground water would be discharged to a nearby sanitary sewer. During a process upset, contaminated ground water could be discharged to the sanitary sewer, and some volatilization of contaminants could occur. With dilution in the ambient air, the risk of exposure to contaminants should be minimal. Also under an upset condition, contaminated ground water could leak from the sanitary sewer and contaminate other water-bearing and non-water-bearing zones. Again, the dilution and volatilization factor in the sewer should be sufficient to minimize any additional risk.

4.5.3.3 Compliance with ARARs

The evaluation of Alternative 2B for this criterion should be the same as that for Alternative 2A. However, Alternative 2B must also meet the pretreatment requirements of the City of Fort Worth's sanitary sewer use ordinance. Preliminary conversations with City of Fort Worth personnel indicate that the air stripping process provides adequate removal of volatile organic contaminants to achieve the limits established by the City.

4.5.3.4 Long-Term Effectiveness and Permanence

The evaluation of Alternative 2B for this criterion should be the same as that for Alternative 2A, with the following exception: if at any time the City of Fort Worth changes its sewer use ordinance or limits the incoming flow to the POTW, an alternate disposal method for the treated effluent may be required. Presumably, notification of the changes by the City would be adequate to evaluate other discharge options, make a selection, and avoid disruption of operations.

4.5.3.5 Reduction in Toxicity, Mobility, or Volume

The evaluation of Alternative 2B for this criterion should be the same as that for Alternative 2A. However, during upset conditions the potential exists for contaminant discharge to the sanitary sewer. Such discharges could result in the migration of contaminants through leaking sewer pipes and in the exposure of City workers to volatilized contaminants.

4.5.3.6 Short-Term Effectiveness

The evaluation of Alternative 2B for this criterion is the same as that for Alternative 2A.

4.5.3.7 Implementability

The evaluation of Alternative 2B for this criterion should be the same as that for Alternative 2A, with the following exception: implementation of Alternative 2B may require a permit to discharge into the sanitary sewer. This permit would be issued under the POTW's sewer use ordinance. Preliminary conversations with City of Fort Worth personnel have indicated that the volume and quality of the treated ground water from the air stripper should not present a problem to the treatment plant and should meet the sewer use ordinance requirements.

4.5.3.8 Cost

The present worth cost estimate for Alternative 2B for Site BSS is approximately \$1,523,400. The estimated capital cost for Alternative 2B is approximately \$516,000. The annual O&M cost estimate is approximately \$65,500.

4.5.4 Alternative 3--In-Situ Biological Treatment

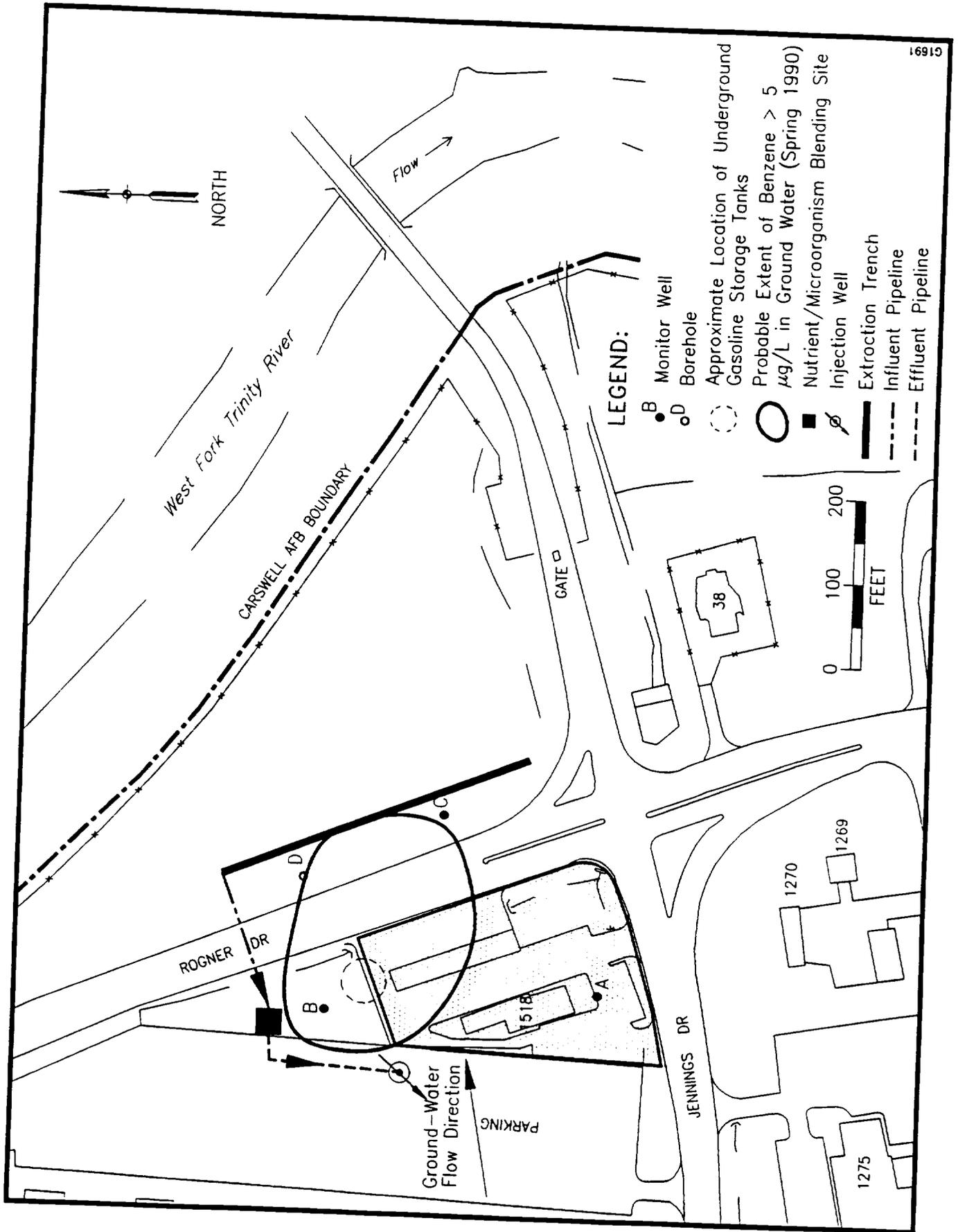
The following subsections describe the alternative and discuss each of the CERCLA evaluation criteria.

4.5.4.1 Description of the Alternative

Alternative 3 (see Figure 4-6) uses many of the components of Alternative 2A. However, Alternative 3 involves the use of in-situ biological degradation rather than air stripping to treat the contaminated ground water. Changes in components between Alternative 2A and 3 are as follows:

- A nutrient and microorganism blending facility will be substituted for the air stripping tower; and
- 200 feet of 2-inch/4-inch dual-wall containment pipe will be used (in lieu of the 200 feet of 2-inch, Schedule 80 PVC pipe used in Alternative 2A).

In Alternative 3, treatment of contaminated ground water will occur in the Upper Zone. Therefore, the piping from the blending facility to the injection wells will be conveying contaminated ground water. Dual containment piping is necessary to minimize contaminant migration resulting from pipe breaks or leaks.



16910

Figure 4-6. Alternative 3, Site P-3, East Area, Carswell AFB, Texas

4.5.4.2 Protection of Human Health and the Environment

Alternative 3 should reduce the risk to human health and the environment resulting from ground-water contamination at Site BSS. This alternative will extract contaminated ground water from the Upper Zone, blend it with nutrients and microorganisms, and re-inject the mixture into the Upper Zone. The microorganisms will utilize the carbon from the contaminants as an energy source, converting it to carbon dioxide and water. Contaminants adsorbed onto soil particles in the saturated portions of the Upper Zone may also be degraded. As a result of the extraction and re-injection, the Upper Zone should experience increased flushing and thus potentially reduced remediation time. Migration of contaminated ground water to other portions of the Upper Zone, as well as to the West Fork of the Trinity River, should be minimized and possibly prevented by Alternative 3. Potential spills from the blending facility and influent and effluent pipelines will be minimized through the use of appropriate containment designs.

4.5.4.3 Compliance with ARARs

Alternative 3 should achieve all remedial action objectives established for the site. Dissolved and adsorbed contaminants in the Upper Zone should be biologically remediated to concentrations below MCLs. Further contamination of ground water and contaminant migration to other portions of the Upper Zone or to other media should be minimized if not prevented. Measures to contain spills originating from pipelines conveying contaminated ground water, blending equipment, and by-product storage will all be incorporated into the design and implementation of the alternative, thus minimizing inadvertent migration of contaminants from treatment equipment.

4.5.4.4 Long-Term Effectiveness and Permanence

The evaluation of Alternative 3 for this criterion should be the same as that for Alternative 2A. However, the expected simultaneous biological treatment of the ground water and the aquifer materials should reduce the

amount of residual contamination in the Upper Zone. Leaching of remnant contamination after remediation is complete is therefore minimized or prevented.

4.5.4.5 Reduction in Toxicity, Mobility, or Volume

The evaluation of Alternative 3 for this criterion is essentially the same as that for Alternative 2A. Alternative 3 provides an additional benefit by biologically destroying the contaminants of concern, thus reducing the toxicity.

4.5.4.6 Short-Term Effectiveness

The evaluation of Alternative 3 for this criterion is essentially the same as that for Alternative 2A, with one exception. Alternative 3 may require additional time to achieve the RAOs. The length of time that the biological treatment requires to achieve the RAOs will depend on the microorganism population and on physical conditions in the Upper Zone.

4.5.4.7 Implementability

Alternative 3 makes use of several proven, reliable technologies in support of a somewhat new and innovative approach to biological treatment. Physically, the implementation of Alternative 3 depends on the Upper Zone being sufficiently homogeneous and isotropic such that microorganisms and nutrients injected into it will contact with all of the contamination. The permeability and porosity of the soil must be adequate to allow for the growth of microorganisms without impeding flow. The in-situ biological process has been used in recent years to clean up a number of sites. However, regulatory acceptance of the in-situ biological treatment system would be necessary prior to implementation. Treatability studies may be required to demonstrate the effectiveness and timeliness of treatment before the regulatory agencies approve the alternative.

4.5.4.8 Cost

The present worth cost estimate for Alternative 3 for Site BSS is approximately \$1,390,400. The estimated capital cost for Alternative 3 is approximately \$359,200. The annual O&M cost estimate is approximately \$67,100.

4.6 Opportunities for Coordination of Remedial Activities

The proximity of Sites ST14 and BSS and the similarity of feasible remedial action alternatives provides the opportunity to coordinate the two remedial actions. The following paragraphs describe possibilities for coordinating remedial actions at the two sites.

4.6.1 Ground-Water Alternatives

Remedial action alternatives for contaminated ground water at Sites ST14 and BSS are based on two primary technologies, air stripping and in-situ biological treatment. Because of the proximity of the two sites and the similarity of the contaminants in the two plumes, the most obvious opportunity for coordinating ground-water remedial actions is a combination of Alternatives 4B (Site ST14) and 2B (Site BSS). A common air stripper facility and discharge point could be used by the two remedial actions. Contaminated ground water would be removed using an extraction well at Site ST14 and an extraction/interceptor trench at Site BSS. The contaminated ground water would then be pumped to the common treatment facility. The treated ground water would be pumped to a common point of discharge to a nearby sanitary sewer.

The most obvious advantage of coordinating remedial actions at the two sites is the cost savings related to elimination of one treatment facility. While the capacity of the combined facility would be greater than that of a single facility at either site, the capital cost of the larger facility would be less than the capital cost of two separate facilities. Even adding

4-39

the cost for additional influent piping, the cost for combining the two facilities should be less.

For Alternatives 4A and 5 (Site ST14) and 2A and 3 (Site BSS), the advantages of a combined treatment facility are not as apparent. In a combined scenario for these alternatives, the treated (or blended) ground water would have to be pumped back to the two sites and re-injected. The cost of the additional effluent piping from the combined treatment facility to each site plus the cost of the additional influent piping may be comparable to the cost savings realized by the elimination of one plant. However, some savings may be realized by the reduction in operation and maintenance of one plant versus two.

Disadvantages of a combined ground-water remedial action include:

- The potential for exceeding the allowable TACB discharge limits of 5 lb/day of contaminants from the air stripper; and
- For Alternatives 3 and 5, the potential for cross-contaminating the two sites.

4.6.2 Soil Alternatives

Opportunities for coordinating remedial alternative for soil contamination at Sites ST14 and BSS also exist. Like the ground-water alternatives, remedial alternatives for soils are based on a primary technology involving treatment. For Alternative 2 (both of Sites ST14 and BSS), the technology is treatment of volatile organic vapors extracted from the soils using extraction trenches or wells. For Alternative 3 (both of Sites ST14 and BSS), the common technology would be the soil piles used to treat contaminated soils excavated from either (or both) site(s). For Alternative 4 (both of Sites ST14 and BSS), in-situ biological treatment of soils at the two sites could share a common blending facility. Like the ground-water alternatives, the alternatives that offer the most obvious advantages are those that do not require the treated material to be returned to the respective

sites. Alternative 2, and to a lesser extent Alternative 3, offers this advantage. The disadvantages that apply to the combined soils alternatives are the same as those that apply to the combined ground-water alternatives.

4.6.3 Combined Soil and Ground-Water Alternatives

The interactions of ground water and soil responses to certain remedial alternatives are significant at Sites BSS and ST14. Therefore, opportunities for combining complementary remedial actions for each medium exist at both sites individually and together.

The ground-water and soil treatment technologies which provide complementary remediation due to media interactions, and which therefore can be combined as remedial alternatives, are:

- Air stripping of ground-water and soil vapor extraction;
- In-situ biological treatment of ground water and soil; and
- Air stripping of ground-water and soil pile treatment.

Soil vapor extraction depends on the porosity of the subsurface to remove the VOC contaminants. If a treatment is chosen that may decrease soil porosity, such as injection of nutrient-rich water for biological treatment, it would reduce the effectiveness of the soil vapor extraction. In-situ biological treatment of the ground water and soil complement each other. The microorganisms and nutrients allowed to infiltrate into the soil will percolate down to the water table and augment the ground-water bio-treatment. Treatment of contaminant-laden soil vapors from the soil piles can easily be treated along with contaminant-laden air stripper off-gases. All three complementary remedial actions would avoid duplication or unnecessary diversity of treatment facilities for the remedial alternatives, (e.g., two secondary treatment facilities, one for air-stripping off-gas and the other for soil vapors, or two biological mixing facilities, one for ground water and the other for soils). As mentioned previously, the need for the secondary treatment for air

stripping and soil gas is dependent on the quantity of emissions and on state guidelines.

The obvious advantage of coordinating media-specific alternatives is cost. By combining treatment facilities, a reduction in the capital cost for one (combined) facility versus two (uncombined) facilities should be realized. In addition to capital cost, another potential benefit of combining treatment facilities is that the O&M cost for one (combined) facility should be marginally smaller than the cost for two smaller (uncombined) facilities. Treatment efficiencies, and thus power and materials, should be higher with a larger facility. The labor needed to staff and maintain one (combined) facility should be less than that for two (uncombined) facilities.

For coordinating combined-media remedial alternatives, there are the same opportunities as those that exist for coordinating media-specific remedial alternatives at Sites ST14 and BSS. The advantages and disadvantages for the coordinated combined-media alternatives are also the same.

4.7 Comparative Evaluation of Remedial Alternatives

A matrix evaluation was conducted on the remedial alternatives discussed in the preceding sections. The matrix approach allows a comparative analysis of the alternatives using both their ability to satisfy established criteria and present worth cost. The matrix evaluation was performed using information presented in Sections 4.4 and 4.5 of this report.

4.7.1 Matrix Approach

Up to this point, each alternative has been descriptively evaluated with respect to the following criteria:

- Overall protection of human health and the environment;
- Compliance with ARARs;
- Long-term effectiveness and permanence;
- Reduction of toxicity, mobility, or volume through treatment;

- Short-term effectiveness;
- Implementability; and
- Cost.

For the comparative analysis or matrix evaluation, a scoring system was established for the above criteria, and scores for each criteria were determined for each alternative. Table 4-1 lists the scoring basis for each of the evaluation criteria parameters (except for cost).

Tables 4-2 and 4-3 are blank evaluation matrix tables showing the four alternatives for each site, evaluation parameters, weighting factors, cost measures, the effectiveness total column, and the effectiveness-to-cost quotient column. The capital, operating and maintenance, and net present value costs for each alternative discussed earlier in the report are summarized in the table under the appropriate column headings. Using the matrix approach, evaluation scores for six of the seven criteria are developed for each alternative. These scores are multiplied by a weighting factor (top row on Tables 4-2 and 4-3) and summed to determine the effectiveness total. The alternative having the greatest quotient of the effectiveness total divided by the present worth cost total is considered to be the most cost-effective alternative. The quotient value is presented in the right hand column of the matrix.

The results of the comparative analysis using the matrix approach are presented in Tables 4-4 and 4-5. From Table 4-4, the most cost-effective alternative (excluding the no-action alternative) for Site ST14 is Alternative 5. From Table 4-5, the most cost-effective alternative for Site BSS is Alternative 3. As previously documented, the only feasible action for Sites LF01 and SD13 is no action, other than long-term monitoring. Therefore, the matrix evaluation is not applicable to these sites.

TABLE 4-1. CRITERIA SCORES FOR DETAILED ANALYSIS OF REMEDIAL ALTERNATIVES

| Criterion | Scoring Basis |
|--|--|
| Overall Protection of Human Health/ Environment | 3 - Will greatly reduce risk 2 - Will reduce risks 1 - Will not reduce risks |
| Compliance with ARARs | 3 - Will meet or exceed ARARs 2 - Will meet ARARs 1 - Will not meet ARARs |
| Long-Term Effectiveness/Permanence | 3 - Very little residual con- tamination after remedia- tion 2 - Some residual contamination after remediation 1 - Contamination unchanged by remediation |
| Reduction in Toxicity, Mobility, or Volume | 3 - Reduction of all three 2 - Reduction in mobility and volume, but not toxicity 1 - No reduction in mobility, volume, or toxicity |
| Short-Term Effectiveness | 3 - Very few additional risks to on- and off-site person- nel during remediation; remedial action objectives achieved within 2-5 years 2 - Some minor additional risks; remedial action objectives met within 10 years 1 - Major risks during imple- mentation; remedial action objectives met within 20 to 30 years |
| Implementability | 3 - No impediments 2 - Some impediments, but easily overcome 1 - Some impediments overcome with difficulty |

TABLE 4-2. REMEDIAL ALTERNATIVES COMPARATIVE EVALUATION MATRIX,
SITE ST14, EAST AREA, CARSWELL AFB, TEXAS

| Alternative | Capital Cost (\$ M) | OM Cost (\$ M) | NPW (\$ M) | Protect. Human Hlth. & Env. | Compliance w/ARARs | Long-Term Effect. | Reduct. of Tox., Mob. & Vol. | Short-Term Effect. | Effect. Total | Effect. Quotient |
|---|---------------------|----------------|------------|-----------------------------|--------------------|-------------------|------------------------------|--------------------|---------------|------------------|
| Weighting Factor | 1 | 1 | 1 | 3 | 2 | 3 | 3 | 1 | 2 | |
| 1 No Action | | | | | | | | | | |
| 4A Air Stripping and Re-injection | | | | | | | | | | |
| 4B Air Stripping and Discharge to San. Sev. | | | | | | | | | | |
| 5 In-situ Biological Treatment | | | | | | | | | | |

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M = 1,000,000 (e.g., \$2M = \$2,000,000)

TABLE 4-3. REMEDIAL ALTERNATIVES COMPARATIVE EVALUATION MATRIX,
SITE BSS, EAST AREA, CARSWELL AFB, TEXAS

| Alternative | Capital Cost (\$ M) | O&M Cost (\$ M) | NPW (\$ M) | Protect. Human Hlth. & Env. | Compliance w/ARARs | Long-Term Effect. | Reduct. of Tox., Mob. & Vol. | Short-Term Effect. | Effect. Total | Effect. Quotient |
|---|---------------------|-----------------|------------|-----------------------------|--------------------|-------------------|------------------------------|--------------------|---------------|------------------|
| Weighting Factor | 1 | 1 | 1 | 3 | 2 | 3 | 3 | 1 | 2 | |
| 1 No Action | | | | | | | | | | |
| 2A Air Stripping and Re-injection | | | | | | | | | | |
| 2B Air Stripping and Discharge to San. Sew. | | | | | | | | | | |
| 3 In-situ Biological Treatment | | | | | | | | | | |

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M = 1,000,000 (e.g., \$2M = \$2,000,000)

TABLE 4-4. REMEDIAL ALTERNATIVES COMPARATIVE EVALUATION MATRIX,
SITE ST14, EAST AREA, CARSWELL AFB, TEXAS

| Alternative | Capital Cost (\$ M) | O&M Cost (\$ M) | NPW (\$ M) | Protect. Human Hlth. & Env. | Compliance w/ARARs | Long-Term Effect. | Reduct. of Tox., Mob. & Vol. | Short-Term Effect. | Implement. | Effect. Total | Effect. Quotient |
|---|---------------------|-----------------|------------|-----------------------------|--------------------|-------------------|------------------------------|--------------------|------------|---------------|------------------|
| | 1 | 1 | 1 | | | | | | | | |
| 1 No Action | 0.0264 | 0.053 | 0.8442 | 1 | 1 | 1 | 1 | 2 | 1 | 15 | 18 |
| 4A Air Stripping and Re-injection | 0.5106 | 0.0943 | 1.3070 | 2 | 3 | 2 | 2 | 3 | 3 | 33 | 25 |
| 4B Air Stripping and Discharge to San. Sev. | 0.4690 | 0.0918 | 1.8806 | 2 | 3 | 2 | 2 | 3 | 2 | 31 | 16 |
| 5 In-situ Biological Treatment | 0.3919 | 0.1002 | 1.9330 | 3 | 3 | 2 | 3 | 2 | 2 | 36 | 19 |

M = 1,000,000 (e.g., \$2M = \$2,000,000)

TABLE 4-5. REMEDIAL ALTERNATIVES COMPARATIVE EVALUATION MATRIX,
SITE BSS, EAST AREA, CARSWELL AFB, TEXAS

| Alternative | Capital Cost (\$ M) | O&M Cost (\$ M) | NPW (\$ M) | Protect. Human Hith. & Env. | Compliance w/ARARs | Long-Term Effect. | Reduct. of Tox., Mob. & Vol. | Short-Term Effect. | Implement. | Effect. Total | Effect. Quotient |
|---|---------------------|-----------------|------------|-----------------------------|--------------------|-------------------|------------------------------|--------------------|------------|---------------|------------------|
| | 1 | 1 | 1 | 3 | 2 | 3 | 3 | 1 | 2 | | |
| 1 No Action | 0.0211 | 0.0266 | 0.4300 | 1 | 1 | 1 | 1 | 2 | 1 | 15 | 35 |
| 2A Air Stripping and Re-injection | 0.5288 | 0.0678 | 1.5704 | 2 | 3 | 2 | 2 | 3 | 3 | 33 | 21 |
| 2B Air Stripping and Discharge to San. Sew. | 0.5160 | 0.0655 | 1.5233 | 2 | 3 | 2 | 2 | 3 | 2 | 31 | 20 |
| 3 In-situ Biological Treatment | 0.3592 | 0.0671 | 1.3904 | 3 | 3 | 2 | 3 | 2 | 2 | 36 | 26 |

M = 1,000,000 (e.g., \$2M = \$2,000,000)

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GLOSSARY

| | |
|---------|---|
| 1,2-DCE | <u>cis</u> -1,2-dichloroethene |
| AFB | air force base |
| Ag | silver |
| ARAR | applicable or relevant and appropriate requirement |
| As | arsenic |
| Ba | barium |
| bgl | below ground level |
| BTEX | benzene, toluene, ethylbenzene, and xylene(s) |
| Cd | cadmium |
| CERCLA | Comprehensive Environmental Response, Compensation, and Liability Act of 1980 |
| cfm | cubic feet (or foot) per minute |
| Cr | chromium |
| DRMO | Defense Reutilization and Marketing Office |
| EPA | U.S. Environmental Protection Agency |
| ESLs | Effects Screening Levels [used by the Texas Air Control Board] |
| ft/day | feet (or foot) per day |
| g/L | gram(s) per liter |
| gpm | gallon(s) per minute |
| IRP | Installation Restoration Program |
| lb/day | pound(s) per day |
| lb/hr | pound(s) per hour |
| MCL | maximum contaminant level (established under the Safe Drinking Water Act) |
| mg/L | milligram(s) per liter |

GLOSSARY (con't)

| | |
|-------|---|
| NPDES | National Pollutant Discharge Elimination System |
| O&M | operating and maintenance |
| Pb | lead |
| POTW | publicly owned treatment works |
| RAO | remedial action objective |
| ROD | Record of Decision |
| Se | selenium |
| TACB | Texas Air Control Board |
| TCE | trichloroethene |
| TPH | total petroleum hydrocarbon(s) |
| TWC | Texas Water Commission |
| VOC | volatile organic compound |
| µg/L | microgram(s) per liter |

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Cost estimates for each of the alternatives are presented in Tables A-1 and A-8. The cost estimates encompass both capital costs and operating and maintenance costs. In addition, a present worth analysis was performed. In conducting the present worth analysis, the following assumptions were made: as recommended by CERCLA guidance, a discount rate of 5 percent was used. A 30 year period of performance was used to calculate the present worth of annual O&M costs. The present value costs for each remedial alternative assume that all design, permitting, and construction occurs within the first year of remediation. Pumps and equipment will require replacement every 10 years. Construction costs are for labor and material costs only. A 1.4 multiplier was used to estimate contractor overhead and profit. The accuracy of these "study estimate" costs is expected to be within 50 percent. The costs presented were developed from Means Site Work Cost Data, 1990, 95th Annual Edition, and from vendor quotes.

TABLE A-1
 COST ESTIMATE FOR ALTERNATIVE 1 (No-Action) SITE LF01

OPERATION AND MAINTENANCE COSTS

| | Total Cost (\$) / Year 0-30 Years |
|---|--------------------------------------|
| Ground-Water Monitoring System | |
| Semi-Annual Sampling and Analysis 5 Wells @ \$5000/well | 25,000 ----- |
| Total Annual Operation and Maintenance Cost | 25,000 |

NET PRESENT VALUE

| | |
|--|------------------|
| Present Value of Operation and Maintenance Cost | 384,311 ===== |
| TOTAL PRESENT VALUE | 384,311 |

0014 + 000

TABLE A-2

COST ESTIMATE FOR ALTERNATIVE 1 (No-Action) SITE SD13

OPERATION AND MAINTENANCE COSTS

| | Total Cost (\$) / Year 0-30 Years |
|---|--------------------------------------|
| Ground-Water Monitoring System | |
| Semi-Annual Sampling and Analysis 4 Wells @ \$3600/well | 14,400 |
| 4 Surface Water Stations @ \$2,700/Point | 10,800 ----- |
| Total Annual Operation and Maintenance Cost | 25,200 |
| | |
| NET PRESENT VALUE | |
| Present Value of Operation and Maintenance Cost | 387,386 ===== |
| TOTAL PRESENT VALUE | 387,386 |

2025 RELEASE UNDER E.O. 14176

TABLE A-3

COST ESTIMATE FOR ALTERNATIVE 1 (No-Action) SITE ST14

| Capital Costs | Units | Qty | Unit Price (\$) | Total Cost (\$) |
|--------------------------|-------|-----|-----------------|-----------------|
| Additional Mon Wells | Ea | 5 | 2,000 | 10,000 |
| Additional Well SUBTOTAL | | | | <u>10,000</u> |
| Multiplier | | | | <u>1.4</u> |
| TOTAL | | | | <u>14,000</u> |
| | | | | ===== |
| CONSTRUCTION SUBTOTAL | | | | 14,000 |

| | Percentage of Total Cost | |
|-----------------------------|--------------------------|---------------|
| | Percentages | |
| Bid Contingencies | 15 | 2,100 |
| Scope Contingencies | 25 | 3,500 |
| Construction Total | | <u>19,600</u> |
| Permitting and Legal | 5 | 980 |
| Bonding and Insurance | 3 | 588 |
| Service During Construction | 4 | 784 |
| Miscellaneous Lab Testing | 5 | 980 |
| Total Implementation Cost | | <u>22,932</u> |
| Engineering Design | 15 | 3,440 |
| Total Capital Cost | | <u>26,372</u> |

Page 100

OPERATION AND MAINTENANCE COSTS

Total Cost (\$) / Year
0-30 Years

Ground-Water Monitoring System

Semi-Annual Sampling
and Analysis
14 Wells @ \$3800/well

53,200

Total Annual Operation and
Maintenance Cost

53,200

NET PRESENT VALUE

Capital Cost

26,372

Present Value of Operation and
Maintenance Cost

817,814

=====

TOTAL PRESENT VALUE

844,186

TABLE A-4

COST ESTIMATE FOR ALTERNATIVE 4A SITE ST14

| Capital Costs | Units | Qty | Unit Price (\$) | Total Cost (\$) |
|---|-------|-----|-----------------|-----------------|
| Ground Water Withdrawal System | | | | |
| Extraction Well | Ea | 1 | 2,000 | 2,000 |
| Well Pump | Ea | 1 | 2,500 | 2,500 |
| Plastic Dual Wall Pipe and fittings | LF | 250 | 32.00 | 8,000 |
| Excavation Backfill (1' wide, 3' deep) | LF | 250 | 2.45 | 613 |
| Withdrawal System SUBTOTAL | | | | 13,113 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 18,358 |
| Ground-water treatment system | | | | |
| Oil Water Separator | Ea | 1 | 38,000 | 38,000 |
| Air Stripping Tower | Ea | 1 | 50,000 | 50,000 |
| Liquid Circ. Pump | Ea | 1 | 3,550 | 3,550 |
| Gas Blower | Ea | 1 | 20,000 | 20,000 |
| Storage Tank | Ea | 1 | 7,500 | 7,500 |
| Controls & Plumbing | Ea | 1 | 20,000 | 20,000 |
| Containment Pad | Ea | 1 | 10,000 | 10,000 |
| Sched 80 PVC - 2" pipe and fittings | LF | 670 | 4.40 | 2,948 |
| Excavation Backfill (1' wide, 3' deep) | LF | 670 | 2.45 | 1,642 |
| Boring for 2" pipe (100' minimum) | LF | 100 | 12.14 | 1,214 |
| Jacking Pit Prep | Ea | 1 | 8,000 | 8,000 |
| Ground-water treatment System SUBTOTAL | | | | 162,854 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 227,995 |

Treated Water Injection System

| | | | | |
|---------------------------|----|---|-------|--------|
| Injection Wells | Ea | 2 | 2,000 | 4,000 |
| Injection Pumps | Ea | 2 | 3,500 | 7,000 |
| Injection System SUBTOTAL | | | | 11,000 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 15,400 |

| | | | | |
|--------------------------|----|---|-------|--------|
| Additional Mon Wells | Ea | 5 | 2,000 | 10,000 |
| Additional Well SUBTOTAL | | | | 10,000 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 14,000 |

CONSTRUCTION SUBTOTAL 275,752

Percentage of Total Cost

| | Percentages | |
|-----------------------------|-------------|---------|
| Bid Contingencies | 15 | 41,363 |
| Scope Contingencies | 25 | 68,938 |
| Construction Total | | 386,053 |
| Permitting and Legal | 3 | 11,582 |
| Bonding and Insurance | 3 | 11,582 |
| Service During Construction | 4 | 15,442 |
| Miscellaneous Lab Testing | 5 | 19,303 |
| Total Implementation Cost | | 443,961 |
| Engineering Design | 15 | 66,594 |
| Total Capital Cost | | 510,556 |

TABLE A-5

COST ESTIMATE FOR ALTERNATIVE 4B SITE ST14

| Capital Costs | Units | Qty | Unit Price (\$) | Total Cost (\$) |
|---|-------|-----|-----------------|-----------------|
| Ground Water Withdrawal System | | | | |
| Extraction Well | Ea | 1 | 2,000 | 2,000 |
| Well Pump | Ea | 1 | 2,500 | 2,500 |
| Plastic Dual Wall Pipe and fittings | LF | 250 | 32.00 | 8,000 |
| Excavation Backfill (1' wide, 3' deep) | LF | 250 | 2.45 | 613 |
| Withdrawal System SUBTOTAL | | | | 13,113 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 18,358 |
| Ground-water treatment system | | | | |
| Oil Water Separator | Ea | 1 | 38,000 | 38,000 |
| Air Stripping Tower | Ea | 1 | 50,000 | 50,000 |
| Liquid Circ. Pump | Ea | 1 | 3,550 | 3,550 |
| Gas Blower | Ea | 1 | 20,000 | 20,000 |
| Storage Tank | Ea | 1 | 7,500 | 7,500 |
| Controls & Plumbing | Ea | 1 | 20,000 | 20,000 |
| Containment Pad | Ea | 1 | 10,000 | 10,000 |
| Excavation Backfill (1' wide, 3' deep) | LF | 670 | 2.45 | 1,642 |
| Ground-water treatment System SUBTOTAL | | | | 150,692 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 210,968 |
| Treated Water Transport System | | | | |
| Manhole to Existing 8" Sewer Line | Ea | 1 | 1,620 | 1,620 |
| Sched 80 PVC - 4" pipe and fittings | LF | 250 | 7.15 | 1,788 |

| | | | | |
|--|----|-----|-------|-----------------|
| Excavation Backfill (1' wide, 3' deep) | LF | 250 | 2.45 | 613 ----- |
| Treated Water Transport System SUBTOTAL | | | | 4,020 |
| Multiplier | | | | 1.4 ----- |
| TOTAL | | | | 5,628 |
| | | | | |
| Additonal Mon. Well | Ea | 5 | 2,000 | 10,000 ----- |
| Additional Well SUBTOTAL | | | | 10,000 |
| Multiplier | | | | 1.4 ----- |
| TOTAL | | | | 14,000 ===== |
| CONSTRUCTION SUBTOTAL | | | | 248,954 |

Percentage of Total Cost

| | Percentages | |
|-----------------------------|-------------|-----------------|
| Bid Contignencies | 15 | 37,343 |
| Scope Contingencies | 25 | 62,238 |
| Construction Total | | 348,535 |
| Permitting and Legal | 5 | 17,427 |
| Bonding and Insurance | 3 | 10,456 |
| Service During Construction | 4 | 13,941 |
| Miscellaneous Lab Testing | 5 | 17,427 ----- |
| Total Implementation Cost | | 407,786 |
| | | |
| Engineering Design | 15 | 61,168 ----- |
| Total Capital Cost | | 468,954 |

OPERATION AND MAINTENANCE COSTS

| | Total Cost (\$)/Year 0-30 Years |
|--|------------------------------------|
| | ----- |
| Ground-Water Monitoring System | |
| Quarterly Sampling and Analysis 14 Wells @ \$3800/well | 53,200 |
| Ground Water Withdrawal System Power (@ .06/Kwh) | |
| 1 Extraction well, 1.5Hp, 100% on-line | 550 |
| Labor @ \$25/hr, 200hr/yr | 5,000 |
| Air Stripping Treatment System | |
| Sampling and Analysis of Effluent | 10,000 |
| 1 Blower(5Hp) & 1 Pump(5Hp) 100% on-line | 3,900 |
| Maintenance (\$35/hr, 500 hr) | 17,500 |
| Annualized Equipment Replacment Cost | |
| 1 Well Pump @ \$2500 | 161 |
| 1 Circulation Pump @ \$ 3550 | 229 |
| 1 Gas Blower @ \$20,000 | 1,289 |
| | ----- |
| Total Annual Operation and Maintenance Cost | 91,829 |
| NET PRESENT VALUE | |
| Capital Cost | 468,954 |
| Present Value of Operation and Maintenance Cost | 1,411,636 |
| | ===== |
| TOTAL PRESENT VALUE | 1,880,590 |

TABLE A-6

COST ESTIMATE FOR ALTERNATIVE 5 SITE ST14

| Capital Costs | Units | Qty | Unit Price (\$) | Total Cost (\$) |
|---|-------|-----|-----------------|-----------------|
| Ground Water Withdrawal System | | | | |
| Extraction Well | Ea | 1 | 2,000 | 2,000 |
| Well Pump | Ea | 1 | 2,500 | 2,500 |
| Plastic Dual Wall Pipe and fittings | LF | 250 | 32.00 | 8,000 |
| Excavation Backfill (1' wide, 3' deep) | LF | 250 | 2.45 | 613 |
| Boring for 2" pipe (100' minimum) | LF | 100 | 12.14 | 1,214 |
| Jacking Pit Prep | Ea | 1 | 8,000 | 8,000 |
| Withdrawal System SUBTOTAL | | | | 22,327 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 31,257 |
| Ground-water treatment system | | | | |
| Oil Water Separator | Ea | 1 | 38,000 | 38,000 |
| Microorganism Blending Facility | | | | |
| Storage Tank | Ea | 1 | 7,500 | 7,500 |
| Blending Tank | Ea | 1 | 3,000 | 3,000 |
| Mixer | Ea | 1 | 4,900 | 4,900 |
| Booster | Ea | 1 | 2,500 | 2,500 |
| Chemical Feed System | Ea | 1 | 4,600 | 4,600 |
| Containment Pad | Ea | 1 | 10,000 | 10,000 |
| Plastic Dual Wall Pipe and fittings | LF | 670 | 32.00 | 21,440 |
| Excavation Backfill (1' wide, 3' deep) | LF | 670 | 2.45 | 1,642 |
| Ground-water treatment System SUBTOTAL | | | | 93,582 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 131,014 |

Blended Water Injection System

| | | | | |
|---------------------------|----|---|-------|--------|
| Injection Wells | Ea | 2 | 2,000 | 4,000 |
| Injection Pumps | Ea | 2 | 3,500 | 7,000 |
| Injection System SUBTOTAL | | | | 11,000 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 15,400 |

| | | | | |
|--------------------------|----|---|-------|--------|
| Additional Mon Wells | Ea | 5 | 2,000 | 10,000 |
| Additional Well SUBTOTAL | | | | 10,000 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 14,000 |

CONSTRUCTION SUBTOTAL 191,671

Percentage of Total Cost

| | Percentages | |
|--------------------------------|-------------|---------|
| Bid Contingencies | 15 | 28,751 |
| Scope Contingencies | 25 | 47,918 |
| Construction Total | | 268,340 |
| Permitting and Legal | 5 | 13,417 |
| Bonding and Insurance | 3 | 8,050 |
| Service During Construction | 4 | 10,734 |
| Treatability and Misc. Testing | 15 | 40,251 |
| Total Implementation Cost | | 340,791 |
| Engineering Design | 15 | 51,119 |
| Total Capital Cost | | 391,910 |

TABLE A-7
 COST ESTIMATE FOR ALTERNATE 1 (No-Action) SITE BSS

| Capital Costs | Units | Qty | Unit Price (\$) | Total Cost (\$) |
|--------------------------|-------|-----|-----------------|-----------------|
| Additional Mon Wells | Ea | 4 | 2,000 | 8,000 |
| Additional Well SUBTOTAL | | | | <u>8,000</u> |
| Multiplier | | | | <u>1.4</u> |
| TOTAL | | | | <u>11,200</u> |
| | | | | ===== |
| CONSTRUCTION SUBTOTAL | | | | 11,200 |

| | Percentage of Total Cost | |
|-----------------------------|--------------------------|--------------|
| | Percentages | |
| Bid Contingencies | 15 | 1,680 |
| Scope Contingencies | 25 | <u>2,800</u> |
| Construction Total | | 15,680 |
| Permitting and Legal | 5 | 784 |
| Bonding and Insurance | 3 | 470 |
| Service During Construction | 4 | 627 |
| Miscellaneous Lab Testing | 5 | <u>784</u> |
| Total Implementation Cost | | 18,346 |
| Engineering Design | 15 | <u>2,752</u> |
| Total Capital Cost | | 21,097 |

OPERATION AND MAINTENANCE COSTS

| | Total Cost (\$) / Year 0-30 Years |
|---|--------------------------------------|
| Ground-Water Monitoring System | |
| Semi-Annual Sampling and Analysis 7 Wells @ \$3800/well | 26,600 |
| Total Annual Operation and Maintenance Cost | <u>26,600</u> |

NET PRESENT VALUE

Capital Cost

21,097

Present Value of Operation and
Maintenance Cost

408,907

=====

TOTAL PRESENT VALUE

430,005

Approved by: _____
Date: _____

TABLE A-8

COST ESTIMATE FOR ALTERNATIVE 2A SITE BSS

| Capital Costs | Units | Qty | Unit Price (\$) | Total Cost (\$) |
|--|--------|-----|-----------------|-----------------|
| Ground Water Withdrawal System | | | | |
| Ground-Water Extraction Trench (3'wide, 10'deep) | 100 LF | 3 | 18,000 | 54,000 |
| Well Pump | Ea | 1 | 2,500 | 2,500 |
| Plastic Dual Wall Pipe and fittings | LF | 200 | 32.00 | 6,400 |
| Excavation Backfill (1' wide, 3' deep) | LF | 200 | 2.45 | 490 |
| Boring for 2" pipe (100' minimum) | LF | 100 | 12.14 | 1,214 |
| Jacking Pit Prep | Ea | 1 | 8,000 | 8,000 |
| Withdrawal System SUBTOTAL | | | | 72,604 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 101,646 |
| Ground-water treatment system | | | | |
| Air Stripping Tower | Ea | 1 | 50,000 | 50,000 |
| Liquid Circ. Pump | Ea | 1 | 3,550 | 3,550 |
| Gas Blower | Ea | 1 | 20,000 | 20,000 |
| Storage Tank | Ea | 1 | 7,500 | 7,500 |
| Controls & Plumbing | Ea | 1 | 20,000 | 20,000 |
| Containment Pad | Ea | 1 | 10,000 | 10,000 |
| Sched 80 PVC - 2" pipe and fittings | LF | 200 | 4.40 | 880 |
| Excavation Backfill (1' wide, 3' deep) | LF | 200 | 2.45 | 490 |
| Ground-water treatment System SUBTOTAL | | | | 112,420 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 157,388 |

Treated Water Injection System

| | | | | |
|---------------------------|----|---|-------|--------|
| Injection Wells | Ea | 2 | 2,000 | 4,000 |
| Injection Pumps | Ea | 2 | 3,500 | 7,000 |
| | | | | ----- |
| Injection System SUBTOTAL | | | | 11,000 |
| Multiplier | | | | 1.4 |
| | | | | ----- |
| TOTAL | | | | 15400 |

| | | | | |
|--------------------------|----|---|-------|--------|
| Additional Mon Wells | Ea | 4 | 2,000 | 8000 |
| | | | | ----- |
| Additional Well SUBTOTAL | | | | 8000 |
| Multiplier | | | | 1.4 |
| | | | | ----- |
| TOTAL | | | | 11,200 |

CONSTRUCTION SUBTOTAL 285,634

Percentage of Total Cost

| | Percentages | |
|-----------------------------|-------------|---------|
| Bid Contingencies | 15 | 42,845 |
| Scope Contingencies | 25 | 71,408 |
| | | ----- |
| Construction Total | | 399,887 |
| | | |
| Permitting and Legal | 3 | 11,997 |
| Bonding and Insurance | 3 | 11,997 |
| Service During Construction | 4 | 15,995 |
| Miscellaneous Lab Testing | 5 | 19,994 |
| | | ----- |
| Total Implementation Cost | | 459,870 |
| | | |
| Engineering Design | 15 | 68,981 |
| | | ----- |
| Total Capital Cost | | 528,851 |

00000000

OPERATION AND MAINTENANCE COSTS

| | Total Cost (\$)/Year 0-30 Years |
|---|------------------------------------|
| | ----- |
| Ground-Water Monitoring System | |
| Quarterly Sampling and Analysis 7 Wells @ \$3800/well | 26,600 |
| Ground Water Withdrawal System Power (@ .06/Kwh) | |
| 1 Sump Pump, 3.0Hp, 70% on-line | 850 |
| Labor @ \$25/hr, 200hr/yr | 5,000 |
| 1 Injection Well, 5Hp, 100% on-line | 2,000 |
| Air Stripping Treatment System | |
| Sampling and Analysis of Effluent | 10,000 |
| 1 Blower(5Hp) & 1 Pump(5Hp) 100% on-line | 3,900 |
| Maintenance (\$35/hr, 500 hr) | 17,500 |
| Annualized Equipment Replacment Cost | |
| 1 Sump Pump @ \$2500 | 161 |
| 1 Injection Pumps @ \$3500 | 226 |
| 1 Circulation Pump @ \$ 3550 | 229 |
| 1 Gas Blower @ \$20,000 | 1,289 |
| | ----- |
| Total Annual Operation and Maintenance Cost | 67,754 |
| NET PRESENT VALUE | |
| Capital Cost | 528,851 |
| Present Value of Operation and Maintenance Cost | 1,041,553 |
| | ===== |
| TOTAL PRESENT VALUE | 1,570,403 |

10111111

TABLE A-9

COST ESTIMATE FOR ALTERNATIVE 2B SITE BSS

| Capital Costs | Units | Qty | Unit Price (\$) | Total Cost (\$) |
|--|--------|-----|-----------------|-----------------|
| Ground Water Withdrawal System | | | | |
| Ground-Water Extraction Trench (3'wide, 10'deep) | 100 LF | 3 | 18,000 | 54,000 |
| Well Pump | Ea | 1 | 2,500 | 2,500 |
| Plastic Dual Wall Pipe and fittings | LF | 200 | 32 | 6,400 |
| Excavation Backfill (1' wide, 3' deep) | LF | 200 | 2.45 | 490 |
| Boring for 2" pipe (100' minimum) | LF | 100 | 12.14 | 1,214 |
| Jacking Pit Prep | Ea | 1 | 8,000 | 8,000 |
| Withdrawal System SUBTOTAL | | | | 72,604 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 101,646 |
| Ground-water treatment system | | | | |
| Air Stripping Tower | Ea | 1 | 50,000 | 50,000 |
| Liquid Circ. Pump | Ea | 1 | 3,550 | 3,550 |
| Gas Blower | Ea | 1 | 20,000 | 20,000 |
| Storage Tank | Ea | 1 | 7,500 | 7,500 |
| Controls & Plumbing | Ea | 1 | 20,000 | 20,000 |
| Containment pad | Ea | 1 | 10000 | 10,000 |
| Excavation Backfill (1' wide, 3' deep) | LF | 200 | 2.45 | 490 |
| Ground-water treatment System SUBTOTAL | | | | 111,540 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 156,156 |
| Treated Groundwater Transport | | | | |
| Manhole to Existing 8" Sewer Line | Ea | 1 | 1,620 | 1,620 |

| | | | | |
|--|----|-----|------|-------|
| Sched 80 PVC - 4" pipe and fittings | LF | 200 | 7.15 | 1,430 |
| Excavation Backfill (1' wide, 3' deep) | LF | 200 | 2.45 | 490 |
| | | | | ----- |
| Treated Water Transport System SUBTOTAL | | | | 3,540 |
| Multiplier | | | | 1.4 |
| | | | | ----- |
| TOTAL | | | | 4,956 |

| | | | | |
|--------------------------|----|---|-------|--------|
| Additional Mon Wells | Ea | 4 | 2,000 | 8,000 |
| | | | | ----- |
| Additional Well SUBTOTAL | | | | 8,000 |
| Multiplier | | | | 1.4 |
| | | | | ----- |
| TOTAL | | | | 11,200 |

CONSTRUCTION SUBTOTAL 273,958

Percentage of Total Cost

| | Percentages | |
|-----------------------------|-------------|---------|
| Bid Contingencies | 15 | 41,094 |
| Scope Contingencies | 25 | 68,489 |
| | | ----- |
| Construction Total | | 383,541 |
| Permitting and Legal | 5 | 19,177 |
| Bonding and Insurance | 3 | 11,506 |
| Service During Construction | 4 | 15,342 |
| Miscellaneous Lab Testing | 5 | 19,177 |
| | | ----- |
| Total Implementation Cost | | 448,743 |
| Engineering Design | 15 | 67,311 |
| | | ----- |
| Total Capital Cost | | 516,054 |

OPERATION AND MAINTENANCE COSTS

| | Total Cost (\$) / Year 0-30 Years |
|---|--------------------------------------|
| | ----- |
| Ground-Water Monitoring System | |
| Semi-Annual Sampling and Analysis 7 Wells @ \$3800/well | 26,600 |
| Ground Water Withdrawal System Power (@ .06/Kwh) | |
| 1 Sump Pump, 3.0Hp, 70% on-line | 850 |
| Labor @ \$25/hr, 200hr/yr | 5,000 |
| Air Stripping Treatment System | |
| Sampling and Analysis of Effluent | 10,000 |
| 1 Blower(5Hp) and 1 Pump(5Hp100% on-line | 3,900 |
| Maintenance (\$35/hr, 500 hr) | 17,500 |
| Annualized Equipment Replacment Cost | |
| 1 Sump Pump @ \$2500 | 161 |
| 1 Circulation Pump @ \$ 3550 | 229 |
| 1 Gas Blower @ \$20,000 | 1,289 |
| | ----- |
| Total Annual Operation and Maintenance Cost | 65,529 |
| NET PRESENT VALUE | |
| Capital Cost | 516,054 |
| Present Value of Operation and Maintenance Cost | 1,007,340 |
| | ===== |
| TOTAL PRESENT VALUE | 1,523,394 |

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TABLE A-10

COST ESTIMATE FOR ALTERNATIVE 3 SITE BSS

| Capital Costs | Units | Qty | Unit Price (\$) | Total Cost (\$) |
|--|--------|-----|-----------------|-----------------|
| Ground Water Withdrawal System | | | | |
| Ground-Water Extraction Trench (3'wide, 10'deep) | 100 LF | 3 | 18,000 | 54,000 |
| Well Pump | Ea | 1 | 2,500 | 2,500 |
| Plastic Dual Wall Pipe and fittings | LF | 200 | 32.00 | 6,400 |
| Excavation Backfill (1-foot wide, 3-foot deep) | LF | 200 | 2.45 | 490 |
| Withdrawal System SUBTOTAL | | | | 63,390 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 88,746 |

Ground-water treatment system**Microorganism Blending
Facility**

| | | | | |
|---|----|-----|--------|--------|
| Storage Tank | Ea | 1 | 7,500 | 7,500 |
| Blending Tank | Ea | 1 | 3,000 | 3,000 |
| Mixer | Ea | 1 | 4,900 | 4,900 |
| Booster | Ea | 1 | 2,500 | 2,500 |
| Chemical Feed System | Ea | 1 | 4,600 | 4,600 |
| Containment Pad | Ea | 1 | 10,000 | 10,000 |
| Plastic Dual Wall Pipe and fittings | LF | 200 | 32.00 | 6,400 |
| Excavation Backfill (1' wide, 3' deep) | LF | 200 | 2.45 | 490 |
| Boring for 2" pipe (100' minimum) | LF | 100 | 12.14 | 1,214 |
| Jacking Pit Prep | Ea | 1 | 8,000 | 8,000 |
| Ground-water treatment System SUBTOTAL | | | | 48,604 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 68,046 |

Blended Water Injection System

| | | | | |
|---------------------------|----|---|-------|-------|
| Injection Wells | Ea | 1 | 2,000 | 2,000 |
| Injection Pumps | Ea | 1 | 3,500 | 3,500 |
| Injection System SUBTOTAL | | | | 5,500 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 7,700 |

| | | | | |
|--------------------------|----|---|-------|--------|
| Additional Mon Wells | Ea | 4 | 2,000 | 8,000 |
| Additional Well SUBTOTAL | | | | 8,000 |
| Multiplier | | | | 1.4 |
| TOTAL | | | | 11,200 |

CONSTRUCTION SUBTOTAL 175,692

Percentage of Total Cost

| | Percentages | |
|--------------------------------|-------------|---------|
| Bid Contingencies | 15 | 26,354 |
| Scope Contingencies | 25 | 43,923 |
| Construction Total | | 245,968 |
| Permitting and Legal | 5 | 12,298 |
| Bonding and Insurance | 3 | 7,379 |
| Service During Construction | 4 | 9,839 |
| Treatability and Misc. Testing | 15 | 36,895 |
| Total Implementation Cost | | 312,380 |
| Engineering Design | 15 | 46,857 |
| Total Capital Cost | | 359,237 |

OPERATION AND MAINTENANCE COSTS

| | Total Cost (\$) / Year 0-30 Years |
|---|--------------------------------------|
| Ground-Water Monitoring System | ----- |
| Semi-Annual Sampling and Analysis 7 Wells @ \$3800/well | 26,600 |
| Ground Water Withdrawal System Power (@ .06/Kwh) | |
| 1 Sump Pump, 3.0Hp, 70% on-line | 850 |
| Labor @ \$25/hr, 200hr/yr | 5,000 |
| 1 Injection Well, 5Hp, 100% on-line | 2,000 |
| Air Stripping Treatment System | |
| Sampling and Analysis of Effluent | 10,000 |
| 1 Blower(5Hp) & 1 Pump(5Hp) 100% on-line | 3,900 |
| Maintenance (\$35/hr, 500 hr) | 17,500 |
| Annualized Equipment Replacment Cost | |
| 1 Well Pump @ \$2500 | 161 |
| 1 Injection Pumps @ \$3500 | 226 |
| 1 Booster Pump @ \$ 3550 | 229 |
| 1 Mixer @ \$4900 | 316 |
| 1 Chemical Feed System @ \$4600 | 296 |
| | ----- |
| Total Annual Operation and Maintenance Cost | 67,078 |
| NET PRESENT VALUE | |
| Capital Cost | 359,237 |
| Present Value of Operation and Maintenance Cost | 1,031,150 |
| | ===== |
| TOTAL PRESENT VALUE | 1,390,386 |

FINAL PAGE

ADMINISTRATIVE RECORD

FINAL PAGE

FINAL PAGE

ADMINISTRATIVE RECORD

FINAL PAGE